

**THE IDENTIFICATION AND DOWN SELECTION OF SUITABLE CATHODE  
MATERIALS FOR USE IN NEXT GENERATION THERMAL BATTERIES**

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This thesis is submitted in partial fulfilment for the degree of PhD  
at the  
University of St Andrews

March 2017

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## Abstract

In this work new novel cathode materials such as transition-metal sulfides, chlorides or fluorides were investigated and studied for their use in lithium ion thermal batteries. All cathodes were synthesized by a solid state reaction in sealed quartz tubes with a duration of firing for 1 week at high temperatures ( $> 500\text{ }^{\circ}\text{C}$ ).

All structures of compounds were probed by powder X-ray diffraction and the morphology and shape of crystallites of cathodes were characterized by scanning electron microscopy. The electrochemical properties of the batteries were investigated by galvanostatic discharge and galvanostatic intermittent titration technique at high temperatures ( $> 400\text{ }^{\circ}\text{C}$ ). All the batteries used as an anode  $\text{Li}_{13}\text{Si}_4$ , as an electrolyte LiCl-KCl eutectic and as separator MgO.

All the products of the discharge mechanism were confirmed using powder X-ray diffraction and EDX analysis.

$\text{CoNi}_2\text{S}_4$  and  $\text{NiCo}_2\text{S}_4$  exhibit two voltage plateaux vs  $\text{Li}_{13}\text{Si}_4$  at  $500\text{ }^{\circ}\text{C}$ , one at around  $1.75\text{ V}$  and the second at  $1.50\text{ V}$ . Capacities of  $350$  and  $290\text{ mA h g}^{-1}$  were achieved, respectively.  $\text{NiS}$ ,  $\text{Co}_3\text{S}_4$  and  $\text{Co}_9\text{S}_8$  were confirmed as the products of discharge mechanism.

$\text{ZrS}_3$  exhibits a single flat voltage plateau of  $1.70\text{ V}$  at a current density of  $11\text{ mA/cm}^2$  and a capacity of  $357\text{ mA h g}^{-1}$ , at  $500\text{ }^{\circ}\text{C}$  was obtained. A new material,  $\text{LiZr}_2\text{S}_4$ , was identified as the product of the electrochemical process, which can be indexed to a  $= 10.452(8)\text{ \AA}$  cubic unit cell.

$\text{KNiCl}_3$  was tested at different current densities from  $15\text{ mA/cm}^2$  to  $75\text{ mA/cm}^2$  and a high cell voltage, with a capacity of  $262\text{ mA h g}^{-1}$  was achieved at  $425\text{ }^{\circ}\text{C}$ . Ni metal, KCl and LiCl were confirmed as the products of the discharge mechanism.

$\text{Li}_2\text{MnCl}_4$  was tested at the same current densities as  $\text{KNiCl}_3$  at  $400\text{ }^{\circ}\text{C}$  and a capacity of  $254\text{ mA h g}^{-1}$  was achieved. Mn metal and LiCl were confirmed as the products after discharge.

$\text{Li}_6\text{VCl}_8$  has a capacity of  $145\text{ mA h g}^{-1}$  and a flat voltage plateau of  $1.80\text{ V}$  at  $500\text{ }^{\circ}\text{C}$ .

$\text{NiCl}_2$  has also a capacity of  $360\text{ mA h g}^{-1}$  and a high voltage profile of  $2.25\text{ V}$  at  $500\text{ }^{\circ}\text{C}$ .

CoCl<sub>2</sub> exhibits a lower capacity of 332 mA h g<sup>-1</sup> and lower voltage profile compared to NiCl<sub>2</sub> at 500 °C. CuF<sub>2</sub> and PbF<sub>2</sub> were tested at 500 °C. PbF<sub>2</sub> exhibits a single flat voltage plateau of 1.25 V and a capacity of 260 mA h g<sup>-1</sup> was obtained. CuF<sub>2</sub> has a high voltage profile but a voltage plateau could not be obtained.

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## List of Abbreviations

EDX	Energy Dispersive X-ray Spectroscopy
GITT	Galvanostatic Intermittent Titration Technique
GSAS	General Structure Analysis System
HRPD	High Resolution Powder Diffractometer
LAN	Liquid Anode
PXRD	Powder X-ray Diffraction
SEM	Scanning Electron Microscopy
VTXRD	Variable Temperature powder X-ray Diffraction

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## **Chapter 1: Introduction**

### **1.1 What is a Lithium ion Battery and why is it useful?**

In the 20<sup>th</sup> century, the main power source was the combustion engine because of its high energy and power densities. Today the rate of global warming and the limited oil supply require a sustainable alternative.

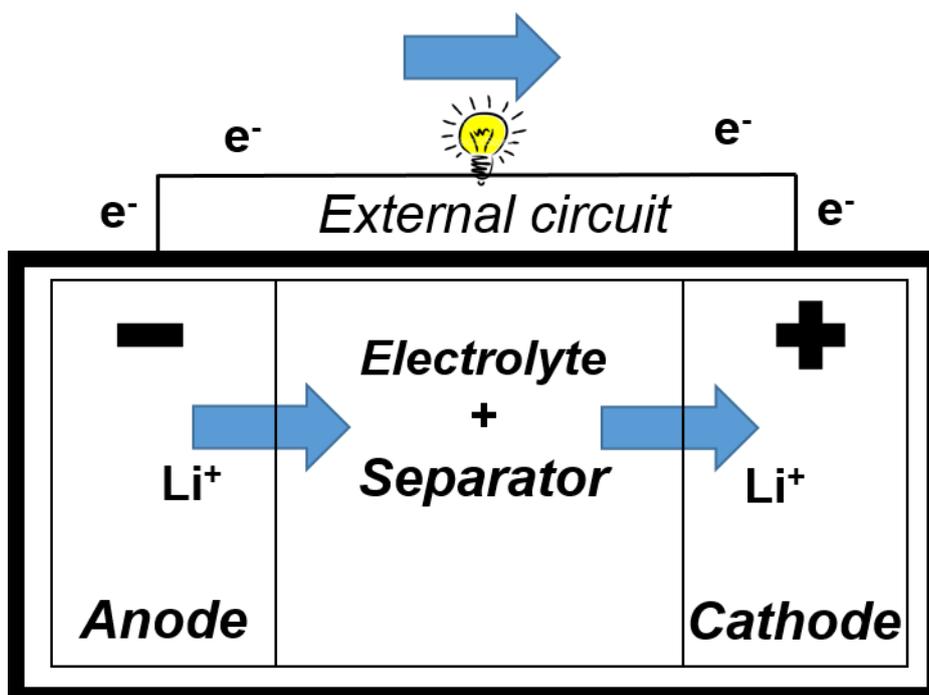
Moreover, the human society and technology progress in electric vehicles, medical equipment, military applications and space technology require power systems with high energy, safety and long shelf – life characteristics. However, the energy conversion and the ability to store huge quantities of electrical energy, which are derived from wind, photovoltaics, fuel cells and engines, is one of the most important social challenges.

There are different kinds of power systems such as supercapacitors, fuel cells and batteries for this goal. Supercapacitors have a low specific energy but the highest specific power. The difference between fuel cells and batteries derives from the fact that fuel cells require a fuel from an outside source, while the batteries do not. However, fuel cells have a higher specific energy than other electrochemical conversion energy devices. Batteries have specific energy and power in a range between supercapacitors and fuel cells. Lastly, batteries provide a higher energy density than supercapacitors or ultracapacitors. However, supercapacitors provide higher power density and longer cyclic life than batteries [1, 2].

Since the SONY Corporation developed a rechargeable lithium - ion battery in 1990, the batteries have been used as power sources in a wide range of applications. Nowadays, batteries are part of our everyday life as they generate power for laptops, mobile phones, electric cars, cameras etc.

Batteries are electrochemical devices that offer a direct conversion of chemical energy to electrical energy by an electrochemical oxidation – reduction reaction as presented in Figure 1.1. During this electrochemical reaction the anode or else, the negative electrode, is oxidized and electrons flow to the external circuit. The cathode or

else, the positive electrode, is reduced and accepts electrons from the external circuit. Between these electrodes there is a high ionic conductor, which is called electrolyte, and provides the motivation of ions from the anode to the cathode. Another part of the battery is also the separator, which used to avoid the physical contact of the anode and the cathode electrode. Batteries need to be sealed to prevent leakage and dry-out.



**Figure 1.1.** A simple illustration of a primary battery. Blue arrows represent the moving of lithium ions during the discharge process

The force that causes the electrons to flow from the anode to the cathode is the difference in the potential energy of the electrons at the anode compared to the one at the cathode. In other words, the potential energy of the electrons is higher at the anode than the one at the cathode. This potential difference is measured in Volts (V) and is called the cell voltage [3]. The theoretical standard cell voltage can be defined by using  $E^{\circ}$  values as:

$$E^{\circ}(\text{cathode}) - E^{\circ}(\text{anode}) = E^{\circ}(\text{cell}) \quad [1.1]$$

This standard theoretical cell voltage is modified by the Nernst equation [4] which relates the reduction potential of an electrochemical reaction (half - cell or full cell reaction) to the standard electrode potential of the chemical species undergoing reduction and oxidation. It is the most important equation in the field of electrochemistry.

The actual cell voltage will often be lower than the theoretical cell voltage due to the polarisation and the cell resistance losses (IR drop) of the battery and is dependent upon the applied current density. These factors are dependent upon electrode kinetics and thus, vary with temperature, state of cycling, and with the age of the battery. Moreover, the IR drop is a result of the change of internal resistance, including the resistance of the electrolyte, electrode materials, and other connectors or auxiliaries. The cell resistance (IR drop) can be decreased by the use of a conductive coating on the surface of the electrode materials [5]. The actual cell voltage needs to be sufficient for the intended application. Typical values of cell voltage range from 1.2 V for a Ni/Cd battery to 4.0 V for a Li ion battery.

There are two types of batteries, primary and secondary. Primary batteries cannot be recharged electrically and are discharged once and discarded. They are only for one use because the electrochemical reaction which occurs in primary batteries is not reversible. Primary batteries have a shelf - life 3 to 5 years.

Secondary batteries can be recharged electrically to their initial condition once they are discharged by passing current in the opposite direction. During discharge process, the ions from the anode pass through the electrolyte and are intercalated into the crystallographic structure of the cathode. As the electrochemical reaction is reversible, the opposite movement of ions takes place during charge process. Secondary batteries have a shelf – life of more years than primary batteries but it depends on their use.

### 1.1.1 Characteristics of Lithium ion Battery

Some characteristics of a lithium ion battery are the discharge curve, the capacity, the energy density, the power density and the operation temperature.

The discharge curve is a plot of cell voltage against time or capacity. A single flat voltage profile is desirable, because this means that the cell voltage remains constant as the battery is discharged. The cell voltage of a lithium ion battery is directly proportional to the reduction of Gibbs free energy when lithium ions are inserted into the cathode electrode, during the discharge process [6, 7].

Capacity of a lithium ion battery is the quantity of electricity involved in the electrochemical reaction between anode and cathode electrode. Capacity is given by Faraday's Law [8] as

$$\text{Capacity} = e^- * F * n \quad [1.2]$$

Where  $n$  = number of moles involved in the electrochemical reaction,  $e^-$  = number of electrons involved in the electrochemical reaction,  $F$  = Faraday's constant (1 mole of electrons,  $F = 96487$  Coulombs) and is measured in units of Ampere - hours per gram ( $A \text{ h g}^{-1}$ ) or ( $\text{mA h g}^{-1}$ ). The capacity in a lithium ion battery depends on (i) the capability of the electrodes to change the oxidation states, (ii) the capability of the electrodes to accommodate the lithium ions, and (iii) the reversibility of the electrochemical reactions [6, 7]. For example, the metal lithium and the lithium silicon alloy  $\text{Li}_{22}\text{Si}_4$  anodes exhibit a theoretical capacity of 3850 and 4200  $\text{mA h g}^{-1}$ , respectively [9, 10]. In the case of  $\text{LiCoO}_2$  cathode, the theoretical capacity is 273  $\text{mA h g}^{-1}$  if one Li ion is inserted into the host lattice. However, the experimental capacity is only 140  $\text{mA h g}^{-1}$  as half of the Li ions can be reversibly inserted into or extracted from the  $\text{LiCoO}_2$  host [11].

The energy density of a battery is a measure of how much energy the battery can store in a given size or mass and its units are ( $\text{Wh/kg}$ ). This energy density is limited by the capacity of the battery and the cell voltage [12, 13].

Power density is a measure of how quickly the battery can deliver energy and its units are ( $\text{W/kg}$ ). The power density of a battery can be improved by nanostructured

electrode materials, which have a large specific surface area and a short solid-state transport distance [14, 15].

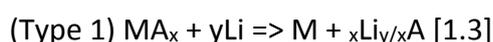
The operation temperature of a lithium ion battery affects the internal resistance. For example, very low temperatures cause higher internal resistance; then, the electrolyte may freeze causing a lower cell voltage as ions are transferred more difficult. However, at very high temperatures the chemical components may decompose, or there may be enough thermal energy available to activate unwanted, reversible reactions, reducing the capacity of the battery.

### **1.1.2 Types of Electrochemical Reactions in a Lithium ion Battery**

There are two different kinds of reaction that can take place in a lithium ion battery. These reactions can be an intercalation reaction or a conversion reaction. An intercalation reaction takes place in lithium ion batteries when the positive electrode is a solid host network that can store guest lithium ions. The lithium ions can be inserted into the structure, or can be removed from, during discharge and charge process. In a lithium ion battery, the guest ions are  $\text{Li}^+$  and the host network compounds are metal chalcogenides, transition metal oxides, or poly-anion compounds. These compounds can be divided into several crystal structures, such as layered, spinel, olivine etc. The layered structure is the most known structure of intercalation compounds for use as cathode materials in lithium ion batteries. However, the most current research is focused on the spinel and olivine structures as these structures exhibit higher operating voltage and higher energy storage capability than the layered structure [16]. The most commercially used transition metal oxide is  $\text{LiCoO}_2$ , introduced by Goodenough and forms a layered structure [17].  $\text{LiCoO}_2$  is a very attractive intercalation cathode material until now, because it has a high theoretical specific capacity of  $274 \text{ mA h g}^{-1}$ , a low self-discharge, a high discharge voltage, and a good cycling performance [18, 19]. However,  $\text{LiCoO}_2$  is expensive because of the high cost of Co. Another, intercalation cathode material (layered structure) is  $\text{LiNiO}_2$  and is cheaper than  $\text{LiCoO}_2$ .  $\text{LiNiO}_2$  has similar electrochemical properties with  $\text{LiCoO}_2$  but is unattractive, because the Ni ions have a

tendency to occupy the lithium ion sites during the synthesis, or delithiation, and as a result they block the Li diffusion pathways [20].  $\text{LiNiO}_2$  is also less thermally stable than  $\text{LiCoO}_2$ , because Ni ions are more easily reduced than Co ions [21].  $\text{LiMnO}_2$  can also replace  $\text{LiCoO}_2$  and  $\text{LiNiO}_2$ , because Mn is much cheaper and less toxic than Co and Ni [22]. However, the performance of  $\text{LiMnO}_2$  needs to be improved because the layered structure has a tendency to change into spinel structure during lithium ion extraction [23].  $\text{LiFePO}_4$  and  $\text{LiMnPO}_4$  are the most known materials for the olivine structure and exhibit good thermal stability and high power capability [24, 25]. The major disadvantage of the  $\text{LiFePO}_4$  is the low electrical and ionic conductivity. Usually, the intercalation cathode materials exhibit capacities of 100 to 200 mA h g<sup>-1</sup> and voltages 3 to 5 V vs. Li/Li<sup>+</sup>.

A conversion reaction takes place in a lithium ion battery, when the cathode material undergoes a solid-state redox reaction during lithiation, or delithiation, in which the crystalline structure changes and is accompanied by the breaking and recombining of chemical bonds [16]. A single flat and long voltage plateau indicates good kinetics of the reaction between two solid phases. There are two types (Type 1 and 2) of a conversion reaction as presented:



and



For example, Type 1 conversion reaction takes place for the  $\text{FeF}_2$  and Type 2 conversion reaction takes place for sulfur ( $\text{Li}_2\text{S}$ ). In the case of  $\text{FeF}_2$ , the fluorine ions have the higher mobility so they diffuse out of the  $\text{FeF}_2$ . LiF and Fe nanosized phases are formed [26]. Moreover, Type 1 conversion cathode materials form metal nanoparticles at their fully lithiated state. Sulfur was studied because it exhibits a high theoretical specific capacity (1675 mA h g<sup>-1</sup>) and is cheap. In the conversion reaction of sulfur there are polysulfides, which are soluble in organic electrolytes [27]. Transition-metal fluoride and chloride compounds have recently been investigated due to their intermediate

operating voltages and their high theoretical specific or volumetric capacities. However, these compounds generally suffer from a poor conductivity, a large voltage hysteresis, a volume expansion, unwanted side reactions, and a dissolution of active material [16]. For example,  $\text{FeF}_3$  and  $\text{FeF}_2$  exhibit a poor electronic conductivity because of their large band gap induced by the highly ionic character of the metal-halogen bond. However, their structures can support a good ionic conduction [28, 29]. Transition-metal chlorides exhibit also a poor electronic conductivity for the same reason [30].

### **1.1.3 Factors affecting the electrochemical properties of a Lithium ion Battery**

In general, there are some factors which affect the electrochemical properties (e.g. cell voltage) of the battery, such as the electronegativity of chemical elements, the structure of the electrodes and the electronic structure of the compounds [31].

It is known that chemical elements with a large atomic number and a large electronegativity lead to a high cell voltage [32]. Electronegativity describes the tendency of an atom to attract a bonding pair of electrons. The electronegativity increases as the atomic number increases in the same row on the periodic table. Different values of electronegativity determine the character of chemical bonds, which are formed between transition-metal ions and anions. Large differences in electronegativity between chemical elements lead to ionic bonds and small differences in electronegativity between chemical elements to covalent bonds. Compounds with ionic bonds are formed in denser structures than compounds with covalent bonds.

This structure density affects the specific site energy of lithium ions and this site energy affects the electrochemical properties of electrodes [31]. This site energy of lithium ions is the main factor of the Gibbs free energy. The Gibbs free energy describes the equilibrium voltage of the electrodes in lithium ion batteries. Moreover, the site energy is the contribution of the enthalpy change ( $H$ ) to the process of lithium ion intercalation ( $dH/dn$ ) [33].

For example, if the site energy in a crystal lattice is low then the external energy, which is consumed to transfer one lithium ion from the occupied site to a free site is high. Different positions in a crystal lattice exhibit different site energies and produce different voltages when lithium ions are inserted into, or extracted from, host electrodes.

The crystal structure of the electrodes affect the electrochemical properties of a lithium ion battery. The crystal structure describes the unique arrangement of the atoms in a crystal which minimises the total energy. The size of the structure can be divided into microstructure and nanostructure. The electrochemical properties of a lithium ion battery change as the size of the structure gets smaller. More specifically, nanostructured electrode materials, the smallest possible crystal structure, enhance these electrochemical properties. This happens because the reversibility of the lithium ions insertion and extraction reaction in nanostructured electrodes takes place without destroying the crystal structure. The reduced particle size affects also the path of lithium ion transfer and increases the rate capability [34]. Small-sized particles have a large specific surface area and therefore a high surface energy.

In addition, the use of defects and disorder of atomic arrangement in the crystal can also affect the cell voltage. Defects change the site energy and can be introduced through doping and control of conditions of the synthesis [35 - 37].

Moreover, electrodes with polyanionic groups, such as phosphates, silicates and sulfates, exhibit higher cell voltage than transition-metal oxides which contain lithium ions. For example,  $\text{LiCoPO}_4$  exhibits a high voltage of 4.8 V compared to  $\text{LiCoO}_2$  which exhibits a voltage of 4 V [38].

The electronic structure of electrode materials is one of the factors that affects the electrochemical properties of a lithium ion battery. For example, the atomic numbers of Mn and Fe are 25 and 26, respectively. Fe is more electronegative than Mn and attracts electrons more strongly than Mn. The energy state of the available electrons is also higher in  $\text{Fe}^{2+}$  than the one in  $\text{Mn}^{2+}$ . However,  $\text{LiMnPO}_4$  exhibits a higher voltage of 4.13 V [39] compared to that one of  $\text{LiFePO}_4$  of 3.43 V [40]. Both compounds are formed in the same crystal structure, as all the lithium ions occupy octahedral sites and are bonded

with six transition metal ions. The difference is that the  $\text{Fe}^{2+}$  ( $3d^6$ ) requires the electron pairing energy to insert the sixth electron in the  $t_{2g}$  orbital and the  $\text{Mn}^{2+}$  ( $3d^5$ ) does not [41]. This provides more energy that could be released or be consumed, in the electrochemical process of Mn phosphate [42, 43].

In general, during the electrochemical process, the lithium ions occupy the space between layers or the octahedral or tetrahedral sites in the host crystal. At the same time, an equal number of electrons occupy the free  $d$  orbitals of the transition-metal cations in the host crystal [31]. Moreover, if the energy, which is realised when the electrons are inserted into or extracted from  $d$  orbitals, is high then the cell voltage is high as well. In addition, the cell voltage of a battery increases as the number of electrons in  $d$  orbitals of the transition-metal elements of the same period in the periodic table increases. As a result, the cell voltage of a battery is directly correlated with the energy, which is required to add or remove lithium ions and to reduce or oxidize the transition-metal cations in the host crystal.

## **1.2 Room temperature and high temperature (thermal) Lithium ion Battery**

Room temperature lithium ion batteries use liquid or polymer gels electrolytes, which are ionically conductive at room temperature and they have self-discharge issues during storage because of the transport of charged species through the electrolyte. Self - discharge decreases the available capacity of the batteries.

This practical problem is solved by using high-temperature lithium ion batteries. Thermal batteries are primary batteries and use molten salt electrolytes (in the separator between the anode and the cathode), which are solid and non – conductive at room temperature. These electrolytes are only ionically conductive when molten and the batteries remain active while the electrolyte stays molten. The electrolytes which are used typically melt  $> 300\text{ }^{\circ}\text{C}$ . The electrodes (anode and cathode) and separator material remain solid during the operation of the battery.

This advantage of the molten electrolyte, provides stable energy storage for decades [44]. The elevated temperature also enhances the electrochemical kinetics in order to provide higher power as they can be discharged at higher currents than the room temperature batteries. For example, the molten salt LiCl – KCl eutectic electrolyte has a value of ionic conductivity of  $1850\text{ mS cm}^{-1}$  at  $500\text{ }^{\circ}\text{C}$ . Thermal batteries provide specific power of  $8000\text{ W kg}^{-1}$  compared to room temperature batteries, for example, Ni/Cd battery, ( $175\text{ W kg}^{-1}$ ) or Li-ion battery, ( $340\text{ W kg}^{-1}$ ) [44, 45].

Thermal batteries, as all batteries, are hermetically sealed and can be stored for more than 25 years over a wide range of storage temperatures (typically,  $- 55$  to  $+ 75\text{ }^{\circ}\text{C}$ ) without degradation [44].

The most common applications of thermal batteries are those that need a long shelf-life and an instant high power like emergency power systems, such as in pilot ejector seats and sonobuoys.

### **1.3 History of Lithium ion Thermal Battery**

The first time that thermal batteries were designed was by German scientists during World War II for V2 rockets as a military application; there, the electrolyte was melted by the rocket exhaust heat in the mission [46]. After World War II, the technology that was used was under the investigation of the United States in 1946. In 1947, Catalyst Research Corp. investigated different kinds of electrolytes and finally, chose the LiCl-KCl eutectic. In 1954, Eagle Picher Technologies, which is the largest US manufacturer of thermal batteries until now, and Sandia National Laboratories, started to develop thermal batteries for the Atomic Energy Commission [44].

The early technology of thermal batteries, the so-called 'cup and cover technology', used the molten salt electrolyte LiCl-KCl eutectic with a glass tape as separator material in a metal cup. The heat source was a mixture of BaCrO<sub>4</sub> and Zr powder; however, this material was very dangerous as it was sensitive to shock.

The later technology, the so-called 'pellet technology', used a powdered kaolin clay to immobilize the electrolyte [47]. Nowadays, ceramic materials are used as separators [48] and thermal batteries include a pyrotechnic material such as Fe-KClO<sub>4</sub> instead of the chromate, which is much safer.

In Chapter 2, there is more discussion and description about the history of the materials that have been used in lithium ion thermal batteries until these days.

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## **Chapter 2: Materials for use in Li Thermal Batteries**

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## **Chapter 2: Materials for use in Li Thermal Batteries**

### **2.1 Anodes for Li thermal batteries**

A high number of different materials have been studied and investigated as anode electrodes for use in Li thermal batteries until recent days. These anode materials are listed and described below.

The materials that have been used as anodes in Li thermal batteries in the early stages of the thermal battery technology, were Ca (calcium) and Mg (magnesium) foils [1]. However, this technology has been replaced quickly by the Ca/CaCrO<sub>4</sub> system in the decade of 1950s. This anode/cathode system was the basic technology for the future of Li thermal batteries.

This basic technology did not use separators between the anode and the cathode. Therefore, there was a physical contact between Ca anode and CaCrO<sub>4</sub> cathode and the cathode was dissolved in the chosen molten salt electrolyte (LiCl-KCl). This reaction created a liquid phase Ca-Li anode, which was the major disadvantage of the system as a short circuit could be obtained. This constitutes the electrochemical issue of that technology. The chemical issue of it is the direct chemical reaction (exothermic) of the Ca-Li liquid anode with the dissolved cathode. This caused an uncontrolled extra heat to the battery and the battery failed [2].

The new technology replaced these materials with calcium, magnesium, aluminium, silicon, or lithium alloys as anode electrodes.

Magnesium alloys were used as anodes in the 1970s, such as Mg-Si, Mg-B, Li-Mg and the performance of the thermal batteries was much better than the previous Ca/CaCrO<sub>4</sub> [3,4]. As new alloys were considered as anodes for use in Li thermal batteries, the next step was the mechanical processing of these alloys [5].

A limited amount of research has been published for Al (aluminium) anodes in tetrachloroaluminate-based electrolytes [6-10] as the system exhibits low rate capabilities and there are temperature limitations (250 °C) imposed by the nature of the chosen electrolyte.

## Chapter 2: Materials for use in Li Thermal Batteries

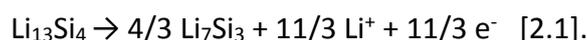
Thermal batteries did not use pure Li as anode as lithium melts at 180 °C, because there would be the same issue as in the case of Ca-Li liquid anode. Nevertheless, some researchers used the liquid Li as anode, the so-called 'LAN', using Fe powder as binder [11]. The amount of the Fe powder as binder was quite big (80% wt) and this reduced the energy density and the potential specific energy of the anode. Lastly, another issue was the chemical reaction of molten Li with potassium ions on the electrolyte (LiCl-KCl).

The later studies include the investigation of Li alloys such as Li-Al, Li-Si, Li-Sb, Li-Bi, Li-Sn, Li-B and Li-Ge for use as anode electrodes.

Several patents describe the preparation of Li-Al alloys [12-14] and many authors have studied the phase diagram of Li-Al [15-18]. However, only the phase  $\beta$ -LiAl is suitable for use as anode in Li thermal batteries as this phase is stable at high temperatures (melting point around 700 °C).

Li-Al alloys have been replaced by Li-Si alloys in the decade of 1980s, as Li-Si alloys have higher specific energies than Li-Al alloys [19] and also, the lithium diffusion in silicon ( $10^{-8} \text{ cm}^2 \text{ s}^{-1}$ ) is greater than the one in aluminium ( $10^{-10} \text{ cm}^2 \text{ s}^{-1}$ ) [20]. Additionally, Li-Si alloys have better rate capabilities and multiple phase transitions [21]. The less lithium content is in the Li-Si alloy, the less power the battery will have, because of the lower rate of lithium diffusion in the alloy under high currents. There are a number of compounds that form within the Li-Si system, and as the Li content increases the potential vs Li decreases.

$\text{Li}_{13}\text{Si}_4$  alloy has the highest Li content and the least oxidation under dry-room conditions. This alloy has also a lower potential (about 157 mV) vs Li at 415 °C compared to others alloys (Li-Al, 297 mV) and this is what makes it the preferred choice in most Li thermal batteries. The capacity of  $\text{Li}_{13}\text{Si}_4$  alloy is  $485 \text{ mA h g}^{-1}$  and the discharge reaction is as it is described below [22]:



Li-Sb, Li-Bi and Li-Sn alloys were not attractive as they have potential vs Li, 800 mV at 400 °C, 720 mV at 487 °C, and 450 mV at 415 °C respectively, and these values are much

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higher than the potential of the  $\text{Li}_{13}\text{Si}_4$  alloy [17, 23]. In addition, Li-Bi has a low melting point, especially Bi (271.3 °C), and this could lead to short-circuit problems in a battery. Li-Sn has also a lower capacity of 265 mA h  $\text{g}^{-1}$  compared to  $\text{Li}_{13}\text{Si}_4$  [24].

Li-B alloys exhibit a higher capacity (2138 mA h  $\text{g}^{-1}$ ) than the Li-Al or Li-Si alloys but there was a difficulty in scaling; more specifically, going from a small-sized laboratory batch to a larger commercial scale. As a result, they have not been used in thermal batteries [25, 26].

Furthermore, Li-Ge alloys were tested as anodes, but they exhibited a high potential of 420 mV vs Li at 400 °C. Lastly, the very high cost of Ge metal makes them also unattractive [27, 28].

To conclude, the preferred choice of this work is the  $\text{Li}_{13}\text{Si}_4$  alloy as it has a lower specific energy and energy density than the Li-Al alloys. Calcium anodes have a very fast activation but a low capacity. Li-Al anodes have a low cost, but compared to Li-Si anodes, they have a lower capacity. LAN anodes have the highest energy and power of them all, but they are expensive and their high Fe content reduces the capacity [29].

Li-Sn and Li-Bi alloys have low melting points, therefore, they could cause short circuit in thermal batteries. Li-Ge alloys exhibit high potentials vs Li for thermal batteries and have the additional limitation of Ge being exorbitantly expensive.

## **2.2 Molten salt electrolytes and separators for Li thermal batteries**

Molten salt electrolytes that are used in Li thermal batteries should have some specific characteristics that are described below.

The most important characteristic of molten salt electrolytes is that they exhibit an extremely low conductivity at room temperature, a very high ionic conductivity and a low electronic conductivity at operating temperatures of 500 - 600 °C range.

All chosen molten salt electrolytes should not be evaporated inside the battery and should have a large electrochemical window, because the chemical reactions between the electrodes and the electrolyte are not desirable. As an example, the fluorides are the most stable halides  $F > Cl > Br > I$ . The oxidation potential of iodide is 3.14 V versus  $Li^+/Li$  at 450 °C [30].

Moreover, electrolytes should not be oxidized by the cathode electrode or be reduced by the anode electrode. The electrolytes should be chemically, kinetically and thermodynamically stable to both electrodes, and should be thermally stable at the battery chosen operating temperature.

High stability towards moisture and oxygen is necessary as this prevents the production of oxides and hydroxides in the molten salt.

The melting point of chosen electrolytes must be lower than the temperature of thermal decomposition of electrodes. The ability to wet both the separator and the electrodes is also important as this minimises the resistance at the electrolyte/electrode interface [31].

The most commonly used electrolytes until now are lithium-halide electrolytes, such as  $LiCl-KCl$  and  $LiCl-LiBr-KBr$ , because of their low melting points (354°C and 310 °C, respectively) [32-35] and their high ionic conductivities ( $1.69 \text{ S cm}^{-1}$  at 475 °C, and  $1.70 \text{ S cm}^{-1}$  at 475 °C, respectively) [36,37]. Lithium-based electrolytes exhibit the highest ionic conductivities due to the high mobility of the lithium ions compared to other alkali-based electrolytes.

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Alkali halide electrolytes have lower melting points ( $< 300\text{ }^{\circ}\text{C}$ ) than lithium halides but they are more expensive (example Cs and Rb). They are, also, more sensitive to moisture and cause self-discharge reactions in the batteries [38].

Some nitrate-based and chlorate systems, such as  $\text{LiNO}_3\text{-KNO}_3\text{-CsNO}_3$ ,  $\text{LiCl-LiNO}_3\text{-NaNO}_2$  and  $\text{LiClO}_3$  respectively, have been examined as electrolytes for their use in thermal batteries. However, they were unattractive candidates due to their exothermic reaction of the anode and the fact that they cause complete meltdown of the battery [39]. Tetrachloroaluminates such as  $\text{NaAlCl}_4$  were also used as electrolytes, but they suffer from poor conductivity of  $250 - 500\text{ mS cm}^{-1}$  at  $200\text{ }^{\circ}\text{C}$  [40].

In Li thermal batteries, due to the high level of mechanical stress (acceleration, shock, spin, vibration, etc.), the chosen molten salt electrolyte should be firmly immobilized by a separator. Usually, the separator consists of powders of metallic oxides such as silica, alumina or magnesia that are electrical insulators.

The first material which was used as separator was ceramic fibre felts and was developed by Argonne National Laboratory [41, 42].

Then, researchers at Sandia National Laboratories in the decade of 1970s developed alternative separators to the kaolin clay that were used for  $\text{Ca/LiCl-KCl/CaCrO}_4$  system [43].

Later technology used fumed silica ( $\text{SiO}_2$ ) and was found to be suitable for application, as it was cheap and the electrolyte required only a small amount of 10% w.t compared to the kaolin clay that needed 30 – 40% w.t. Some fumed silicas, fumed titania and alumina were also investigated for their use as separators. The only problem was that silica had a high reactivity with metallic lithium and Li-alloys anodes at high temperatures.

$\text{Y}_2\text{O}_3$ ,  $\text{ZrO}_2$  oxides have also been tested but  $\text{MgO}$  is the most preferred choice as it has a high thermal stability in contact with high-activity electrodes at elevated temperatures. The lithium chloride-potassium chloride ( $\text{LiCl-KCl}$ ) eutectic electrolyte has become established for use at high temperature batteries and requires a minimum of 35% wt  $\text{MgO}$  as separator [44].

The amount of mass of the separator compared to the mass of the electrolyte is critical. If the mass of separator (e.g. MgO) is too low, either a short circuit between the electrodes (anode/cathode) could be caused, or a leaking of the molten electrolyte could be obtained. If any of these two happen, the battery is out of order and fails. However, if the amount of mass of the separator is too high, there is no wetting of the electrodes by the molten salt electrolyte and therefore, the ionic conductivity will be decreased.

### **2.3 Cathodes for Li thermal batteries**

Cathode materials for use in Li thermal batteries should have some specific characteristics that are described below.

The crucial point is that cathodes should exhibit a high thermal stability as the operation temperature of the battery is high and the products of their thermal decomposition could not cause self-discharge of the battery.

Cathode electrodes should have both high electronic and ionic conductivity.

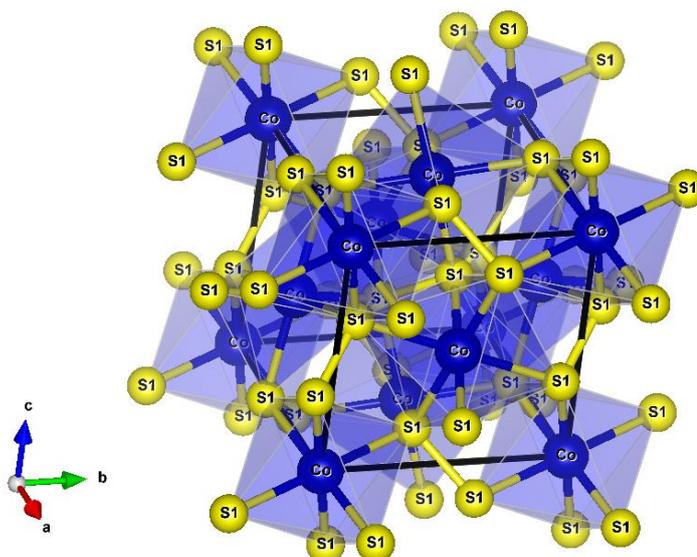
Cathodes should be stable towards moisture and oxygen at ambient temperature. Good wetting by the electrolyte is also important and a minimum resistance at the electrolyte/cathode interface is required [45]. These materials need to be environmentally friendly and inexpensive.

MS<sub>2</sub> sulfides where M is Fe, Ni or Co are the most studied cathodes until now and they exhibit voltages vs Li<sub>13</sub>Si<sub>4</sub> at around 1.70 V for their first electrochemical transition. Moreover, they have further electrochemical transitions, which eventually end in complete reduction to the metal (Fe, Ni, Co respectively) [46].

### 2.3.1 Cathode CoS<sub>2</sub>

CoS<sub>2</sub> was studied for first time as a cathode material at Argonne National Laboratory (ANL) in the decade of 1970s [47]. CoS<sub>2</sub> is preferred as cathode due to the high thermal stability, starting its thermal decomposition above 650 °C. CoS<sub>2</sub> decomposes to Co<sub>3</sub>S<sub>4</sub> and sulfur gas is released [48].

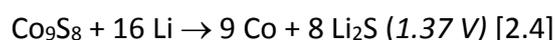
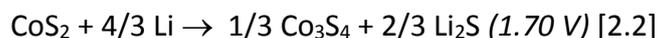
CoS<sub>2</sub> crystallises in a cubic pyrite structure with a unit cell parameter ( $a = 5.539 \text{ \AA}$  and space group  $P\bar{a}3$ ) as presented in Figure 2.1. This structure of CoS<sub>2</sub> is primitive cubic. The cobalt ions are octahedrally coordinated by sulfur, whose pairs form dimers. Each sulfur is shared by three different octahedra and a single dimer. The axes of the diatomic anions are ordered equally along the four  $\langle 111 \rangle$  directions of the cube and the cation octahedra share common corners [49].



**Figure 2.1.** Crystal structure of CoS<sub>2</sub>. Blue atoms are cobalt and yellow atoms are sulfur

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In the discharge reactions of  $\text{CoS}_2$  against Li-Al, as given below, no lithiated products are formed. The voltages of  $\text{CoS}_2$  are against Li-Al at 400 °C and  $\text{CoS}_2$  exhibits three voltage plateaus [46].



The capacity of the first plateau (4/3 Li) is 290 mA h g<sup>-1</sup> which is low as the reader could notice compared to the first plateau of  $\text{FeS}_2$  below. However, the total capacity of  $\text{CoS}_2$  is higher than  $\text{FeS}_2$  with a value of 598 mA h g<sup>-1</sup>.

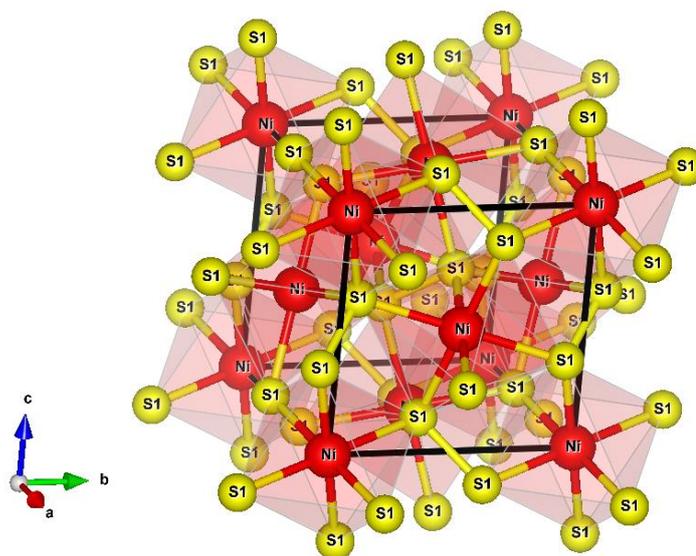
The major advantage of  $\text{CoS}_2$  against  $\text{FeS}_2$  is that  $\text{CoS}_2$  causes less self-discharge reactions in the thermal battery. As a result, the  $\text{CoS}_2$  is an attractive material for long-life thermal batteries.

Nevertheless,  $\text{CoS}_2$  has a major disadvantage, which is the high cost because it should only be synthesized in laboratories.

According to researchers, next studies of  $\text{CoS}_2$  should be the way of synthesising the material with pure phase, low cost and scale up the production [47].

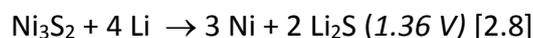
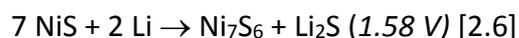
### 2.3.2 Cathode NiS<sub>2</sub>

NiS<sub>2</sub> crystallises in a cubic pyrite structure with a unit cell parameter ( $a = 5.619 \text{ \AA}$  and space group  $Pa\bar{3}$ ) as presented in Figure 2.2. NiS<sub>2</sub> exhibits the same structure as CoS<sub>2</sub> [50].



**Figure 2.2.** Crystal structure of NiS<sub>2</sub>. Red atoms are nickel and yellow atoms are sulfur

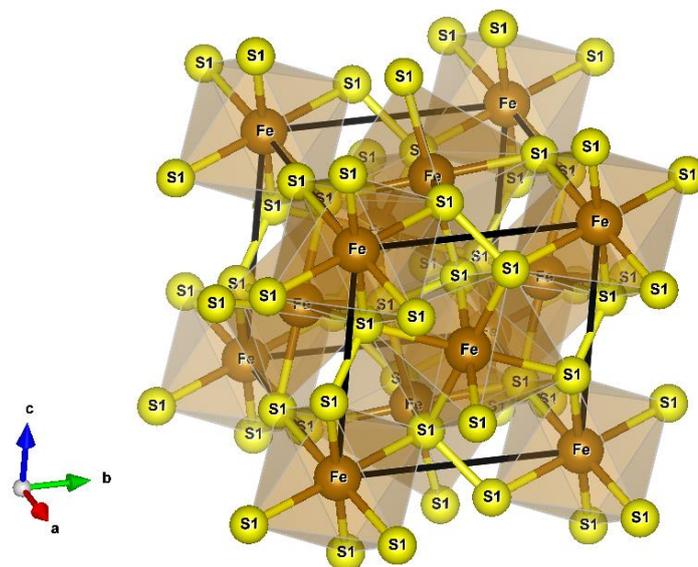
NiS<sub>2</sub> decomposes to NiS and sulfur gas is released at the temperature of 600 °C [51]. In the discharge reactions of NiS<sub>2</sub> against Li-Al, as given below, no lithiated products are formed. The voltages of NiS<sub>2</sub> are against Li-Al at 400 °C and NiS<sub>2</sub> exhibits four voltage plateaus [46]. The total capacity of NiS<sub>2</sub> is 545 mA h g<sup>-1</sup>, which is lower than both CoS<sub>2</sub> and FeS<sub>2</sub>.



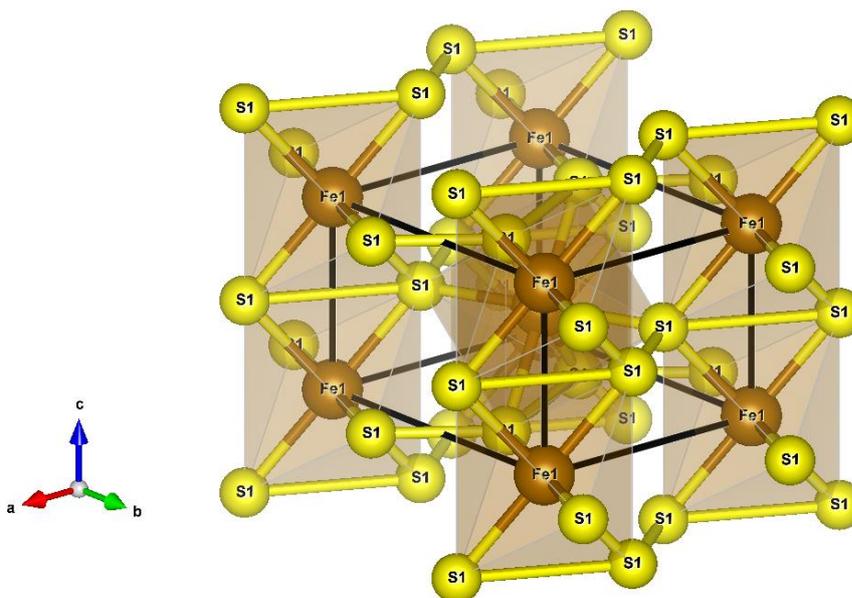
Since the electrochemical performance of the  $\text{NiS}_2$  as cathode is similar to the  $\text{CoS}_2$  and the cost of the  $\text{NiS}_2$  is much less than the one of  $\text{CoS}_2$ , all these characteristics make  $\text{NiS}_2$  an attractive material for use in Li thermal batteries.

### 2.3.3 Cathode $\text{FeS}_2$

$\text{FeS}_2$  has long been used as a cathode in Li thermal batteries since 1978 [52].  $\text{FeS}_2$  exhibits two forms, the pyrite with a unit cell parameters ( $a = 5.428 \text{ \AA}$  and space group  $\text{Pa}\bar{3}$ ) [53] and the marcasite with a unit cell parameters ( $a = 4.445 \text{ \AA}$ ,  $b = 5.425 \text{ \AA}$ ,  $c = 3.388 \text{ \AA}$  and space group  $\text{Pnmm}$ ) [54] as presented in Figure 2.3 and 2.4, respectively. The pyrite structure is described above. The marcasite is an orthorhombic crystal structure. Both structures have the sulfur dimers in a short bonding distance between sulfur atoms. The structures differ only in how these dimers are arranged around the Fe atoms. In the orthorhombic marcasite structure linear chains of edge-shared octahedra run parallel to the orthorhombic  $c$ -axis.

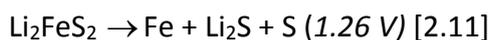
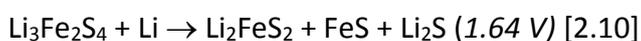


**Figure 2.3.** Crystal structure of pyrite  $\text{FeS}_2$ . Brown atoms are iron and yellow atoms are sulfur



**Figure 2.4.** Crystal structure of marcasite  $\text{FeS}_2$ . Brown atoms are iron and yellow atoms are sulfur

$\text{FeS}_2$  decomposes to  $\text{FeS}$  and sulfur gas is released as well at the temperature of  $580^\circ\text{C}$  in the form of pyrite. Sulfur gas reacts exothermically with the anode electrode or dissolved lithium in the chosen molten salt electrolyte [55, 56]. In the discharge reactions of  $\text{FeS}_2$  against  $\text{Li-Al}$ , as given below, there are formed lithiated products  $\text{Li}_3\text{Fe}_2\text{S}_4$  and  $\text{Li}_2\text{FeS}_2$ . The voltages of  $\text{FeS}_2$  are against  $\text{Li-Al}$  at  $400^\circ\text{C}$  and  $\text{FeS}_2$  exhibits three voltage plateaus [46].



In the first plateau ( $3/2 \text{Li}$ ) the capacity of  $\text{FeS}_2$  is  $335 \text{ mA h g}^{-1}$  which is higher than the capacity in the first plateau of  $\text{CoS}_2$ . However, the total capacity of  $\text{FeS}_2$  is  $558 \text{ mA h g}^{-1}$  and less than the one of  $\text{CoS}_2$ .

## 2.4 Aim of this project

The improvement and the better performance of Li thermal batteries will come through the investigation of novel cathodes, as the materials which are used as anode and electrolyte/separator are standard and well-studied.

The best cathode material for use in Li thermal batteries should have a high voltage (ideally  $> 3$  V) and a high capacity ( $> 614$  mA h  $g^{-1}$ ). It should be also a good electronic conductor and have a low solubility in the chosen molten salt electrolyte (LiCl-KCl).

The ideal circumstances will be if the cathode materials exhibit multiphase discharge (and not intercalation) as this enables better voltage control, providing a constant power for longer than the one in the case an intercalation compound was used [57, 58].

The aim of this project is to investigate, study, synthesise and characterise novel cathode materials for use in Li thermal batteries in order to improve their performance.

More specifically, this work studies some transition metal sulfides, chlorides or fluorides compositions, such as ( $CoNi_2S_4$ ,  $NiCo_2S_4$ ,  $ZrS_3$ ,  $KNiCl_3$ ,  $Li_2MnCl_4$ ,  $Li_6VCl_8$ ,  $NiCl_2$ ,  $CoCl_2$ ,  $CuF_2$  and  $PbF_2$ ).

The aim is, wherever is possible, to achieve spinel structure  $AB_2S_4$  where A and B are transition metals with oxidation state  $A^{+2}$ ,  $B^{+3}$ , and  $S^{-2}$ .

As a guide of this work, these cathodes should have a good thermal stability, be stable, exhibit a flat/single voltage plateau and a long shelf-life, as well as be environmentally friendly.

The characterisation of the novel cathode materials includes techniques such as powder X-ray Diffraction, Scanning Electron Microscopy, Galvanostatic discharge tests etc.

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## **Chapter 3: Experimental procedure**

### **3.1 Solid State Synthesis**

Solid State Synthesis is a stoichiometric reaction of powders (elements, binary compounds, ternary compounds, etc.) at high temperature in different conditions such as in air, under vacuum, or in inert or reactive gases.

The most important advantage of Solid State Synthesis is the fact that it is a very simple method and a high temperature direct reaction. However, it could become a complicated method if the synthesis requires different firing steps and atmosphere conditions to complete the reaction. Though, in consequence, a high temperature reaction usually leads to thermodynamically stable products. Another advantage of it is the selection of the atmosphere, as it is easy to use flowing gases. There are also more choices for the preparation of the samples, which needs evacuated quartz tube or any other sample holders under inert atmosphere. Moreover, the cooling step can be slow in a furnace under controlled conditions or fast in air, in water or in liquid nitrogen conditions.

The most important disadvantage of Solid State Synthesis is that it needs a long time of period in order to be completed and the reaction is limited by slow diffusion. Also, there are problems in case some reactants melt or form a vapour at the reaction temperature. Moreover, the reaction may be limited by phase diagram. Some other issues are the fact that the reaction may be incomplete or some loss of the reactants to take place. At this point, the products may not form the desired microstructure or be compositionally homogeneous. This method can be expensive as high temperatures are required for the diffusion or for bonds' break of the precursors. Additionally, the purification can be difficult with a big number of steps for the removal of impurities.

The standard Solid State Synthesis includes some key points such as the area of contact between reacting powders. It is significant to use starting reagents with large surface area in order to maximise the contact between reactants or to pelletize samples

to encourage intimate contact between crystallites. Another key point is the rate of diffusion. There are two ways to increase it: either by increasing the temperature or by introducing defects at the reagents that decompose prior or during reaction. Furthermore, the rate of nucleation of the product phase is critical as it can be maximised by using reactants with crystal structures similar to these of the product.

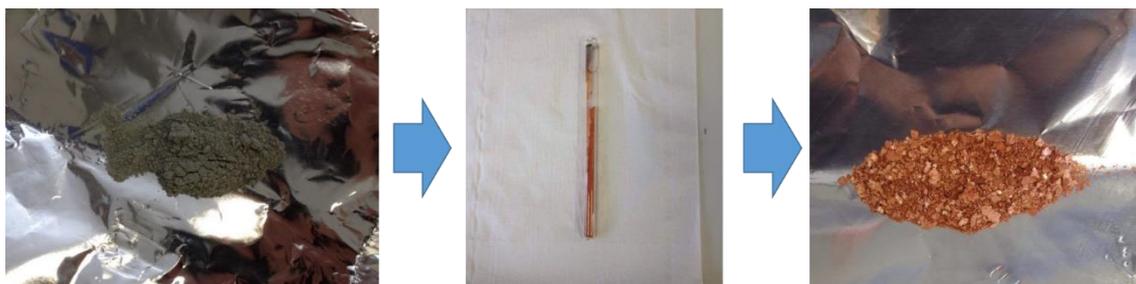
Solid State Synthesis starts with the selection of appropriate starting materials, which are fine grain powders and their surface area is the maximum. Also, reactive starting reagents are better than inert ones for the Solid State Synthesis and well defined compositions are required, too. The next step is to weigh out starting materials and mix them together. The mixing takes place in a mortar and pestle or in a ball mill. Following, the pressing of the mixture into pellets and the selection of the most suitable sample container have to be conducted, because the reactivity, the strength, the cost and the ductility are all important. Finally, when the sample is heated and after that cooled down, the product is ground and analysed by characterisation techniques [1].

### **3.1.1 Synthesis of cathode materials**

All the cathode materials  $ZrS_3$ ,  $CoNi_2S_4$ ,  $NiCo_2S_4$ ,  $KNiCl_3$ ,  $Li_2MnCl_4$  and  $Li_6VCl_8$  were synthesised by a solid state reaction in sealed quartz tubes to prevent oxidation of starting materials during the synthesis.

$NiCl_2$  (Alfa Aesar, 99%),  $CoCl_2$  (Alfa Aesar, 99.7%),  $CuF_2$  (Alfa Aesar, 99.5%) and  $PbF_2$  (BDH Chemicals, 99%) were used as commercial compounds.

0.966 g of zirconium (Aldrich,-100mesh) and 1.026 g of sulfur (Alfa Aesar,-100mesh, 99.5%) powders were used for the synthesis of  $ZrS_3$  as shown in Figure 3.1 [2-5].



**Figure 3.1** Synthesis of  $ZrS_3$

0.77 g of nickel (Aldrich,-100mesh, 99%), 0.38 g of cobalt (Alfa Aesar,-325mesh, 99.5%) and 0.83 g of sulfur (Alfa Aesar,-100mesh, 99.5%) powders were used to synthesise  $CoNi_2S_4$  [6-7].

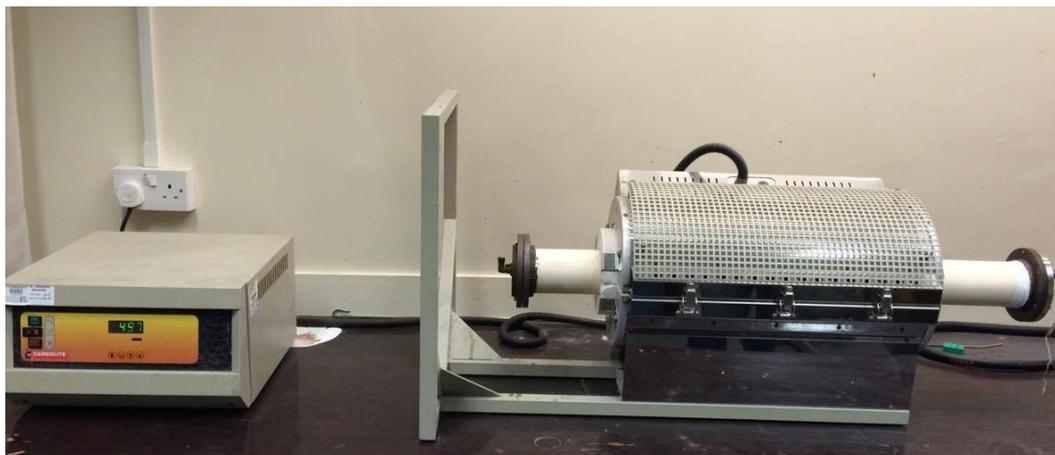
The ratio between nickel and cobalt was changed for  $NiCo_2S_4$  as 0.38 g of nickel (Aldrich,-100mesh, 99%) and 0.77 g of cobalt (Alfa Aesar,-325mesh, 99.5%).

0.73 g of KCl (Aldrich, 99%) and 1.27 g of  $NiCl_2$  (Alfa Aesar, 99%) powders were used to synthesise  $KNiCl_3$  [8-9].

0.81 g of LiCl (Alfa Aesar, 99%) and 1.19 g of  $MnCl_2$  (Strem, 97%) powders were used to synthesise  $Li_2MnCl_4$  [10].

1.18 g of  $VCl_2$  ( $VCl_3$ , Aldrich, 97%) and 0.82 g of LiCl (Alfa Aesar, 99%) powders were used to synthesise  $Li_6VCl_8$ .  $VCl_2$  was prepared through the decomposition of  $VCl_3$  to  $VCl_2$  under nitrogen flow at 797 °C. Following that, in order  $VCl_2$  to be purified, it was heated at 827 °C in a quartz tube [11].

All the powders for the synthesis of transition metal sulfides were weighed out and mixed in a mortar and pestle in air and then sealed into an evacuated ( $10^{-3}$  mbar) quartz tubes before the reactions were carried out inside a tube furnace as shown in Figure 3.2. All the powders for the synthesis of transition metal chlorides were weighed out in the required stoichiometry and mixed in a mortar and pestle in an argon filled glove box and then sealed into evacuated quartz tubes ( $10^{-3}$  mbar).



**Figure 3.2.** Tube furnace with the controller

ZrS<sub>3</sub> was fired at 730 °C for 1 week, with a heating and cooling rate of 1 °C min<sup>-1</sup>. This heating and cooling rate was used for all the compounds. CoNi<sub>2</sub>S<sub>4</sub> and NiCo<sub>2</sub>S<sub>4</sub> were heated in a tube furnace with the duration, the temperature and the number of firings used in the synthesis as presented in Table 3.1. Between each firing the sample was ball milled under argon for 4 hours to achieve homogeneity. The duration and the temperatures of the syntheses of transition metal chlorides KNiCl<sub>3</sub>, Li<sub>2</sub>MnCl<sub>4</sub> and Li<sub>6</sub>VCl<sub>8</sub> are presented in Table 3.2.

**Table 3.1.** Experimental conditions for the synthesis of CoNi<sub>2</sub>S<sub>4</sub> and NiCo<sub>2</sub>S<sub>4</sub>

Compounds	1 <sup>st</sup> Firing	Ball milling	2 <sup>nd</sup> Firing
CoNi <sub>2</sub> S <sub>4</sub>	550 °C for 24 hours	4 hours in argon	550 °C for 156 hours
NiCo <sub>2</sub> S <sub>4</sub>	550 °C for 24 hours	4 hours in argon	550 °C for 156 hours

**Table 3.2.** Firings and temperatures of the syntheses of transition metal chlorides

Compounds	Firings
$\text{KNiCl}_3$	675 °C for 1 week
$\text{Li}_6\text{VCl}_8$	800 °C for 1 week
$\text{Li}_2\text{MnCl}_4$	600 °C for 1 week

## 3.2 Characterisation techniques

In this work, the characterisation of the novel cathode materials includes techniques such as Powder X-ray Diffraction or Powder Neutron Diffraction in order to identify phases and structures; Scanning Electron Microscopy–Energy Dispersive X-ray Spectroscopy in order to study phase morphology and elemental composition; and lastly, Galvanostatic Intermittent Titration Technique and Galvanostatic Discharge tests in order to investigate electrochemical performance.

### 3.2.1 Powder X-ray Diffraction (PXRD)

Powder X-ray Diffraction is a useful technique for studies of the crystallographic structure of materials. This method identifies phase purities/impurities, and lattice parameters of known/unknown phases, as well as analyses multi-phase systems [12].

This technique of X-ray diffraction has existed for over 1 century and its operation is based on the use of Bragg's Law. X-rays are electromagnetic waves with the exact same nature as light, but with wavelengths on the scale of Angstroms and with the same order

as the interatomic distances. Moreover, the incoming X-rays are scattered by the electrons of the atoms. So, the interference between the X-rays and the electrons of the atoms occurs at a certain angle from the sets of atomic planes and the scattering is unique to the crystal structure. The sample is scanned by a detector through a range of angles called  $2\theta$  so that all possible diffraction directions of the lattice can be attained due to the random orientation of the sample. At each angle where the X-rays are diffracted by these crystal planes, a 'peak' is observed by the detector. The pattern that is produced is used to analyse the structure, the cell parameters, the atom positions etc. [13].

Powder X-ray diffraction analysis was conducted in order to identify the crystalline phases. Room temperature powder X-ray diffraction data were collected for all the cathodes using a Panalytical Empyrean diffractometer in Bragg-Bretano geometry with a Ge (220) monochromator and Cu  $K\alpha_1$  radiation ( $\lambda=1.5406 \text{ \AA}$ ) as shown in Figure 3.3.



**Figure 3.3.** Panalytical Empyrean diffractometer in Bragg-Bretano geometry with a Ge (220) monochromator and Cu  $K\alpha_1$  radiation ( $\lambda=1.5406 \text{ \AA}$ )

## Chapter 3: Experimental procedure

For  $ZrS_3$ ,  $NiCo_2S_4$ ,  $KNiCl_3$ ,  $Li_2MnCl_4$ ,  $Li_6VCl_8$ ,  $NiCl_2$ ,  $CoCl_2$ ,  $PbF_2$ , and  $CuF_2$  data were collected from  $5^\circ$  to  $70^\circ 2\theta$  for 1 hour with a step size of  $0.017^\circ$  and a time per step of 0.94 seconds. For  $CoNi_2S_4$ , data were collected in the  $10^\circ$  to  $100^\circ 2\theta$  range for 1 hour, with a step size of  $0.017^\circ$  and a time per step of 0.68 seconds. All the samples are submitted in air-sensitive Si-substrate holders, covered with Kapton film for air protection.

Variable temperature powder X-ray diffraction (VTXRD) data for  $ZrS_3$  were collected using a Panalytical Empyrean diffractometer with  $Mo\ K\alpha_{1,2}$  radiation,  $\beta$ -filter and an X'celerator RTMS detector, equipped with an Anton Paar HTK1200N furnace as shown in Figure 3.4. Data were collected from  $4^\circ$  to  $40^\circ 2\theta$  for 6 hours with a step size of  $0.008^\circ$  and a time per step of 600 seconds. In this case the  $ZrS_3$  sample was loaded into a quartz capillary and sealed for variable temperature data collection.

Crystallographica Search-Match software was used to identify known and unknown peaks and WinXPOW software was used for indexing and refining the unit cell parameters.



**Figure 3.4.** Panalytical Empyrean diffractometer with  $Mo\ K\alpha_{1,2}$  radiation,  $\beta$ -filter and an X'celerator RTMS detector, equipped with an Anton Paar HTK1200N furnace

### **3.2.2 Powder Neutron Diffraction**

Powder neutron diffraction is a technique which is able to study both structure and dynamics; in specific, where atoms are and how atoms move. The neutrons have wavelengths which are comparable to atomic distances, therefore, they can study structures from Angstroms to the scale of microns. Also, they have energies similar to those of atomic and electronic processes enabling lattice vibrations, molecular motions, diffusion and tunnelling to be investigated. In this method, neutrons are scattered from the nucleus of an atom rather than the electrons (which X-rays are scattered from), so light atoms, such as hydrogen, lithium etc., can be seen in the presence of heavier atoms. Advantages of neutron diffraction compared to X-rays are that neighbouring elements in the periodic table can be distinguished and different isotopes of the same element can be used to label parts of molecules and enhance the technique's sensitivity. Neutrons have a relatively weak interaction with matter, so, complex sample environment can be used. Moreover, neutrons have a magnetic moment, which makes them suitable for studying magnetic materials.

Neutrons are produced by a heavy metal target when it is bombarded by an energetic proton beam from a circular, synchrotron accelerator. Then, the neutrons are slowed down by hydrogenous moderators around the target in order their energies (wavelengths) to be suitable for the materials under investigation. Finally, they are directed to some instruments, where each one of them is optimised to explore different atomic-level properties [14].

One of these instruments is the High Resolution Powder Diffractometer (HRPD), the highest resolution neutron diffractometer in the world. It is designed to achieve an optimal balance between the maximum practical resolutions attainable and reasonable counting times. All samples are loaded into cylindrical vanadium cans and are hermetically sealed before attached to sample tank of the instrument. In order to reduce air-scattering in all sample environments, the sample tank is evacuated before the data collection [15-16].

The diffracted neutron beam on HRPD can be detected in one of three fixed angle banks, at 168° (backscattering), at 90° and at low angles 30° as shown in Figure 3.5.

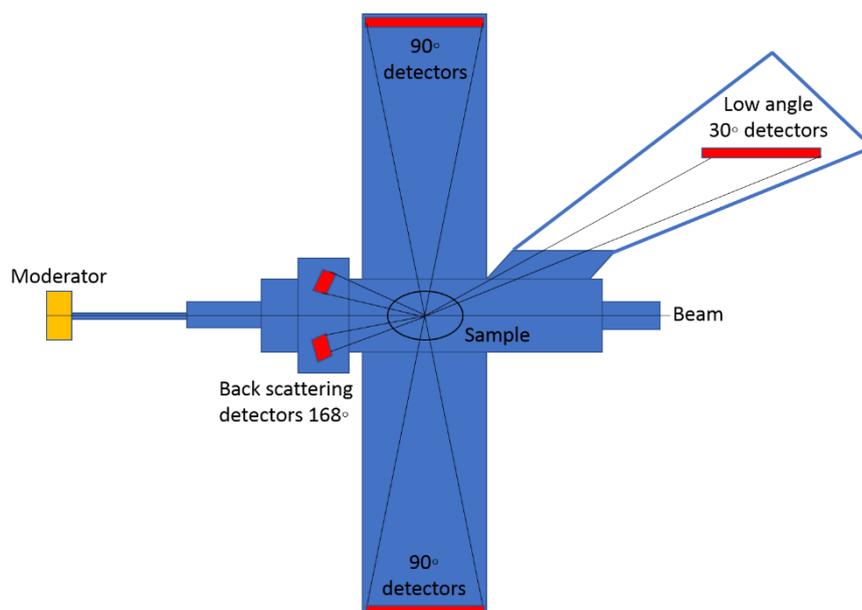


Figure 3.5. Schematic view of the HRPD detector

Powder neutron diffraction data for  $\text{CoNi}_2\text{S}_4$  were collected with the High Resolution Powder Diffractometer (HRPD), using the backscattering detectors, at the ISIS neutron source, Rutherford Appleton Laboratory, UK. Rietveld refinement was carried out using the General Structure Analysis System (GSAS) [17-18].

### 3.2.3 Scanning Electron Microscopy–Energy Dispersive X-ray spectroscopy (SEM-EDX)

Scanning Electron Microscopy (SEM) is an important technique for the production of images of a solid sample's surface and also, for the analysis of the sample's elemental composition (EDX). The microscope uses a focussed electron beam from an electron gun which scans the surface of the sample and detects the secondary electrons that are returned to the detector and as a result, produces an image. If the sample is non-conductive, then it requires sputtering with gold or carbon to prevent charging of the sample and subsequent overexposure of the image. Usually, samples are placed into the

instrument as powders, which are spread on a graphite coated holder in order to study phase morphology [19].

In addition to the study of the morphology, SEM analyses the elemental composition by Energy Dispersive X-ray spectroscopy (EDX). In this method, the incoming electron beam passes through the sample and goes through inelastic scattering of the incident electrons. If the excited electron has sufficient energy, an electron may be ejected from the lower energy level of the atom. Then, a vacancy is created which is filled by an electron from the higher energy level and this results in the emission of an X-ray. The EDX method is based on energy levels of the transitions of electrons taking place in inner atomic orbitals. The energy of the X-rays emitted is exactly equal to the energy of the difference of the two electronic levels. The energy difference between each atomic orbital is unique to each element. However, EDX cannot analyse light elements such as lithium as it is difficult to identify the incident X-ray energy from other lighter elements. This means that it was impossible to study cathodes that consist of lithium such as  $\text{Li}_2\text{MnCl}_4$  and  $\text{Li}_6\text{VCl}_8$ .

Scanning Electron Microscopy was carried out using a Jeol JSM-5600 microscope to study and identify the phase morphology. EDX on the Jeol JSM-5600 SEM was used to identify elemental composition in all synthesised cathode powders via mapping and point analysis as shown in Figure 3.6.



**Figure 3.6.** Jeol JSM-5600 SEM

### 3.2.4 Galvanostatic Intermittent Titration Technique (GITT)

Lithium ion thermal batteries are investigated as energy storage devices due to their relatively high power performances. During discharge of a Li thermal battery, lithium ions are transported from the anode electrode, through the electrolyte, to the cathode electrode and Li-ion diffusion occurs into the bulk material. In this respect, knowing the voltage and the current pulses, it is simple to calculate the cell resistance. Furthermore, this method can give a better understanding of thermal batteries' electrochemical behaviour. The galvanostatic intermittent titration technique (GITT) is a useful procedure for the retrieval of both thermodynamics and kinetics parameters that constitute the cell resistance.

GITT testing consists of galvanostatic discharge pulses, each 10 minutes long, followed by 5 minutes of relaxation time, with no current passing through the battery.

During a current pulse the voltage quickly decreases to a value proportional to IR and then, the voltage slowly decreases due to the galvanostatic discharge pulse. During the relaxation time, the voltage suddenly increases by a value proportional to IR and then, it slowly increases until the electrode is again in equilibrium and the open circuit voltage  $V_{oc}$  of the battery is reached. Then, the following galvanostatic pulse is applied and this sequence of discharge pulse followed by a relaxation time is repeated until the battery is discharged [20-21].

The chemical diffusion coefficient can be calculated at each step, with the following equation

$$D = 4 / \pi t * (n_m V_m / S)^2 * (\Delta E_s / \Delta E_t)^2 \quad [3.1].$$

Where,  $t$  is the duration of the galvanostatic discharge pulse ( $t = 600$  s),  $n_m$  is the number of moles (mol),  $V_m$  is the molar volume of the electrode ( $\text{cm}^3 / \text{mol}$ ),  $S$  is the electrode/electrolyte contact area ( $S = 1.326 \text{ cm}^2$ ),  $\Delta E_s$  is the steady-state voltage change, due to the galvanostatic discharge pulse and  $\Delta E_t$  is the voltage change during the galvanostatic discharge pulse, eliminating the IR drop [20-21].

For the batteries under investigation, in order to have sufficiently slow voltage changes, a current density of 7.5 mA/cm<sup>2</sup> or 15 mA/cm<sup>2</sup> was chosen for discharge for the GITT measurements.

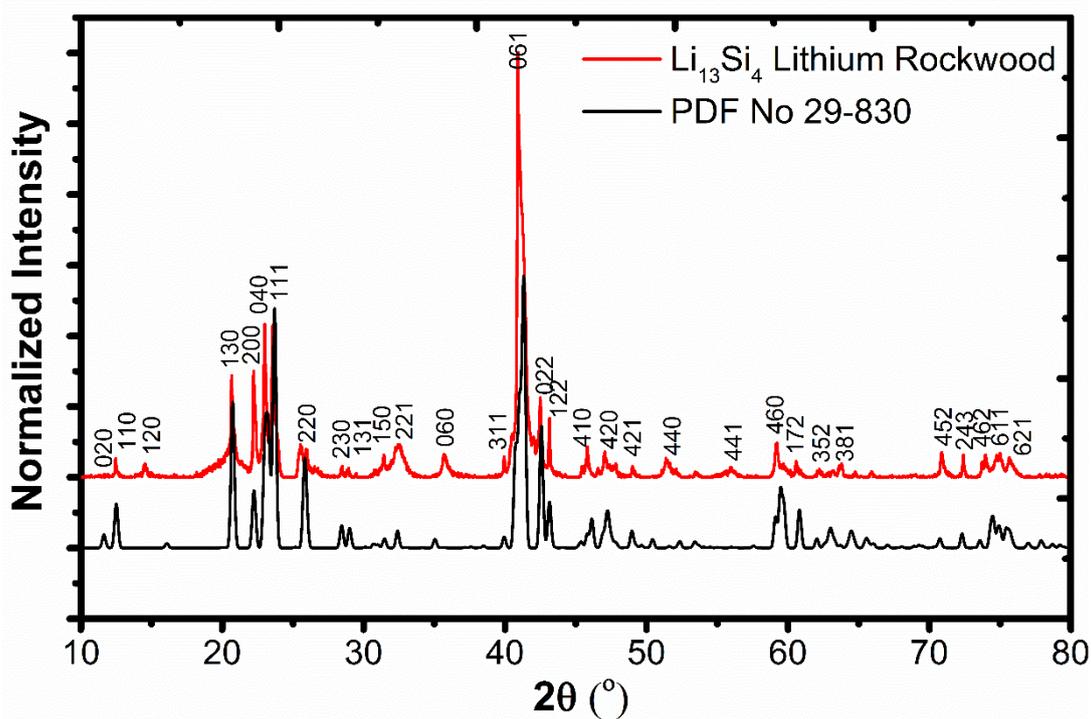
### **3.2.5 Galvanostatic Discharge**

Galvanostatic Discharge is a technique where a current density is applied between the cathode (working) and the anode (counter) electrode and the voltage is measured. The current density is applied until the set lower voltage limit is reached or the battery is fully discharged. This technique is the main testing for the electrochemical investigation of thermal batteries of this work. In this project, different current densities were applied in a range from 7.5 mA/cm<sup>2</sup> to 75 mA/cm<sup>2</sup> in order to investigate the performance and the resulting discharge profiles.

## **3.3 Preparation of Anode and Electrolyte materials**

### **3.3.1 Anode material Li<sub>13</sub>Si<sub>4</sub>**

The anode material Li<sub>13</sub>Si<sub>4</sub> (Lithium Rockwood) was selected in this work as it was described in Chapter 2.1. Therefore, the anode powder Li<sub>13</sub>Si<sub>4</sub> was tested by PXRD as shown in Figure 3.7 to ensure no impurities are formed during storage. Li<sub>13</sub>Si<sub>4</sub> crystallises in primitive orthorhombic *Pbam* space group with unit cell parameters ( $a = 7.9723 \text{ \AA}$ ,  $b = 15.1426 \text{ \AA}$  and  $c = 4.4495 \text{ \AA}$ ). There are no impurities and the resulting diffraction pattern with the red line corresponds to a single phase Li<sub>13</sub>Si<sub>4</sub>.



**Figure 3.7.** PXRD data of  $\text{Li}_{13}\text{Si}_4$  compared to the simulated diffraction pattern of  $\text{Li}_{13}\text{Si}_4$  using the published crystallographic model [22] (black line)

The anode electrode (75 wt %  $\text{Li}_{13}\text{Si}_4$  – 25 wt % LiCl-KCl) was tested also by PXRD after discharge at 500 °C as shown in Figure 3.8 to investigate the products of the electrochemical mechanism. Figure 3.8 shows that the electrochemical result is a cubic phase  $Fd\bar{3}m$  of Si with unit cell parameter ( $a = 5.423(8)$  Å). This means that Li ions are transferred to the cathode electrode and the electrochemical process is completed. There are also some peaks of  $\text{SiO}_2$ . The morphology and the elemental analysis of the anode electrode was tested by SEM/EDX as shown in Figure 3.9. The elemental analysis confirms Si  $66 \pm 1$  at % as the expected.

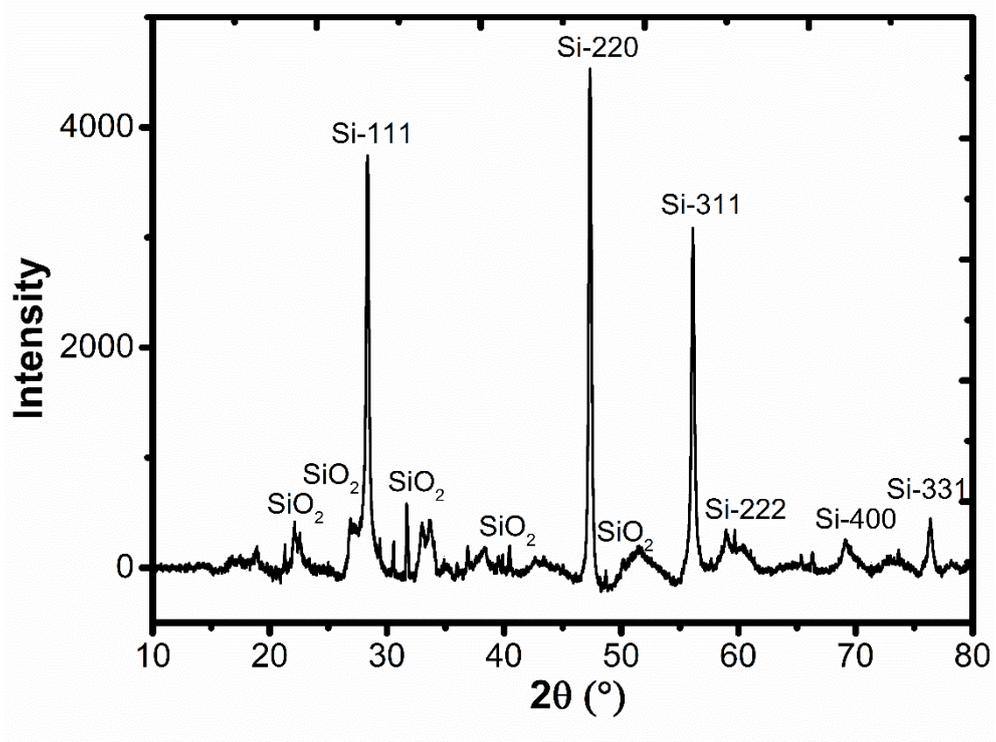


Figure 3.8. PXRD data of  $\text{Li}_{13}\text{Si}_4$  (anode electrode) after discharge at 500 °C

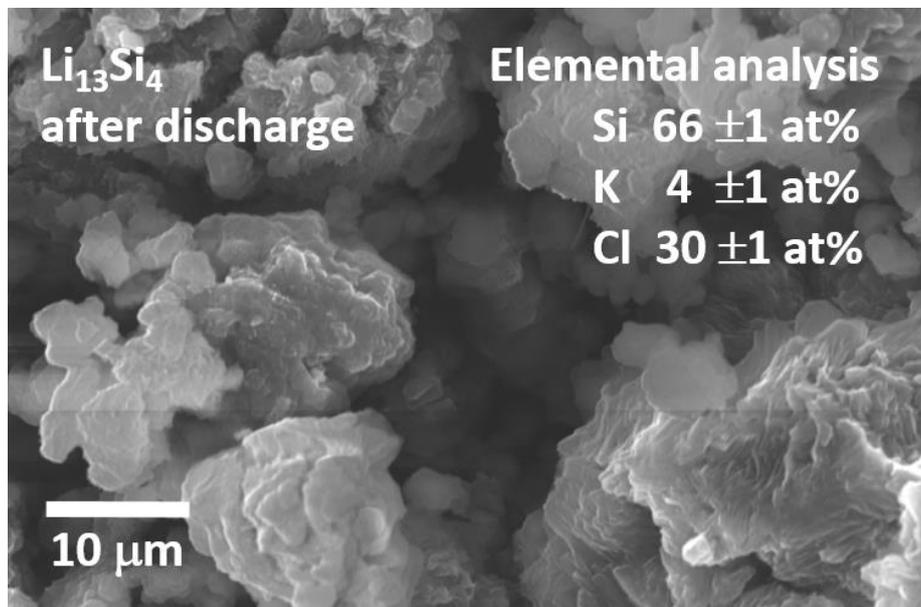
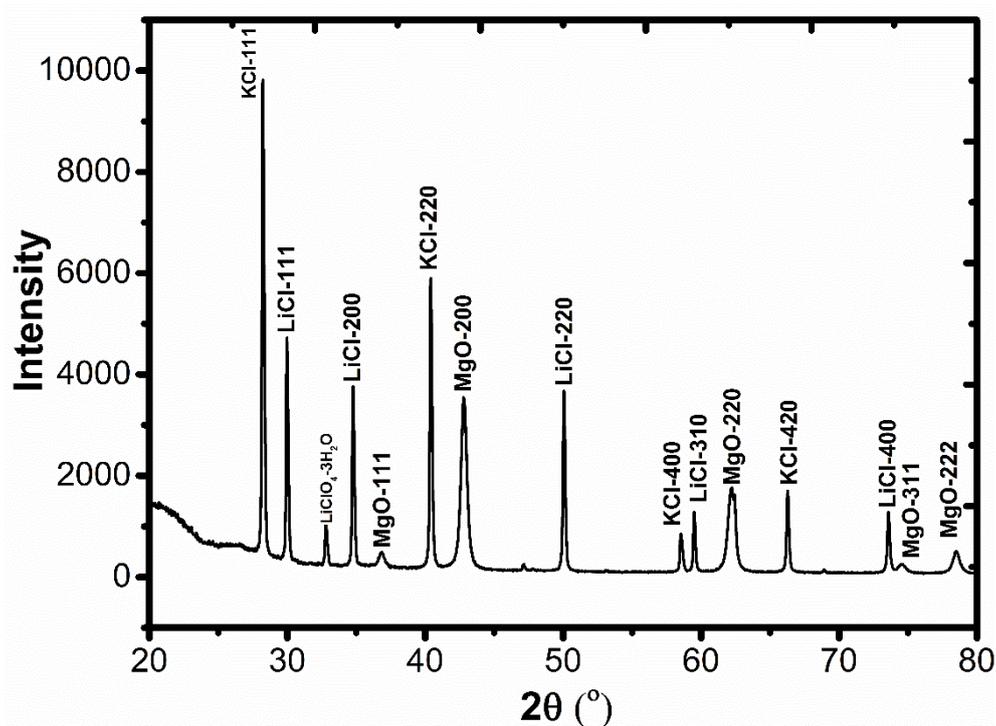


Figure 3.9. SEM image of  $\text{Li}_{13}\text{Si}_4$  (anode electrode) after discharge at 500 °C

### 3.3.2 Electrolyte material LiCl-KCl

In our experiments the separator pellet between anode/cathode electrodes is a mixture of a halide eutectic, along with a binder. The electrolyte material LiCl-KCl eutectic (Sigma Aldrich, 99.99%, LiCl 44.8 wt% - 55.2 wt% KCl) and MgO as binder were selected as were described in Chapter 2.2. The MgO powder is heated up to 650 °C overnight in a muffle furnace to remove any moisture and is transferred immediately to an argon glove box to cool over another night. 11 g of LiCl - KCl eutectic and 9 g of MgO (45 wt% MgO - 55 wt% LiCl-KCl eutectic mixture) are placed into a zirconia milling pot along with zirconia milling balls (5 mm) for 4 hours at 300 rpm in order to create a homogeneous mixture of the separator. For the ball milling, a Fritsch Pulverisette planetary ball mill was used. Figure 3.10 shows the PXRD data of 45 wt% MgO - 55 wt% LiCl-KCl eutectic mixture after milling.



**Figure 3.10.** PXRD data at room temperature of 45 wt% MgO - 55 wt% LiCl-KCl eutectic

### 3.4 Thermal cell fabrication and electrochemical testing

The most important point for the testing of batteries is that batteries have to be completely free of moisture both during storage and electrochemical testing. “Swagelok” cells are used as they are the most flexible and efficient systems for electrochemical studies of batteries as shown in Figures 3.11 and 3.12. Another important issue is the mechanical pressure inside the “Swagelok” cell. In thermal batteries, the most suitable pressure for a LiCl-KCl electrolyte with a minimum 35 wt% MgO separator is  $1.05 \text{ kg cm}^{-2}$  [23]. This pressure is achieved in our “Swagelok” cells by springs that are manufactured from Inconel X750 by Skegness Springs Ltd as shown in Figure 3.12.



**Figure 3.11.** External part of “Swagelok” cell for electrochemical measurements



**Figure 3.12.** Internal parts of “Swagelok” cell for electrochemical measurements

All thermal batteries were assembled in an argon-filled glove box. Fabrication of the composite cathode pellets for high temperature electrochemical investigation was made by mixing 75 wt%  $ZrS_3$ ,  $CoNi_2S_4$ ,  $NiCo_2S_4$ ,  $KNiCl_3$ ,  $Li_2MnCl_4$ ,  $Li_6VCl_8$ ,  $NiCl_2$ ,  $CoCl_2$ ,  $CuF_2$  or  $PbF_2$  and 25 wt% Super P Carbon. 45 wt% MgO and 55 wt% LiCl-KCl eutectic (Sigma Aldrich, 99.99%, LiCl 44.8 wt% - 55.2 wt% KCl) were ball milled under argon in order to make the separator/electrolyte. The anode was made by mixing 75 wt%  $Li_{13}Si_4$  (Lithium Rockwood) and 25 wt% LiCl-KCl eutectic. The cathode, the anode and the electrolyte/separator mixtures were individually pressed into pellets of diameter 13 mm at 5 tonnes for 3 minutes using an Atlas T15 automated press. The anode, the separator/electrolyte and the cathode pellets were held in place using an alumina cup to prevent movement and graphite foil was used as current collectors top and bottom. The alumina cup was chosen as it has little interaction with the electrolyte and was ordered from Ants Ceramics (India). It is re-useable and it was cleaned using dilute nitric acid. The cell assembly was placed in a “Swagelok” fitting allowing the measurements to be carried out sealed and heated

(during this procedure the electrolyte melts and the voltage starts to rise) in an electric furnace. Cell testing was carried out at a higher temperature than the melting point of the LiCl-KCl molten salt electrolyte. The electrochemical cells were tested at elevated temperature (ZrS<sub>3</sub>, CoNi<sub>2</sub>S<sub>4</sub>, NiCo<sub>2</sub>S<sub>4</sub>, Li<sub>6</sub>VCl<sub>8</sub>, NiCl<sub>2</sub>, CoCl<sub>2</sub>, CuF<sub>2</sub> and PbF<sub>2</sub> at 500 °C, KNiCl<sub>3</sub> at 425 °C, LiMnCl<sub>4</sub> at 400 °C) and were investigated electrochemically by a Maccor battery tester Model 5300 as shown in Figure 3.13, by galvanostatic discharge and lastly, by the galvanostatic intermittent titration technique (GITT).



**Figure 3.13.** Maccor battery tester Model 5300

The experimental capacity of cathodes was calculated using the Maccor software and then, this was converted to  $x$ , the moles of lithium ions per moles of formula unit.

For example, the experimental capacity of ZrS<sub>3</sub> by Maccor software was 0.03547 Ah. This number was multiplied by 3600 sec to convert in 127.692 Coulombs. Then 127.692 Coulombs were converted in  $7.97 \times 10^{20}$  electrons as it is known that 1 Coulomb is  $6.24 \times 10^{18}$  electrons. Then  $7.97 \times 10^{20}$  electrons were converted in 0.00132 moles of Li<sup>+</sup> by

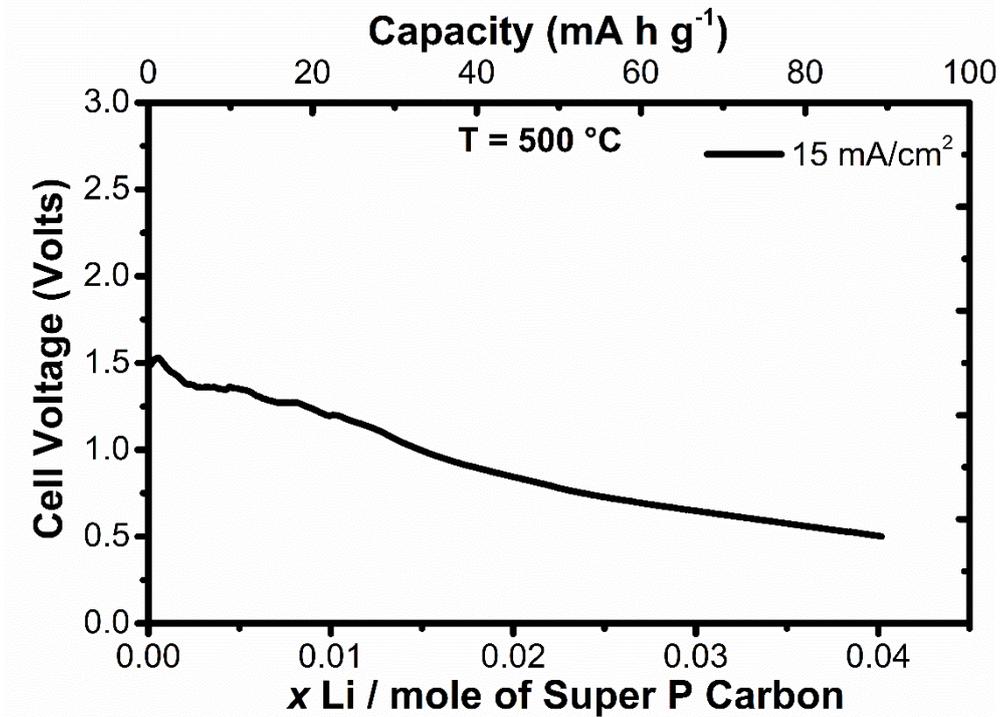
being divided by Avogadro number  $6.02 \times 10^{23} \text{ mol}^{-1}$ . Finally, the  $x$  number equals to 2.48, was calculated by dividing 0.00132 moles of  $\text{Li}^+$  by 0.00534 moles of  $\text{ZrS}_3$  active electrode.

All voltages are reported compared to the anode as a voltage reference *i.e.* all voltages are vs  $\text{Li}_{13}\text{Si}_4$ .

### **3.5 The Effect of Super P Carbon in Li thermal batteries at 500 °C**

Super P Carbon is used in lithium ion batteries and mixed with active cathodes (20 – 25 wt %) to increase the electronic conductivity. Some other carbon materials, such as carbon nanotubes, graphene, and graphene oxide, are used electrodes as electrically conductive additives, structural stabilizers, reactive precursors, catalysts/promoters and provide a significant enhancement in the electrical energy storage performance of the batteries [24-27].

It is known that Super P Carbon exhibits a voltage plateau of 0.5 V against Li metal at room temperature [28] where the lithium ions insert into the structure. In order to investigate the electrochemical reaction of Super P Carbon in Li thermal batteries at 500 °C, a thermal cell consisted of 0.15 g of  $\text{Li}_{13}\text{Si}_4$  and 0.05 g of LiCl - KCl electrolyte as an anode, 0.2 g of 45 wt% MgO - 55 wt% LiCl - KCl eutectic mixture as an electrolyte and 0.2 g of Super P Carbon as a cathode, was discharged at a current density of 15 mA/cm<sup>2</sup> at 500 °C as shown in Figure 3.14. According to the electrochemical results, Super P Carbon exhibits a capacity of around 90 mA h g<sup>-1</sup> equivalent to 0.04 Li per mole of Super P Carbon. Also, a voltage plateau of 0.5 V against  $\text{Li}_{13}\text{Si}_4$  is obtained. In this work the amount of Super P Carbon that is mixed with all the active cathodes is 0.05 g (25 wt %). This amount of Super P Carbon corresponds to around 20 mA h g<sup>-1</sup> of all capacities in our experiments. In all the experiments, Super P Carbon does not look like it reacts with the LiCl-KCl electrolyte during discharge mechanism or that it is oxidized. However, as shown in Figure 3.14, when the cut-off voltage is set to a value of 0.5 V, then a short plateau for Super P Carbon against  $\text{Li}_{13}\text{Si}_4$  is obtained.



**Figure 3.14.** Galvanostatic discharge curve of Super P Carbon at a current density of 15 mA/cm<sup>2</sup> at 500 °C

### 3.6 References

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## **Chapter 4: Transition-Metal Sulfide Cathodes based on Nickel and Cobalt**

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## Chapter 4: Transition Metal Sulfide Cathodes based on Nickel and Cobalt

### 4.1 Material Characterisation of $\text{CoNi}_2\text{S}_4$ and $\text{NiCo}_2\text{S}_4$

The synthesis of  $\text{CoNi}_2\text{S}_4$  has previously been reported by Knop and Huang and their solid state synthesis involves multiple firings at temperatures from 500 °C to 600 °C for a total of two months. The long duration of this reaction is not practical, so it was necessary to explore a variety of synthetic conditions with the aim to synthesise this material in a shorter time frame. The synthetic conditions explored are given in Table 4.1 and corresponding diffraction patterns are shown in Figure 4.1 [1].

**Table 4.1.** Experimental conditions for the synthesis of  $\text{CoNi}_2\text{S}_4$  [1]

Experiment Number	1 <sup>st</sup> Firing	Ball milling	2 <sup>nd</sup> Firing	Ball milling	3 <sup>rd</sup> Firing	Single phase
Experiment 1	400 °C for 24 hours	1 hour in air with acetone	400 °C for 168 hours	1 hour in air with acetone	400 °C for 24 hours	No
Experiment 2	480 °C for 24 hours	1 hour in argon	480 °C for 168 hours	1 hour in argon	480 °C for 24 hours	No
Experiment 3	480 °C for 24 hours	Grinding in mortar and pestle in glove box	480 °C for 168 hours	Grinding in mortar and pestle in glove box	480 °C for 24 hours	No
Experiment 4	500 °C for 24 hours	1 hour in air with acetone	500 °C for 168 hours	1 hour in air with acetone	500 °C for 24 hours	No
Experiment 5	550 °C for 34 hours	4 hours in argon	550 °C for 156 hours	No	No	Yes

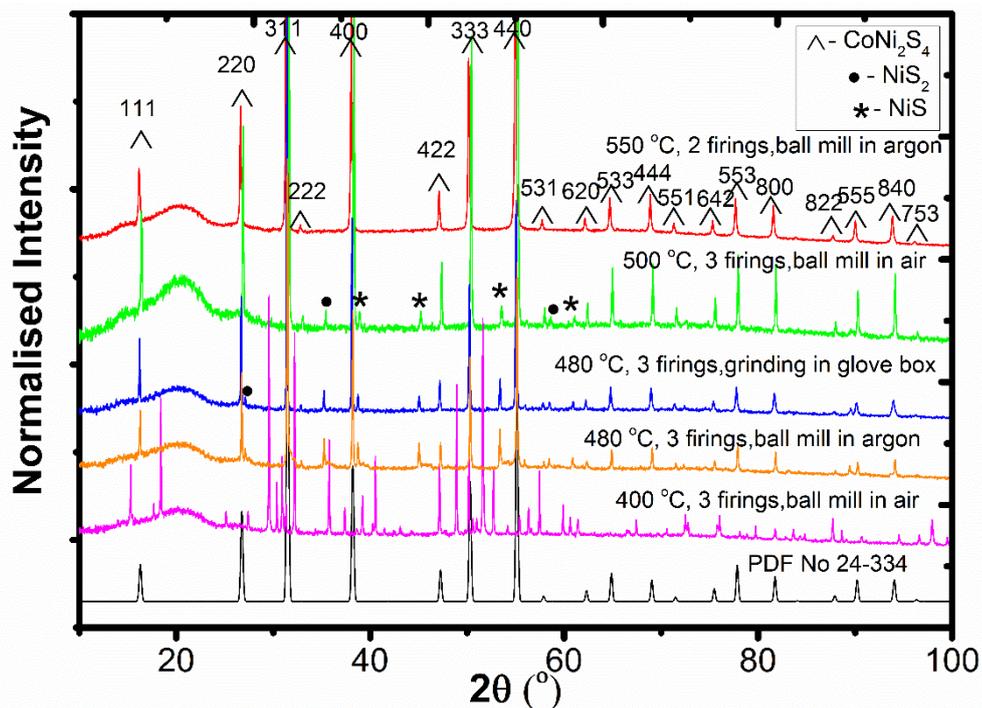
## Chapter 4: Transition Metal Sulfide Cathodes based on Nickel and Cobalt

The first experiment was carried out at 400 °C. This involved three firing steps and two ball milling steps as outlined in Table 4.1 but this did not yield a phase pure sample. Impurities were an amount of NiS and NiS<sub>2</sub> as marked in Figure 4.1. NiS impurity crystallises in a hexagonal structure with cell parameters ( $a = 3.396 \text{ \AA}$ ,  $c = 5.412 \text{ \AA}$ ) and space group  $P6_3/mmc$  compared to literature values ( $a = 3.451 \text{ \AA}$ ,  $c = 5.394 \text{ \AA}$ ) [2]. NiS<sub>2</sub> impurity crystallises in a cubic structure with a cell parameter ( $a = 5.641 \text{ \AA}$ ) and space group  $Pa\bar{3}$  compared to literature value ( $a = 5.669 \text{ \AA}$ ) [3].

The second experiment was carried out at 480 °C. CoNi<sub>2</sub>S<sub>4</sub> was fired three times and ball milled twice in argon and was still not a single phase. A further reaction was carried out at 480 °C replacing the ball milling step. CoNi<sub>2</sub>S<sub>4</sub> was fired three times with hand grinding in a mortar and pestle in an argon glove box but the product was still not single phase.

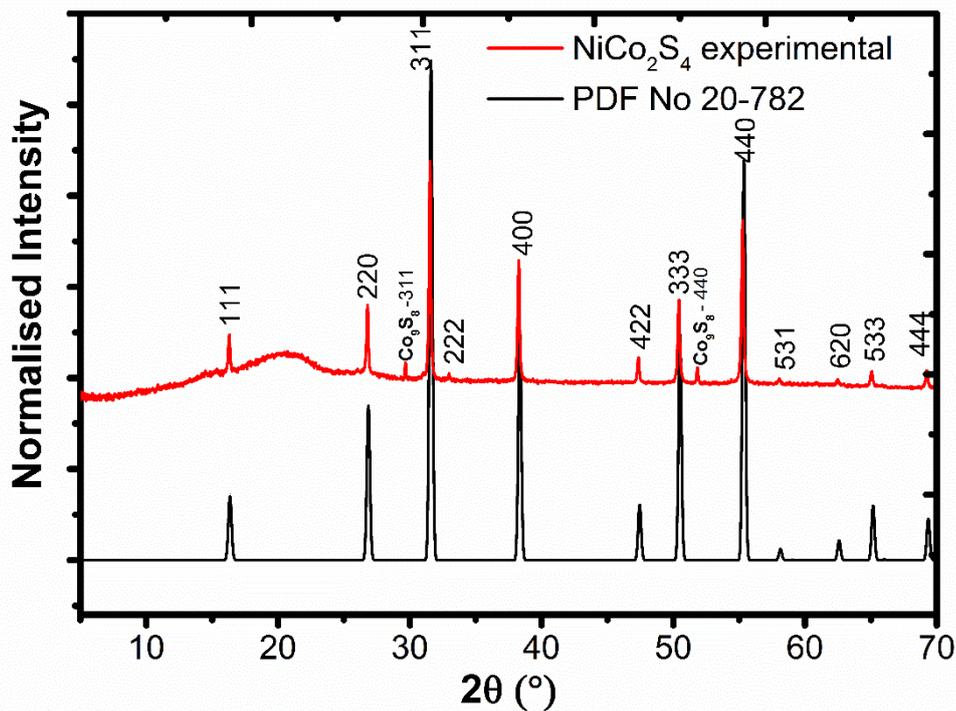
The fourth experiment was carried out at 500 °C, CoNi<sub>2</sub>S<sub>4</sub> was fired three times and ball milled twice and the phase purity was comparable to the reaction carried out at 480 °C. Increasing the temperature to 550 °C resulted in a phase pure sample. The final conditions were explored, the best synthetic conditions for the synthesis of CoNi<sub>2</sub>S<sub>4</sub> were found to be synthesizing the sample in 8 days with 2 firing steps (at temperature of 550 °C) by using ball milling in argon as an intermediate step.

The reader can notice that the reactions carried out at 480 °C show an improved phase purity with respect to the reactions carried out at 400 °C as shown in Figure 4.1. All peaks in the diffraction pattern (red line) could be assigned to CoNi<sub>2</sub>S<sub>4</sub> as a single phase with a cell parameter ( $a = 9.4239(8) \text{ \AA}$ ) and space group  $Fd\bar{3}m$  [1].



**Figure 4.1.** PXRD data of  $\text{CoNi}_2\text{S}_4$  (using different synthetic conditions) compared to the simulated diffraction pattern using the published crystallographic model [4] (black line). The broad peak at around  $20^\circ$  is from the protective air sensitive film which is used during data collection.  $\text{NiS}$  and  $\text{NiS}_2$  impurities are marked [1]

Once the best conditions were found for the synthesis of  $\text{CoNi}_2\text{S}_4$ ,  $\text{NiCo}_2\text{S}_4$  was synthesised using the same conditions. The PXRD pattern is shown in Figure 4.2. The experimental pattern (red line) in Figure 4.2 shows that the main phase is  $\text{NiCo}_2\text{S}_4$  with cell parameter ( $a = 9.3883(8) \text{ \AA}$ ) and space group  $Fd\bar{3}m$ . A small amount of  $\text{Co}_9\text{S}_8$  impurity with cell parameter ( $a = 9.962(8) \text{ \AA}$ ) and space group  $Fm\bar{3}m$  was present in the diffraction pattern. Further optimisation of the synthetic conditions should be explored for the synthesis of pure  $\text{NiCo}_2\text{S}_4$ .



**Figure 4.2.** PXRD data of  $\text{NiCo}_2\text{S}_4$  (red line) compared to the simulated diffraction pattern using the published crystallographic model [5] (black line). A  $\text{Co}_9\text{S}_8$  impurity is marked

The morphology and the shape of the crystallites of  $\text{CoNi}_2\text{S}_4$  and  $\text{NiCo}_2\text{S}_4$  were investigated by SEM and are shown in Figures 4.3 and 4.4. The elemental composition was also analyzed by EDX. The size of the particles ranges from 1 to 10  $\mu\text{m}$  and the shape of crystallites corresponds to the shape of the spinel structure which forms octahedra [6, 7].

EDX analysis confirms the elemental composition of  $\text{CoNi}_2\text{S}_4$  and of  $\text{NiCo}_2\text{S}_4$  as the expected and the data, compared with theoretical values, are given in Table 4.2.

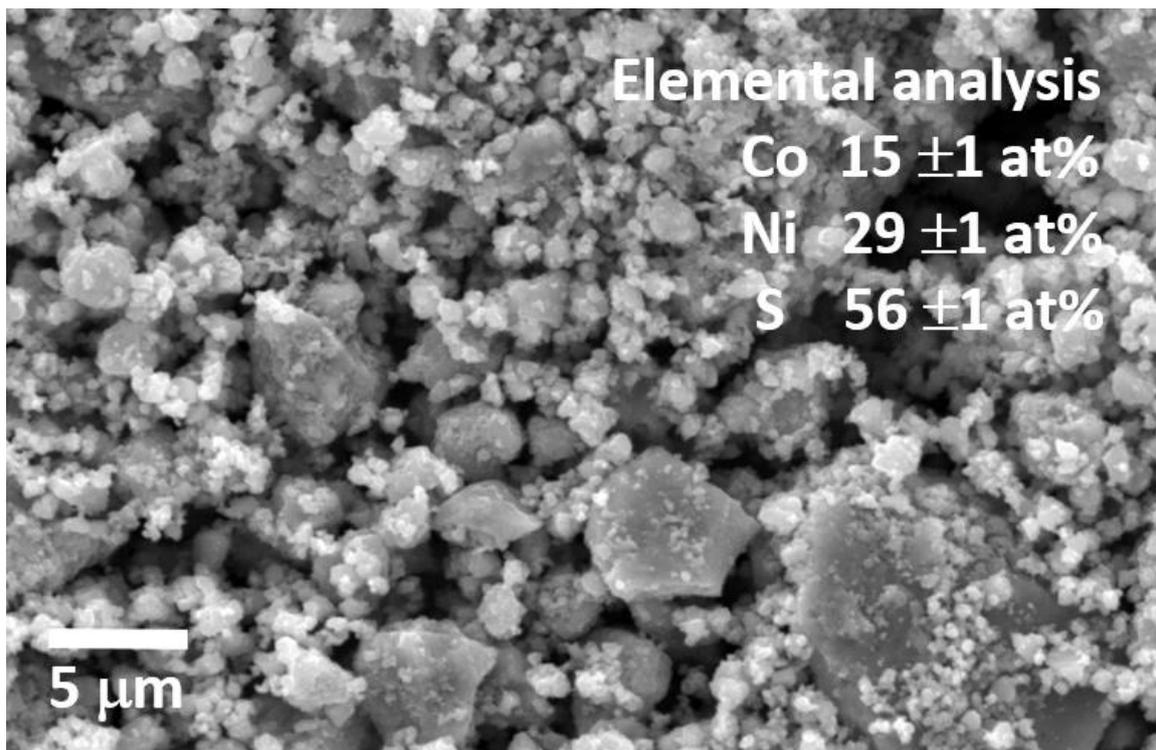
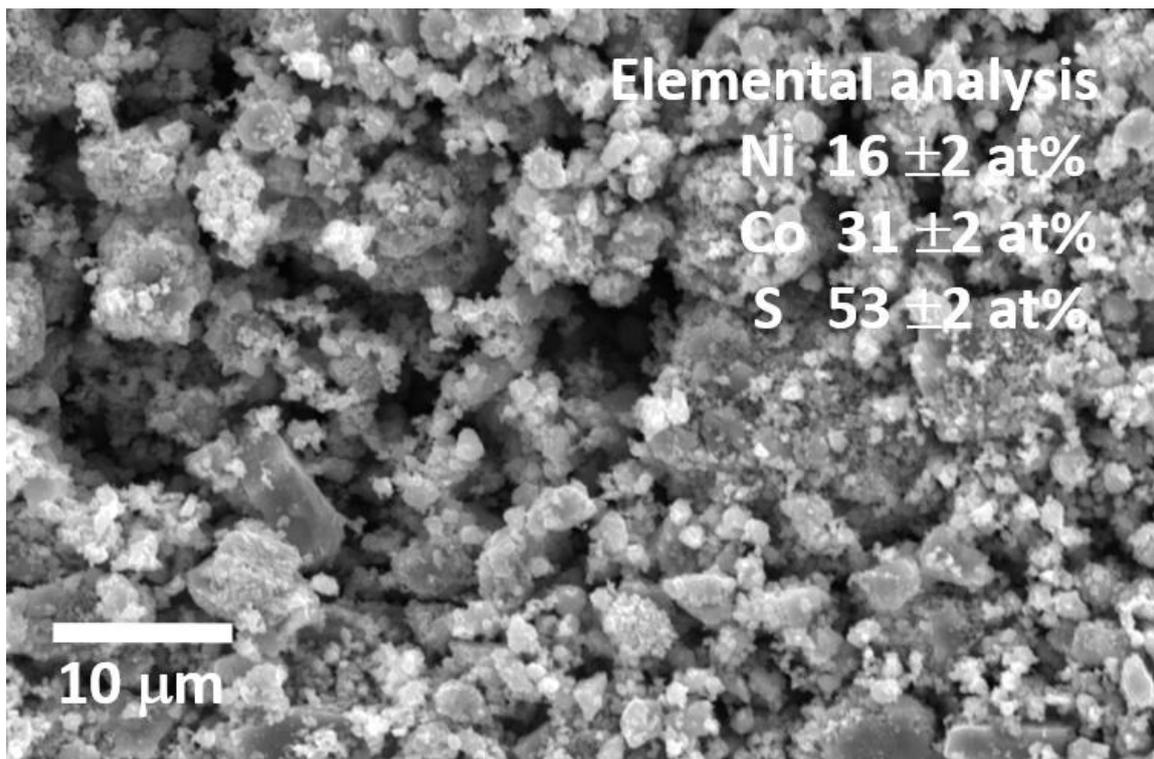


Figure 4.3. SEM image of CoNi<sub>2</sub>S<sub>4</sub> [1]

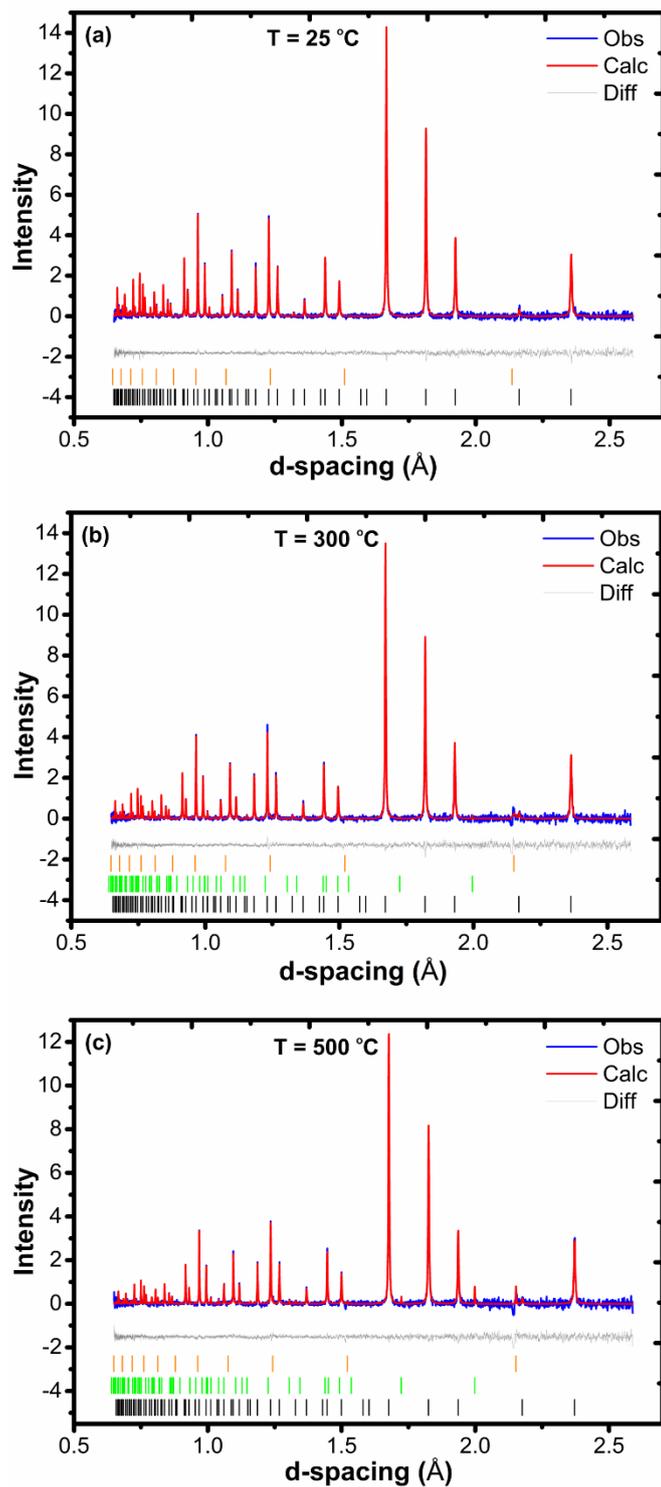
Table 4.2. EDX analysis of CoNi<sub>2</sub>S<sub>4</sub> and NiCo<sub>2</sub>S<sub>4</sub>

Elements	Experimental	Theoretical
<b>CoNi<sub>2</sub>S<sub>4</sub></b>		
Co	15 ±1 at%	14 at%
Ni	29 ±1 at%	29 at%
S	56 ±1 at%	57 at%
<b>NiCo<sub>2</sub>S<sub>4</sub></b>		
Ni	16 ±2 at%	14 at%
Co	31 ±2 at%	29 at%
S	53 ±2 at%	57 at%



**Figure 4.4.** SEM image of NiCo<sub>2</sub>S<sub>4</sub>

As Co<sup>2+</sup> and Ni<sup>3+</sup> are isoelectronic, it is not possible to distinguish between the possible Co and Ni ordering using powder X-ray diffraction. Powder neutron diffraction is the ideal tool to study such a material given the difference in neutron scattering lengths of Co and Ni (2.49 and 10.30 fm, respectively) [8]. In order to explore the thermal stability of CoNi<sub>2</sub>S<sub>4</sub> at elevated temperature and to probe cation (dis)ordering, variable temperature powder neutron diffraction data were collected at temperatures in the range from 25 °C - 500 °C. The Rietveld fits to powder neutron diffraction data, at 25 °C, 300 °C and 500 °C, are shown in Figure 4.5 [1].



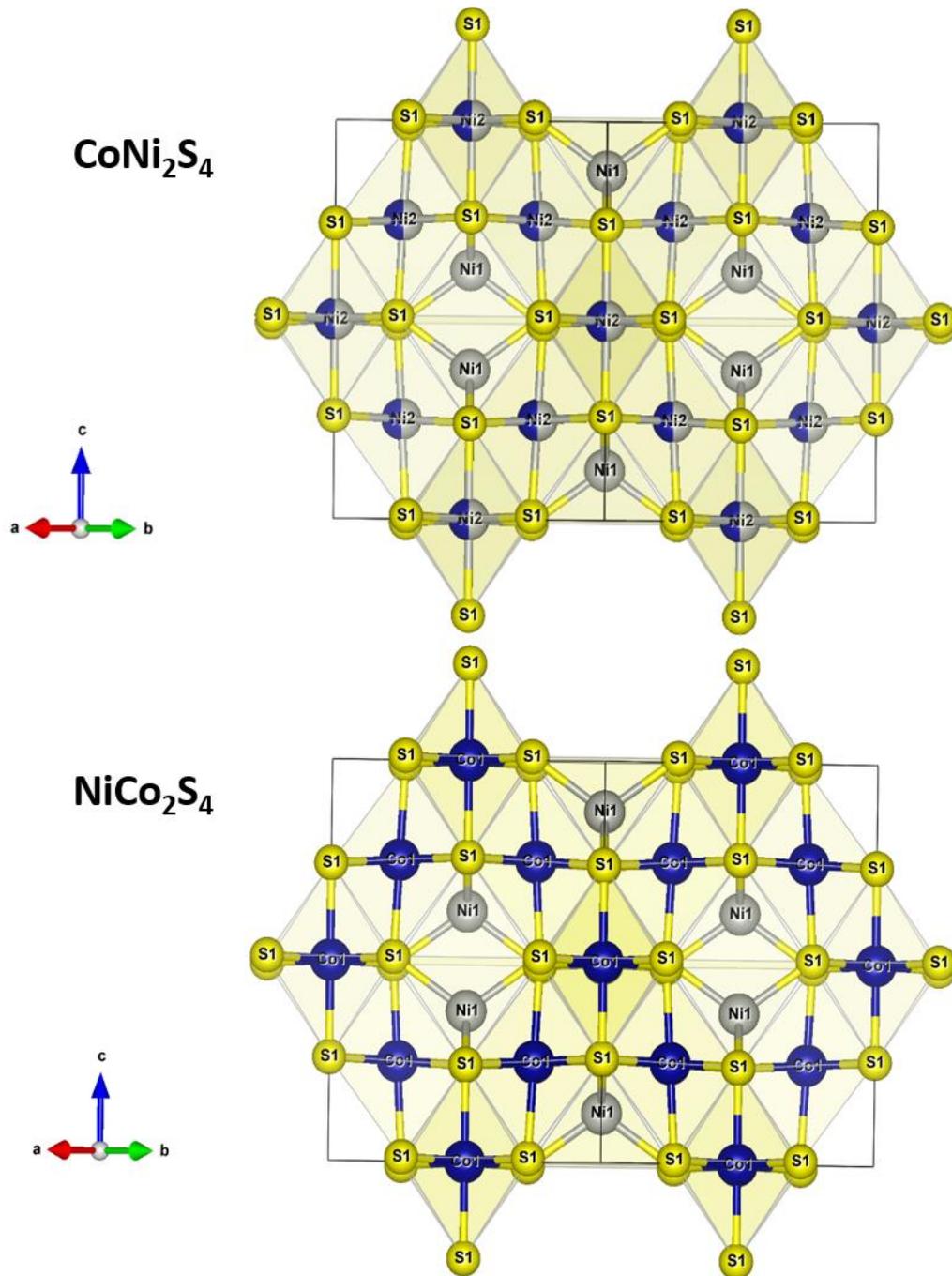
**Figure 4.5.** Rietveld fit to powder neutron diffraction data using an inverse spinel model for  $\text{CoNi}_2\text{S}_4$  at  $25\text{ }^\circ\text{C}$  (a), at  $300\text{ }^\circ\text{C}$  (b) and at  $500\text{ }^\circ\text{C}$  (c). (Black tick marks are  $\text{CoNi}_2\text{S}_4$ , green tick marks are vanadium and orange tick marks are  $\text{Ni}_{1-x}\text{Co}_x\text{S}$ ) [1]

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Refinement of the  $\text{CoNi}_2\text{S}_4$  structural model was carried out in the 25 °C to 500 °C, range. Cell parameters, atomic coordinates for sulfur, cation occupancies, an overall isotropic temperature parameter for the cation sites, an isotropic temperature parameter for the sulfur site, 18 background parameters and a scale factor were refined.

In initial refinements, cation ordering on the both the 8a and 16d sites was tested across the full temperature range. Refinements of the occupancy of the 8a site found that this site was site fully occupied by nickel and in subsequent refinements the occupancy of the 8a site was fixed to 100 % nickel. At room temperature, Rietveld refinement confirms that  $\text{CoNi}_2\text{S}_4$  adopts an inverse spinel structure as shown in Figure 4.6.

Thio-spinels with the general formula  $\text{A}^{2+}\text{B}^{3+}_2\text{S}^{2-}_4$  have the sulfur anions arranged in a cubic close-packed lattice and the  $\text{A}^{2+}$  and  $\text{B}^{3+}$  cations occupy the octahedral and tetrahedral sites in the lattice. In the  $\text{NiCo}_2\text{S}_4$  structure, the  $\text{Co}^{3+}$  cations occupy half of the octahedral holes, while the  $\text{Ni}^{2+}$  cations occupy one-eighth of the tetrahedral holes. In the  $\text{CoNi}_2\text{S}_4$  structure, the Co cations and half of the Ni cations occupy octahedral sites, while the remaining Ni cations occupy tetrahedral sites as shown in Figure 4.6 [1].



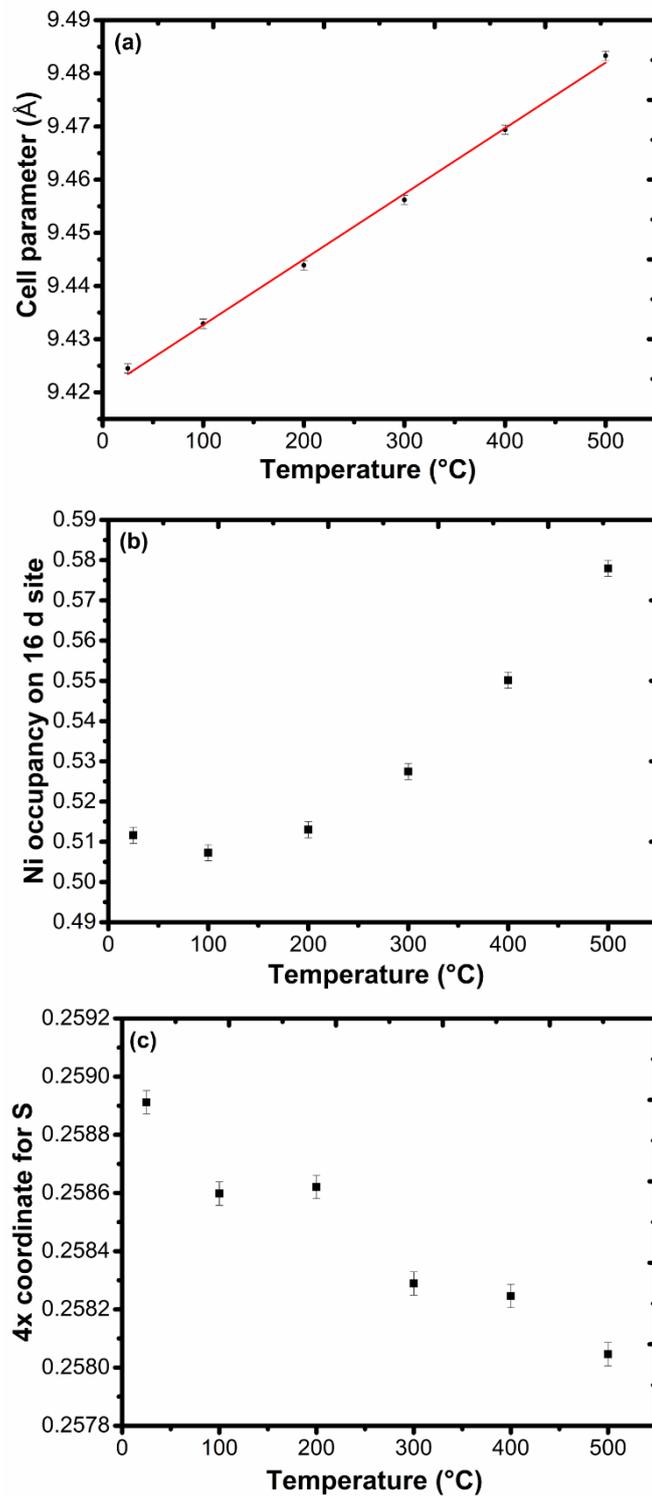
**Figure 4.6.** Crystal structure of an inverse spinel  $\text{CoNi}_2\text{S}_4$  compared to normal spinel  $\text{NiCo}_2\text{S}_4$ . Yellow atoms are sulfur, gray atoms are nickel and blue atoms are cobalt

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Refinement of cation occupancies retains an essentially ordered distribution of cobalt and nickel with no evidence of cation anti-site disorder or non-stoichiometry on the 16d site. This ordering pattern is retained up to 200 °C, but above this temperature, there is a gradual increase of nickel on the 16d site with increasing temperature, as shown in Figure 4.7. This was accompanied by a small decrease in the atomic coordinates of sulfur as these moved closer to ideal 0.25 value. As the S atom is on a 32e site (all the three coordinates are equal to  $x$ ) then we need to specify only one parameter for the sulfur coordinate. At 500 °C, a small amount of secondary phase can be observed in the diffraction pattern (Figure 4.5) and this can be attributed to a “Ni<sub>1-x</sub>Co<sub>x</sub>S”  $P6_3/mmc$  phase ( $a = 3.4468(2)$  Å,  $c = 5.3787(6)$  Å). This suggests some sulfur loss under the vacuum conditions of this experiment. The cell parameter of the unit cell increases as the temperature increases as shown in Figure 4.7. All the refined structural parameters of CoNi<sub>2</sub>S<sub>4</sub> are presented in Table 4.3 [1].

**Table 4.3.** Selected structural parameters of CoNi<sub>2</sub>S<sub>4</sub> [1]

Temperature	25 °C	300 °C	500 °C
R <sub>wp</sub> %	2.25	2.15	2.01
Chi <sup>2</sup>	2.114	1.834	1.737
Unit cell $a$ / (Å)	9.42448(3)	9.45626(4)	9.48343(4)
Ni occupancy on 16d site	0.511(5)	0.527(6)	0.578(6)
( $x,x,x$ ) 32e site (for sulfur)	0.2589(13)	0.2582(15)	0.2580(17)
Ni (8a)-S (Å)	2.186(2)	2.183(2)	2.185(3)
Ni/Co (16d)-S (Å)	2.2752(11)	2.2884(13)	2.2971(16)



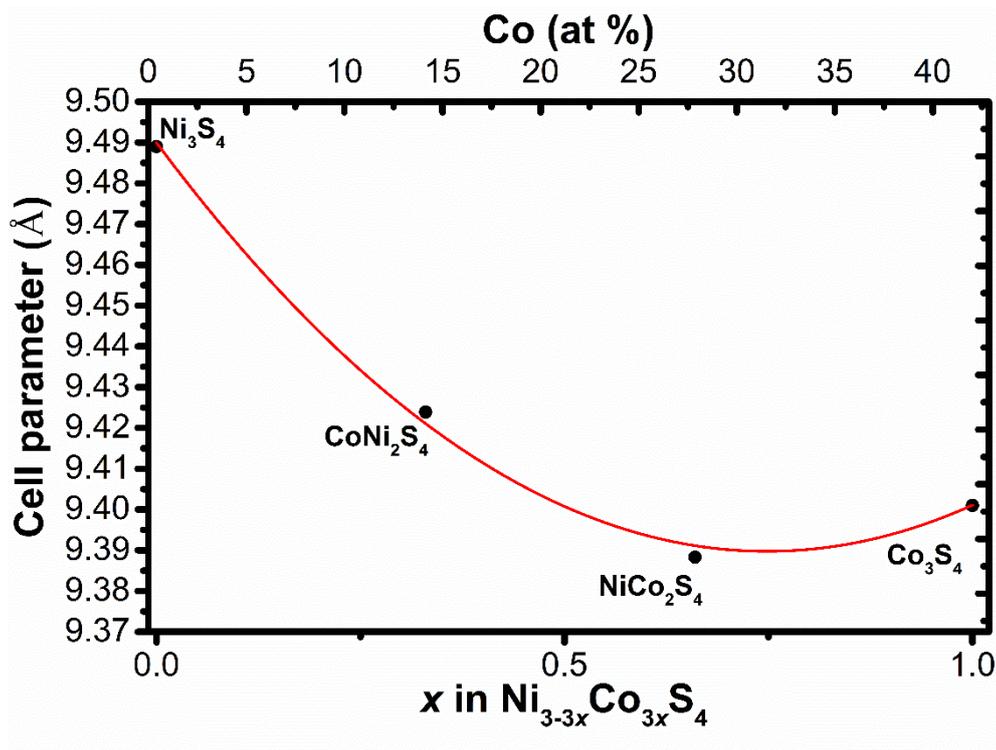
**Figure 4.7.** Unit cell parameter of  $\text{CoNi}_2\text{S}_4$  vs temperature from 25 °C up to 500 °C (a), Ni occupancy vs temperature (b) and '4x' coordinate (for sulfur) vs temperature (c) [1]

## Chapter 4: Transition Metal Sulfide Cathodes based on Nickel and Cobalt

All the spinels  $\text{Ni}_3\text{S}_4$  ( $a = 9.489 \text{ \AA}$ ) [9],  $\text{CoNi}_2\text{S}_4$  ( $a = 9.4239(8) \text{ \AA}$ ),  $\text{NiCo}_2\text{S}_4$  ( $a = 9.3883(8) \text{ \AA}$ ) and  $\text{Co}_3\text{S}_4$  ( $a = 9.401 \text{ \AA}$ ) [10] crystallise in a cubic structure with space group  $Fd\bar{3}m$ . However the unit cell differs as the amount of cobalt (Co) metal is increasing as shown in Figure 4.8. The atomic radius of Co metal is higher (152 pm) compared to the atomic radius of Ni metal (149 pm) [11].

However in  $\text{Ni}_3\text{S}_4$ , low spin  $\text{Ni}^{3+}$  cations occupy octahedral sites with ionic radius 56 pm and high spin  $\text{Ni}^{2+}$  cations occupy tetrahedral sites with ionic radius 55 pm [12]. The M – S distance (where M is transition metal) in octahedral sites is  $2.289(5) \text{ \AA}$  and in tetrahedral sites is  $2.204(5) \text{ \AA}$ . This results to the largest unit cell of all the other spinels. In  $\text{CoNi}_2\text{S}_4$ , high spin  $\text{Ni}^{2+}$  cations occupy tetrahedral sites with ionic radius 55 pm and low spin  $\text{Ni}^{3+}$  cations occupy octahedral sites with ionic radius 56 pm. The low spin  $\text{Co}^{3+}$  cations occupy octahedral sites with ionic radius 54.5 pm [12]. The M – S distance in octahedral sites is  $2.273(3) \text{ \AA}$  and in tetrahedral sites is  $2.189(3) \text{ \AA}$ . This results to a smaller unit cell than  $\text{Ni}_3\text{S}_4$ . In  $\text{NiCo}_2\text{S}_4$ , low spin  $\text{Co}^{3+}$  cations occupy octahedral sites with ionic radius 54.5 pm and high spin  $\text{Ni}^{2+}$  cations occupy tetrahedral sites with ionic radius 55 pm. M – S distance in octahedral sites is  $2.265(3) \text{ \AA}$  and in tetrahedral sites is  $2.181(3) \text{ \AA}$ . This results to a smaller unit cell than  $\text{CoNi}_2\text{S}_4$ . Finally, in  $\text{Co}_3\text{S}_4$ , low spin  $\text{Co}^{3+}$  cations occupy octahedral sites with ionic radius 54.5 pm and high spin  $\text{Co}^{2+}$  cations occupy tetrahedral sites with ionic radius 58 pm [12]. M – S distance in octahedral sites is also  $2.268(5) \text{ \AA}$  and in tetrahedral sites is  $2.184(5) \text{ \AA}$ . This corresponds to a larger unit cell than  $\text{NiCo}_2\text{S}_4$ .

Experimental values M – S distances in both  $\text{CoNi}_2\text{S}_4$  and  $\text{NiCo}_2\text{S}_4$  are in agreement with the literature [4]. The low spin cation has a high preference to the octahedral sites and the high spin prefers the tetrahedral sites [4]. So as the low spin of  $\text{Ni}^{3+}$  cations exhibits higher ionic radius than the low spin of  $\text{Co}^{3+}$  cations in octahedral sites this suggests a bigger unit cell.



**Figure 4.8.** Unit cell parameters of the spinels Ni<sub>3</sub>S<sub>4</sub>, CoNi<sub>2</sub>S<sub>4</sub>, NiCo<sub>2</sub>S<sub>4</sub> and Co<sub>3</sub>S<sub>4</sub> vs cobalt (at %) or x in Ni<sub>3-3x</sub>Co<sub>3x</sub>S<sub>4</sub> formula

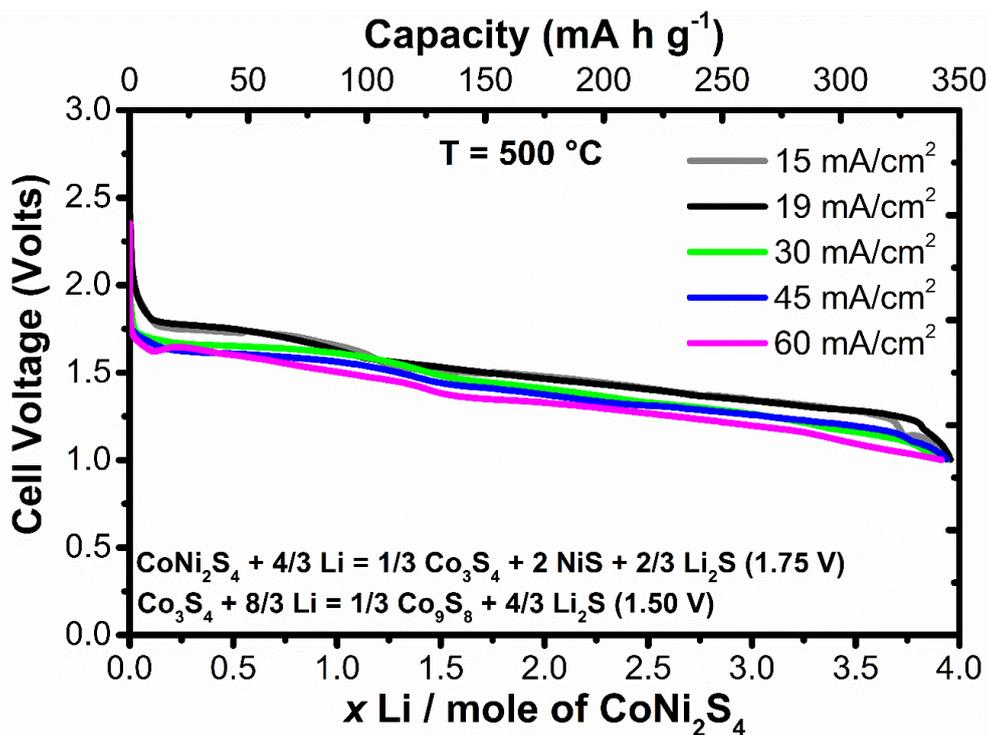
## 4.2 Electrochemical Investigation of CoNi<sub>2</sub>S<sub>4</sub> and NiCo<sub>2</sub>S<sub>4</sub>

CoNi<sub>2</sub>S<sub>4</sub> and NiCo<sub>2</sub>S<sub>4</sub> were investigated electrochemically by galvanostatic discharge and galvanostatic intermittent titration technique.

## Chapter 4: Transition Metal Sulfide Cathodes based on Nickel and Cobalt

Galvanostatic discharging of  $\text{CoNi}_2\text{S}_4$  was performed at current densities from 15 to 60  $\text{mA}/\text{cm}^2$  at 500 °C and the results are presented in Figure 4.9. The lower voltage cut-off for the measurement was 1 Volt. At current densities of 15 and 19  $\text{mA}/\text{cm}^2$ ,  $\text{CoNi}_2\text{S}_4$  exhibits a flat voltage plateau at 1.75 V for  $x = 1.33$  Li, and then a second plateau at 1.50 V for  $x = 2.66$  Li. A total capacity of 350  $\text{mA h g}^{-1}$  was achieved at both current densities. At higher current densities of 30, 45, and 60  $\text{mA}/\text{cm}^2$  the voltages of these plateau are lower by 50 mV and this is probably due to a higher cell resistance.

The amount of active anode (0.15 g) corresponds to 73 mA h for the discharge plateau from  $\text{Li}_{13}\text{Si}_4$  to  $\text{Li}_7\text{Si}_3$  which is 0.157 V vs Li metal. The measured capacity of  $\text{CoNi}_2\text{S}_4$  of the first discharge plateau is 17.50 mA h and of the second discharge plateau is 35 mA h. Total 52.5 mA h, which keeps the discharge as being performed against the 0.157 V vs Li metal plateau [1].

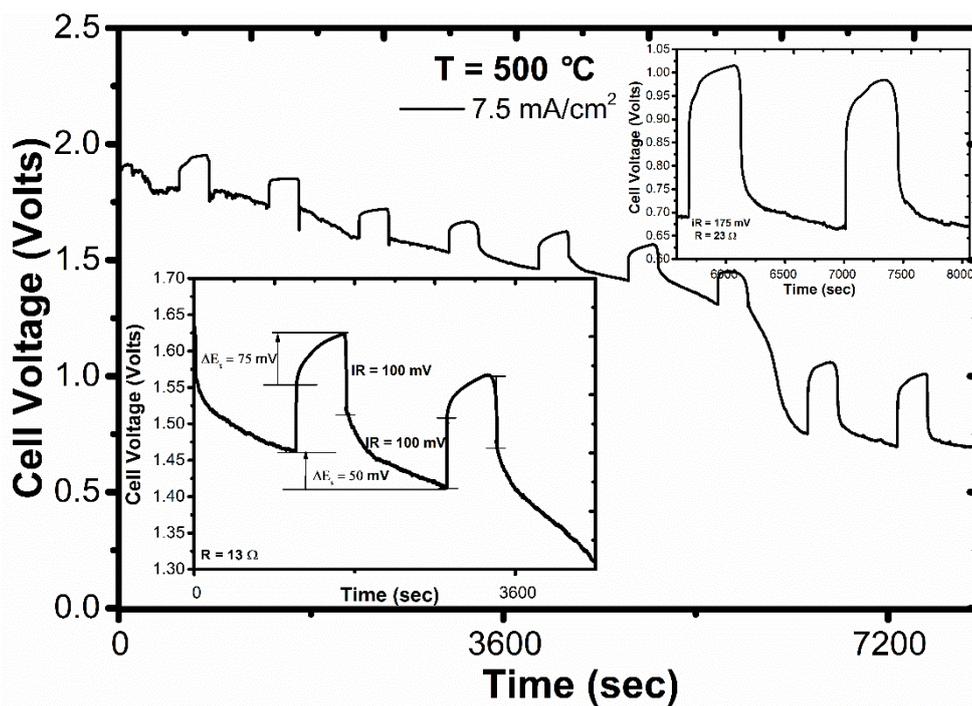


**Figure 4.9.** Galvanostatic discharge of  $\text{CoNi}_2\text{S}_4$  at current densities from 15 to 60  $\text{mA}/\text{cm}^2$  at 500 °C [1]

## Chapter 4: Transition Metal Sulfide Cathodes based on Nickel and Cobalt

The galvanostatic intermittent titration technique of  $\text{CoNi}_2\text{S}_4$  was performed at a current density of  $7.5 \text{ mA/cm}^2$  at  $500 \text{ }^\circ\text{C}$  and the results are presented in Figure 4.10. In this method the voltage of  $\text{CoNi}_2\text{S}_4$  drops between the pulse of current and the relaxation period until a voltage of  $0.5 \text{ V}$  is reached. The IR drop is  $100 \text{ mV}$  at the beginning of discharge and  $175 \text{ mV}$  at the end of the measurement, which indicates that the cell resistance is increasing during the reduction of the cathode, from a resistance of around  $13 \text{ } \Omega$  at the beginning of the measurement to around  $23 \text{ } \Omega$  after the cell discharge, which suggests that it is getting increasingly difficult to insert lithium ions into the structure of the cathode electrode.

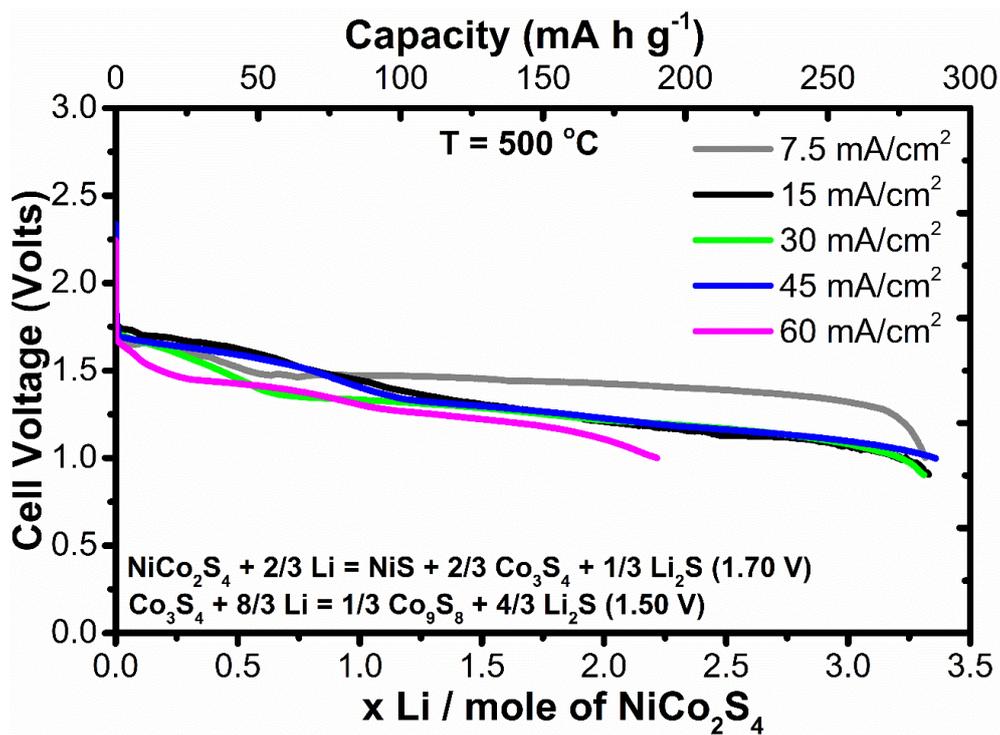
The chemical diffusion coefficient  $D = 9.18 \cdot 10^{-7} \text{ cm}^2 \text{ s}^{-1}$  for  $\text{CoNi}_2\text{S}_4$  can be calculated from equation [3.1] where  $n_m = 0.000656 \text{ (mol)}$ ,  $V_m = 63.06 \text{ (cm}^3 \text{ / mol)}$ ,  $\Delta E_s = 0.050 \text{ (V)}$  and  $\Delta E_t = 0.075 \text{ (V)}$ .



**Figure 4.10.** Galvanostatic intermittent titration technique of  $\text{CoNi}_2\text{S}_4$  at a current density of  $7.5 \text{ mA/cm}^2$  at  $500 \text{ }^\circ\text{C}$

## Chapter 4: Transition Metal Sulfide Cathodes based on Nickel and Cobalt

Galvanostatic discharging of  $\text{NiCo}_2\text{S}_4$  was performed at current densities from 7.5 to 60  $\text{mA}/\text{cm}^2$  at 500 °C and the results are presented in Figure 4.11. The voltage cut off for this measurement was 1 Volt. At a current density of 7.5  $\text{mA}/\text{cm}^2$ ,  $\text{NiCo}_2\text{S}_4$  exhibits a flat voltage plateau at 1.70 V for  $x = 0.66$  Li, and then a second plateau at 1.50 V for  $x = 2.66$  Li. A total capacity of 290  $\text{mA h g}^{-1}$  was achieved. At higher current densities of 15, 30, 45 and 60  $\text{mA}/\text{cm}^2$  the voltage of the second plateau is 50 mV lower and this is probably due to a higher cell resistance. The amount of active anode (0.15 g) corresponds to 73 mA h for the discharge plateau from  $\text{Li}_{13}\text{Si}_4$  to  $\text{Li}_7\text{Si}_3$  which is 0.157 V vs Li metal. The measured capacity of  $\text{NiCo}_2\text{S}_4$  of the first discharge plateau is 9 mA h and of the second discharge plateau is 35 mA h. Total 44 mA h, which keeps the discharge as being performed against the 0.157 V Li metal plateau.

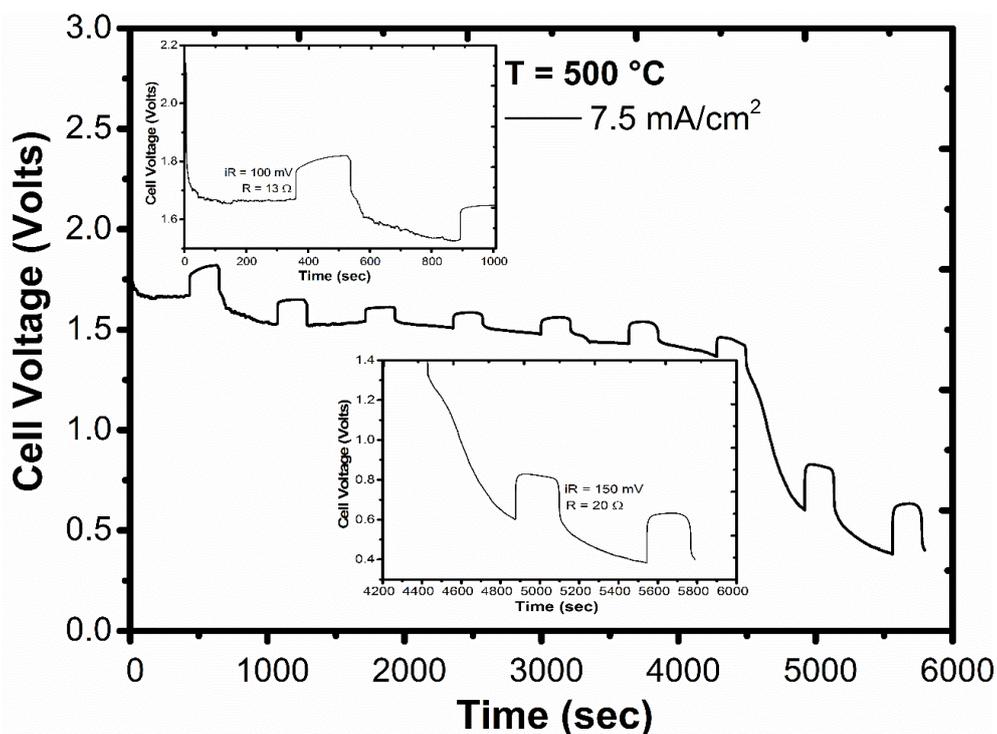


**Figure 4.11.** Galvanostatic discharge of  $\text{NiCo}_2\text{S}_4$  at current densities from 7.5 to 60  $\text{mA}/\text{cm}^2$  at 500 °C

## Chapter 4: Transition Metal Sulfide Cathodes based on Nickel and Cobalt

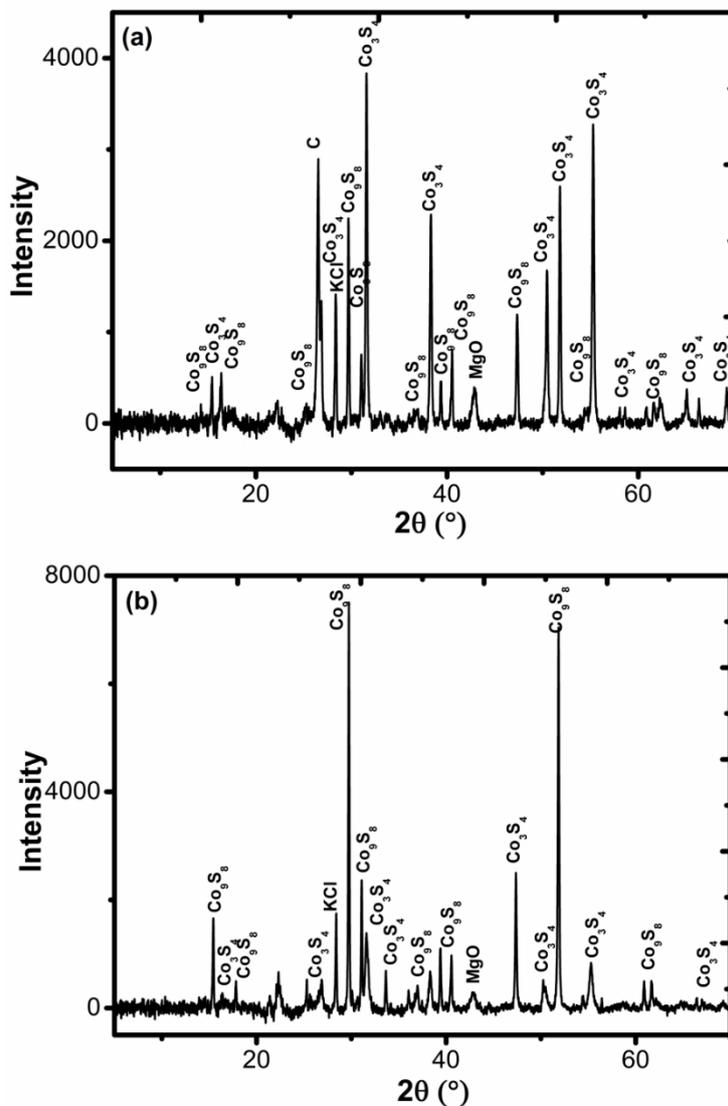
The galvanostatic intermittent titration technique of  $\text{NiCo}_2\text{S}_4$  was performed at a current density of  $7.5 \text{ mA/cm}^2$  at  $500 \text{ }^\circ\text{C}$  and data are shown in Figure 4.12. During discharge the voltage of  $\text{NiCo}_2\text{S}_4$  drops between the current pulses and the relaxation period until a voltage of  $0.5 \text{ V}$  is reached. The IR drop is  $100 \text{ mV}$  at the beginning of discharge and  $150 \text{ mV}$  at the end of the measurement, which indicates that the cell resistance is increasing from a resistance of around  $13 \text{ } \Omega$  at the beginning of the measurement to around  $20 \text{ } \Omega$  after the cell discharge.

The chemical diffusion coefficient  $D = 7.00 \cdot 10^{-6} \text{ cm}^2 \text{ s}^{-1}$  for  $\text{NiCo}_2\text{S}_4$  can be calculated from equation [3.1] where  $n_m = 0.000656 \text{ (mol)}$ ,  $V_m = 62.20 \text{ (cm}^3 \text{ / mol)}$ ,  $\Delta E_s = 0.140 \text{ (V)}$  and  $\Delta E_t = 0.075 \text{ (V)}$ .



**Figure 4.12.** Galvanostatic intermittent titration technique applied to study of  $\text{NiCo}_2\text{S}_4$  at a current density of  $7.5 \text{ mA/cm}^2$  at  $500 \text{ }^\circ\text{C}$





**Figure 4.14.** PXRD data collected at room temperature of the  $\text{NiCo}_2\text{S}_4$  cathode following galvanostatic discharge at 500 °C (a) after stopping the discharge between the first and second plateaus and (b) at the end of the galvanostatic discharge. The crystalline phases have been labelled

## Chapter 4: Transition Metal Sulfide Cathodes based on Nickel and Cobalt

As the electrochemical investigation of  $\text{CoNi}_2\text{S}_4$  suggests that the first plateau corresponds to the electrochemical reaction



and the second plateau of  $\text{CoNi}_2\text{S}_4$  corresponds to the electrochemical reaction



this could be confirmed by PXRD results after testing, as PXRD would allow the crystalline phases to be identified.

The PXRD data of  $\text{CoNi}_2\text{S}_4$  between the first and the second plateaus (Figure 4.13a) show that there are several crystalline phases present which can be assigned to known crystalline phases in the PDF database. The following crystalline phases could be assigned to a hexagonal unit cell, with cell parameters ( $a = 3.47(4) \text{ \AA}$ ,  $c = 5.35(4) \text{ \AA}$ ), and space group  $P6_3/mmc$  and suggests a NiS phase and not a CoS phase or other phases, as the values of unit cell are closer to the literature. Also some other peaks could be indexed to a rhombohedral unit cell, with cell parameters ( $a = 9.607(3) \text{ \AA}$ ,  $c = 3.142(10) \text{ \AA}$ ) and space group  $R\bar{3}m$  and suggests a NiS phase as well.

NiS exists in two phases, a high temperature hexagonal phase NiS and a low temperature rhombohedral phase NiS. This phase transformation takes place at  $379 \text{ }^\circ\text{C}$  and is accompanied by a 4% volume change [13].

A cubic phase with space group  $Fd\bar{3}m$  and unit cell ( $a = 9.402(20) \text{ \AA}$ ) suggests a  $\text{Co}_3\text{S}_4$  phase.

Therefore PXRD data indicate the formation of NiS and  $\text{Co}_3\text{S}_4$  as the product of the electrochemical process after the first plateau in the discharge curve of  $\text{CoNi}_2\text{S}_4$  [1].

## Chapter 4: Transition Metal Sulfide Cathodes based on Nickel and Cobalt

PXRD data were also collected at the end of discharge of  $\text{CoNi}_2\text{S}_4$  (Figure 4.13b) and data show a hexagonal  $\text{NiS}$  phase ( $a = 3.43(7) \text{ \AA}$ ,  $c = 5.34(11) \text{ \AA}$ ), a rhombohedral  $\text{NiS}$  phase ( $a = 9.615(8) \text{ \AA}$ ,  $c = 3.147(4) \text{ \AA}$ ) and also a cubic  $\text{Co}_9\text{S}_8$  phase ( $a = 10.01(9) \text{ \AA}$ ). The main phase present is  $\text{Co}_9\text{S}_8$ . However there are also peaks of  $\text{Co}_3\text{S}_4$  and peaks of the  $\text{KCl}$  from the electrolyte and  $\text{MgO}$  from the separator. Although  $\text{Li}_2\text{S}$  is an expected product of the discharge process but PXRD data do not show  $\text{Li}_2\text{S}$ .

Therefore the formation of  $\text{Co}_9\text{S}_8$  is the product of the electrochemical process at the end of the second plateau.

This PXRD data is in agreement with proposed equations [4.1] and [4.2] based on galvanostatic discharge [1].

In the case of  $\text{NiCo}_2\text{S}_4$ , the first plateau corresponds to the electrochemical reaction



and the second plateau of  $\text{NiCo}_2\text{S}_4$  corresponds to the electrochemical reaction



The PXRD data of  $\text{NiCo}_2\text{S}_4$  between the first and the second plateaus (Figure 4.14a) show that  $\text{Co}_3\text{S}_4$  ( $a = 9.3914(18) \text{ \AA}$ , space group  $Fd\bar{3}m$ ) and  $\text{Co}_9\text{S}_8$  ( $a = 9.9714(14) \text{ \AA}$ , space group  $Fm\bar{3}m$ ) were identified as crystalline products present after the first plateau of the electrochemical discharge.

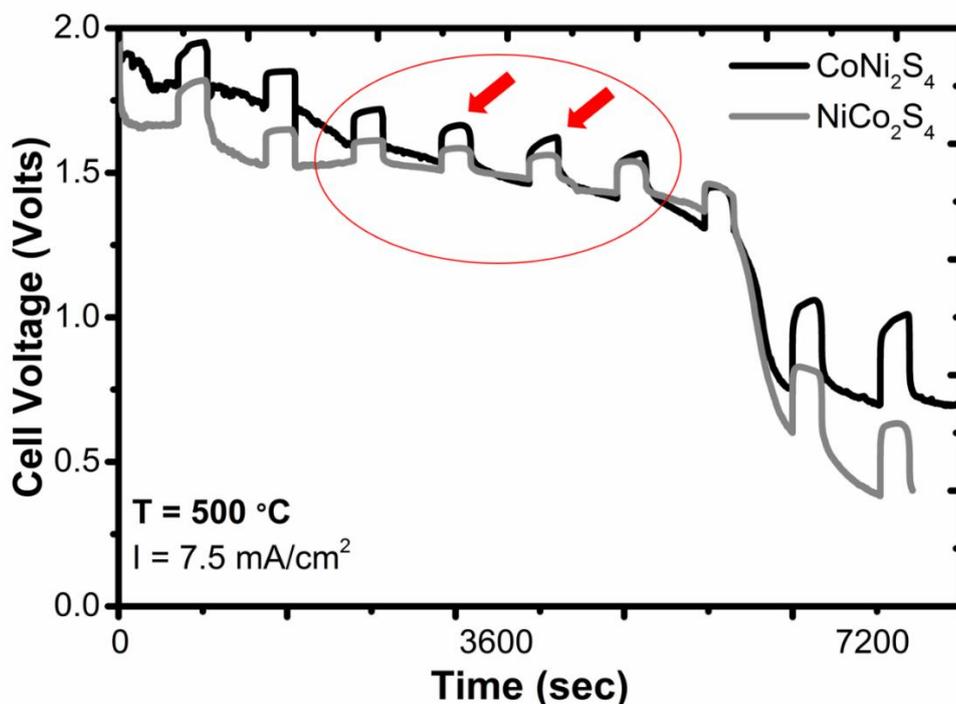
PXRD did not show  $\text{NiS}$  or  $\text{Li}_2\text{S}$ . This could be due to overlap the  $\text{Co}_3\text{S}_4$  and  $\text{Co}_9\text{S}_8$  peaks with peaks of  $\text{NiS}$ . Therefore the PXRD data indicate the formation of  $\text{Co}_3\text{S}_4$  as the product of the electrochemical process after the first plateau in the discharge curve of  $\text{NiCo}_2\text{S}_4$ .

PXRD data of  $\text{NiCo}_2\text{S}_4$  were also collected at the end of discharge (Figure 4.14b) and show a cubic  $\text{Co}_9\text{S}_8$  phase ( $a = 9.963(7) \text{ \AA}$ ) and a cubic  $\text{Co}_3\text{S}_4$  phase ( $a = 9.389(4) \text{ \AA}$ ). Therefore the formation of  $\text{Co}_9\text{S}_8$  is the product of the electrochemical process at the end of the second plateau of  $\text{NiCo}_2\text{S}_4$ .

## Chapter 4: Transition Metal Sulfide Cathodes based on Nickel and Cobalt

This PXRD data is in agreement with proposed equations [4.3] and [4.4] based on the electrochemical reactions of  $\text{NiCo}_2\text{S}_4$ .

GITT results of  $\text{CoNi}_2\text{S}_4$  and  $\text{NiCo}_2\text{S}_4$  show that both cathodes have similar cell resistances at the beginning of the measurement ( $13 \Omega$ ) to the end of the measurement ( $20\text{-}23 \Omega$ ). GITT data of both cathodes also show in Figure 4.15 that the shape of the voltage “steps” (shown by red arrows) during the relaxation period differs during discharge and that could be explained by unique thermodynamics and kinetics procedures as phase formation or decomposition rather than a phase transformation take place during discharge as different phases have different equilibrium procedures [14].



**Figure 4.15.** GITT data of both  $\text{CoNi}_2\text{S}_4$  and  $\text{NiCo}_2\text{S}_4$  at  $500 \text{ }^\circ\text{C}$  at a current density of  $7.5 \text{ mA/cm}^2$ . Red arrows show the different shape of voltage “steps”

### 4.3 Summary

$\text{CoNi}_2\text{S}_4$  and  $\text{NiCo}_2\text{S}_4$  exhibit two electrochemical steps with capacities of  $350 \text{ mA h g}^{-1}$  and  $290 \text{ mA h g}^{-1}$  respectively. This is comparable to the capacities for the most commonly used sulfide based cathodes such as  $\text{FeS}_2$ ,  $\text{CoS}_2$  and  $\text{NiS}_2$  which exhibit capacities of 558, 598 and  $545 \text{ mA h g}^{-1}$  respectively. However  $\text{CoS}_2$  still exhibits a higher capacity as presented in Table 4.4.

$\text{NiCo}_2\text{S}_4$  has a lower voltage (1.70 V and 1.50 V) than  $\text{CoNi}_2\text{S}_4$  (1.75 V and 1.50 V) against  $\text{Li}_{13}\text{Si}_4$  at  $500^\circ\text{C}$  and this might be explained by the different nickel/cobalt ratio or structure (normal spinel/inverse spinel) to the compounds. It is known that the voltage of a battery ranges of compounds consisting of transition metal ions [15]. There is a relationship between battery voltage and the number of electrons in the  $d$  orbitals of transition-metal ions. Moreover the voltage of the battery increases with increasing number of electrons in the  $d$  orbitals. Ni metal exhibits more electrons in the  $d$  orbitals than Co ( $d^8$  and  $d^7$ , respectively). As a result the compound  $\text{CoNi}_2\text{S}_4$  has higher voltage than  $\text{NiCo}_2\text{S}_4$ . However,  $\text{NiCo}_2\text{S}_4$  has a greater lithium diffusion coefficient than  $\text{CoNi}_2\text{S}_4$ .

Also both have similar voltages with  $\text{FeS}_2$ ,  $\text{CoS}_2$  and  $\text{NiS}_2$  vs Li-Al at  $400^\circ\text{C}$  [16 -18] as shown in Table 4.5.

$\text{CoNi}_2\text{S}_4$  and  $\text{NiCo}_2\text{S}_4$  have a similar behaviour (two electrochemical steps, similar voltage plateaus) to the most studied industrial cathodes so they are promising candidates for novel materials in Li thermal batteries. Further investigation of  $\text{CoNi}_2\text{S}_4$  and  $\text{NiCo}_2\text{S}_4$  may enable further enhancement of properties. For example the influence of particle size on the electrochemical process.

The work in Chapter 4 has been published titled as: *Synthesis and Electrochemical Study of  $\text{CoNi}_2\text{S}_4$  as a Novel Cathode Material in a Primary Li Thermal Battery* at Journal of The Electrochemical Society [1].

## Chapter 4: Transition Metal Sulfide Cathodes based on Nickel and Cobalt

**Table 4.4.** Capacities of CoNi<sub>2</sub>S<sub>4</sub> and NiCo<sub>2</sub>S<sub>4</sub> compared to FeS<sub>2</sub>, CoS<sub>2</sub> and NiS<sub>2</sub>

Sulfides	Capacity (mA h g <sup>-1</sup> )
FeS <sub>2</sub>	558 [16]
CoS <sub>2</sub>	598 [16] ~ 1.70 times more capacity than CoNi <sub>2</sub> S <sub>4</sub>
NiS <sub>2</sub>	545 [16]
CoNi <sub>2</sub> S <sub>4</sub>	350
NiCo <sub>2</sub> S <sub>4</sub>	290

**Table 4.5.** Electrochemical reactions and voltages of CoNi<sub>2</sub>S<sub>4</sub> and NiCo<sub>2</sub>S<sub>4</sub> compared to FeS<sub>2</sub>, CoS<sub>2</sub> and NiS<sub>2</sub>. All FeS<sub>2</sub>/CoS<sub>2</sub>/NiS<sub>2</sub> voltages are versus Li-Al, CoNi<sub>2</sub>S<sub>4</sub>/NiCo<sub>2</sub>S<sub>4</sub> voltages are versus Li-Si

Sulfides	Voltage at 400 °C vs Li-Al (1 <sup>st</sup> plateau)	Voltage at 400 °C vs Li-Al (2 <sup>nd</sup> plateau)	Voltage at 400 °C vs Li-Al (3 <sup>rd</sup> plateau)	Voltage at 400 °C vs Li-Al (4 <sup>th</sup> plateau)
FeS <sub>2</sub>	FeS <sub>2</sub> + 3/2 Li → ½ Li <sub>3</sub> Fe <sub>2</sub> S <sub>4</sub> (1.75 V)	Li <sub>3</sub> Fe <sub>2</sub> S <sub>4</sub> + Li → Li <sub>2</sub> FeS <sub>2</sub> + FeS + Li <sub>2</sub> S (1.64 V)	Li <sub>2</sub> FeS <sub>2</sub> → Fe + Li <sub>2</sub> S + S (1.26 V)	-
CoS <sub>2</sub>	CoS <sub>2</sub> + 4/3 Li → 1/3 Co <sub>3</sub> S <sub>4</sub> + 2/3 Li <sub>2</sub> S (1.70 V)	Co <sub>3</sub> S <sub>4</sub> + 8/3 Li → 1/3 Co <sub>9</sub> S <sub>8</sub> + 4/3 Li <sub>2</sub> S (1.64 V)	Co <sub>9</sub> S <sub>8</sub> + 16 Li → 9 Co + 8 Li <sub>2</sub> S (1.37 V)	-
NiS <sub>2</sub>	NiS <sub>2</sub> + 2 Li → NiS + Li <sub>2</sub> S (1.74 V)	7 NiS + 2 Li → Ni <sub>7</sub> S <sub>6</sub> + Li <sub>2</sub> S (1.58 V)	3 Ni <sub>7</sub> S <sub>6</sub> + 8 Li → 7 Ni <sub>3</sub> S <sub>2</sub> + 4 Li <sub>2</sub> S (1.55 V)	Ni <sub>3</sub> S <sub>2</sub> + 4 Li → 3 Ni + 2 Li <sub>2</sub> S (1.36 V)
	Voltage at 500 °C vs Li-Si (1 <sup>st</sup> plateau)	Voltage at 500 °C vs Li-Si (2 <sup>nd</sup> plateau)	Voltage at 500 °C vs Li-Si (3 <sup>rd</sup> plateau)	Voltage at 500 °C vs Li-Si (4 <sup>th</sup> plateau)
CoNi <sub>2</sub> S <sub>4</sub>	CoNi <sub>2</sub> S <sub>4</sub> + 4/3 Li → 1/3 Co <sub>3</sub> S <sub>4</sub> + 2 NiS + 2/3 Li <sub>2</sub> S (1.75 V)	Co <sub>3</sub> S <sub>4</sub> + 8/3 Li → 1/3 Co <sub>9</sub> S <sub>8</sub> + 4/3 Li <sub>2</sub> S (1.50 V)	-	-
NiCo <sub>2</sub> S <sub>4</sub>	NiCo <sub>2</sub> S <sub>4</sub> + 2/3 Li → 2/3 Co <sub>3</sub> S <sub>4</sub> + NiS + 1/3 Li <sub>2</sub> S (1.70 V)	Co <sub>3</sub> S <sub>4</sub> + 8/3 Li → 1/3 Co <sub>9</sub> S <sub>8</sub> + 4/3 Li <sub>2</sub> S (1.50 V)	-	-

## 4.4 References

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## Chapter 5: Zirconium Sulfide Cathodes

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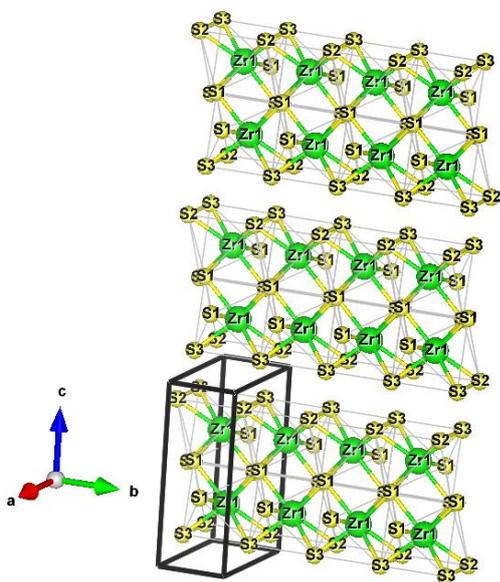
## Chapter 5: Zirconium Sulfide Cathodes

### 5.1 Material Characterisation of Zirconium Sulfides

#### 5.1.1 $ZrS_3$

$ZrS_3$  has a pseudo one-dimensional structure as shown in Figure 5.1 and Zr atoms occupy the center of a trigonal prism with sulfur atoms at the corners and two of those S atoms bond to each other. Neighboring atoms create an infinite chain along the *b*-axis of the crystal [1]. These chains stack to form corrugated layers perpendicular to *c*-axis.

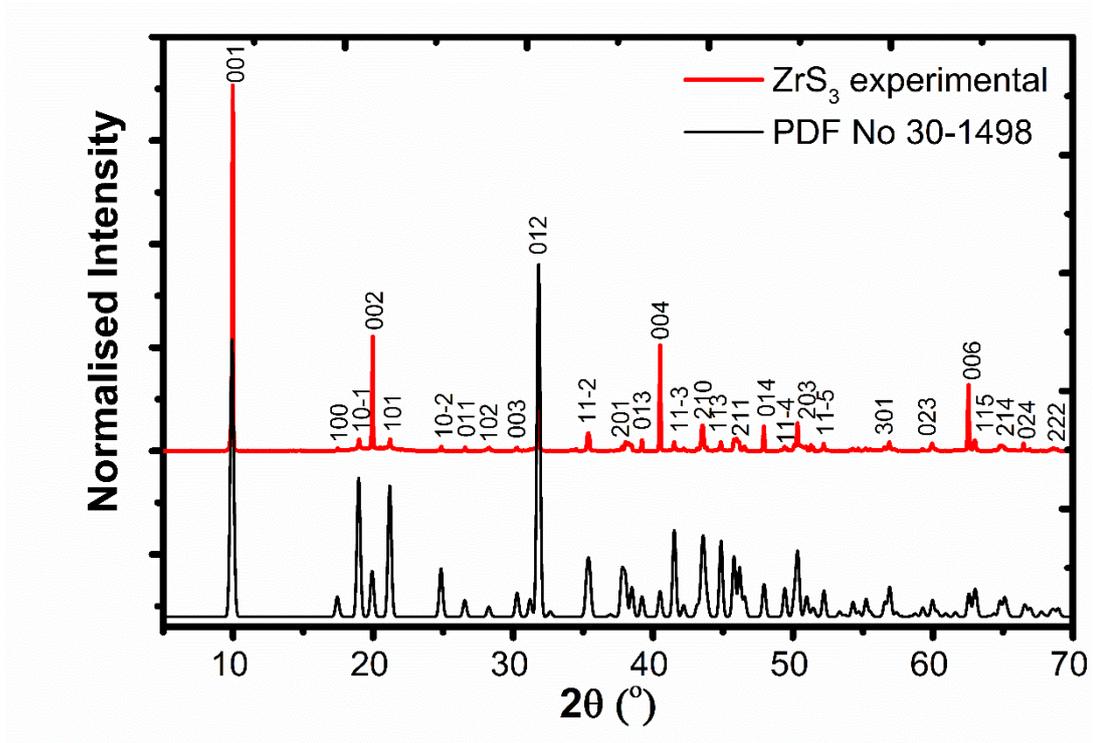
The synthesis of  $ZrS_3$  has previously been reported by many authors [2-5] and their solid state synthesis involves multiple firings at temperatures from 600 °C to 1000 °C for almost 1 month. This work improved the synthesis of  $ZrS_3$ , in synthesizing the sample in shorter time using only one firing step for 1 week.



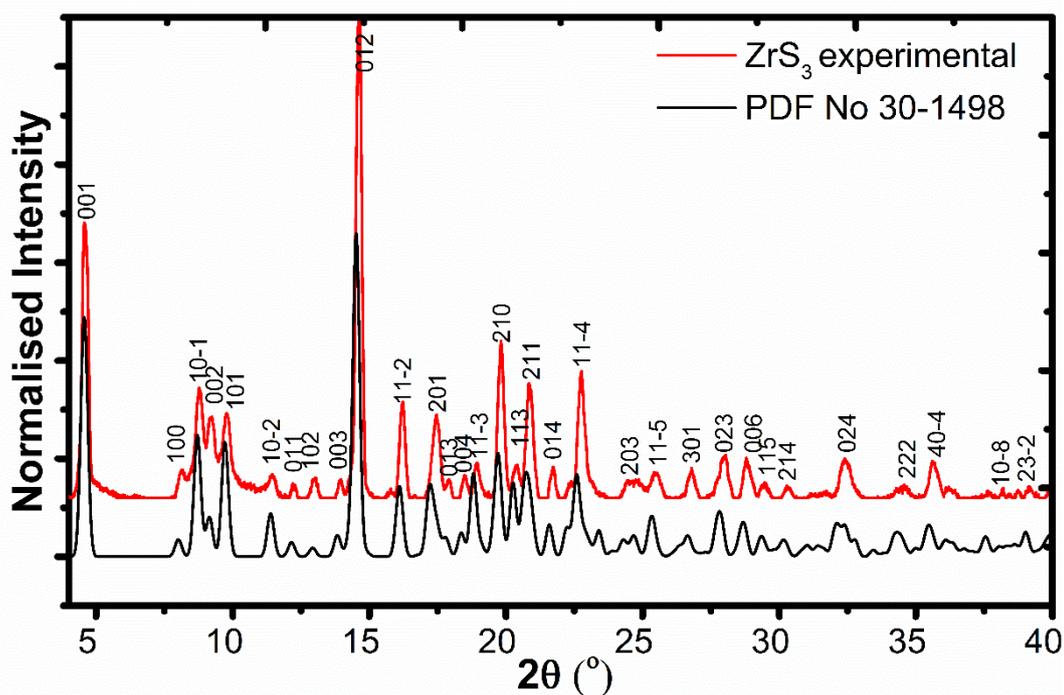
**Figure 5.1.** Crystal structure of  $ZrS_3$ . Yellow atoms are sulfur, green atoms are zirconium

[6]

Zirconium trisulfide was studied by powder X-ray diffraction in both reflection and transmission geometry and results are presented in Figures 5.2 and 5.3.  $ZrS_3$  was identified as a single phase and could be indexed to the  $P2_1/m$  unit cell reported by Furuseth *et al.* Cell parameters are given in Table 5.1.



**Figure 5.2.** PXRD data (Cu radiation) of  $ZrS_3$  (reflection) (red line) [6] compared to the simulated diffraction pattern using the published crystallographic model [2] (black line)



**Figure 5.3.** PXRD data (Mo radiation) of  $\text{ZrS}_3$  (transmission geometry in a capillary) (red line) [6] compared to the simulated diffraction pattern using the published crystallographic model [2] (black line)

**Table 5.1.** Refined unit cell parameters of  $\text{ZrS}_3$

Unit cell [ $\text{\AA}$ ]	Experimental [6]	Literature [2]
$a$	5.125(5)	5.124
$b$	3.625(4)	3.624
$c$	8.981(10)	8.980
$\beta$ [ $^\circ$ ]	97.29(8)	97.28
Cell Volume [ $\text{\AA}^3$ ]	165.53(21)	165.44

The experimental intensity of  $\text{ZrS}_3$  on the diffraction pattern from reflection, as the sample was pressed into a bulk flat plate sample holder, is different from the intensities in the simulated diffraction pattern in Figure 5.2. However, the collection of data in a quartz capillary from orientation allow much better sampling of intensities as shown in Figure 5.3. As a result the needle-like shape of the  $\text{ZrS}_3$  crystals results in a large effect on the diffraction pattern from preferred orientation. The shape also of the  $\text{ZrS}_3$  crystals means a high surface area which could enable lithium ion diffusion in the thermal battery at high temperatures and this could be confirmed at a later stage by the high capacity of  $357 \text{ mA h g}^{-1}$  [6].

In order to explore the thermal stability of  $\text{ZrS}_3$  at elevated temperature, PXRD data were collected *in situ* at temperatures in the range from  $25 \text{ }^\circ\text{C}$  to  $500 \text{ }^\circ\text{C}$  as shown in Figure 5.4. Throughout this temperature range  $\text{ZrS}_3$  is stable and there are no phase transformations or apparent degradation. The volume of the unit cell and the thermal expansion coefficient increase as the temperature increases as shown in Figure 5.5 [6].

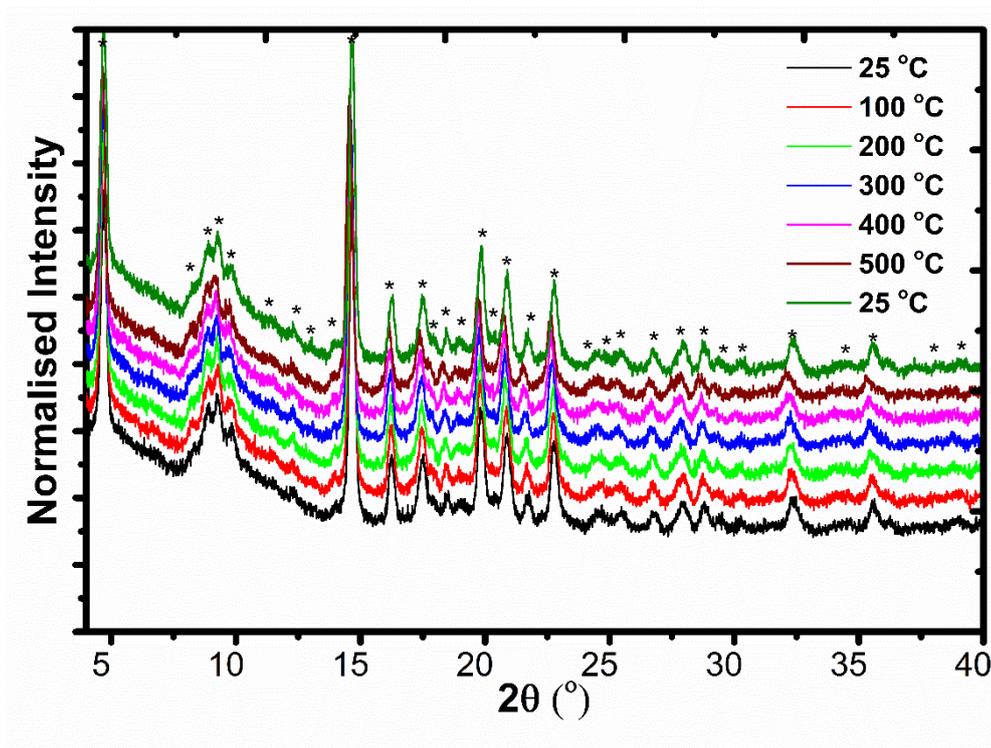


Figure 5.4. Variable temperature PXRD data (Mo radiation) of  $ZrS_3$  at temperatures from 25 °C up to 500 °C [6]

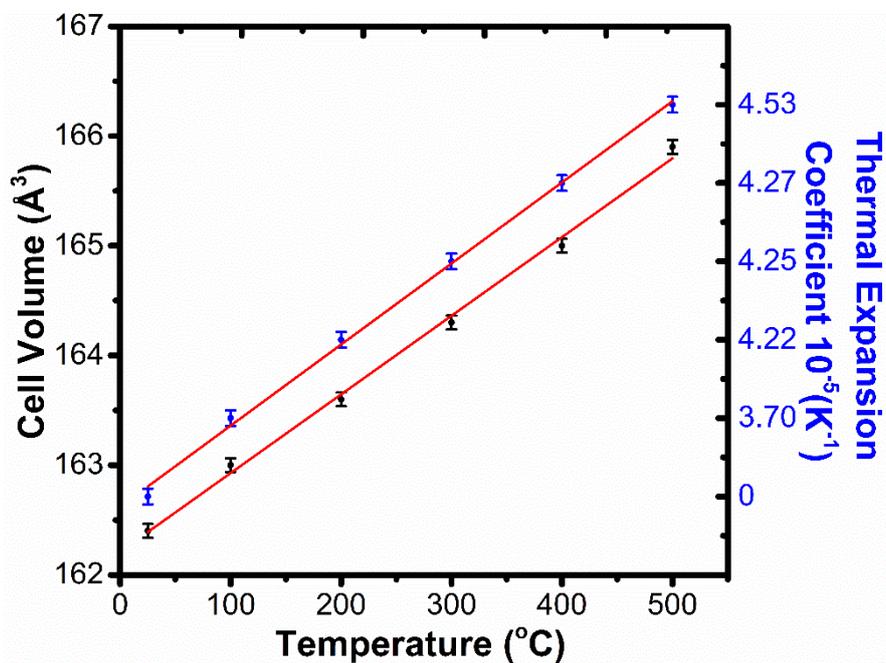
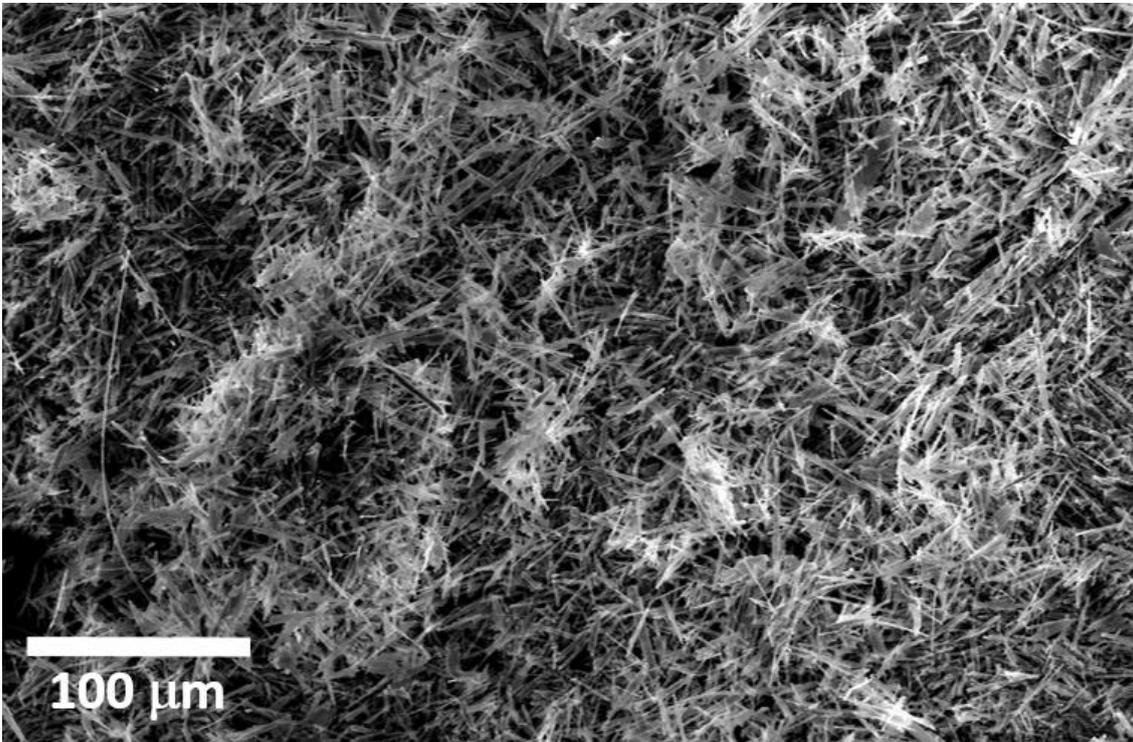
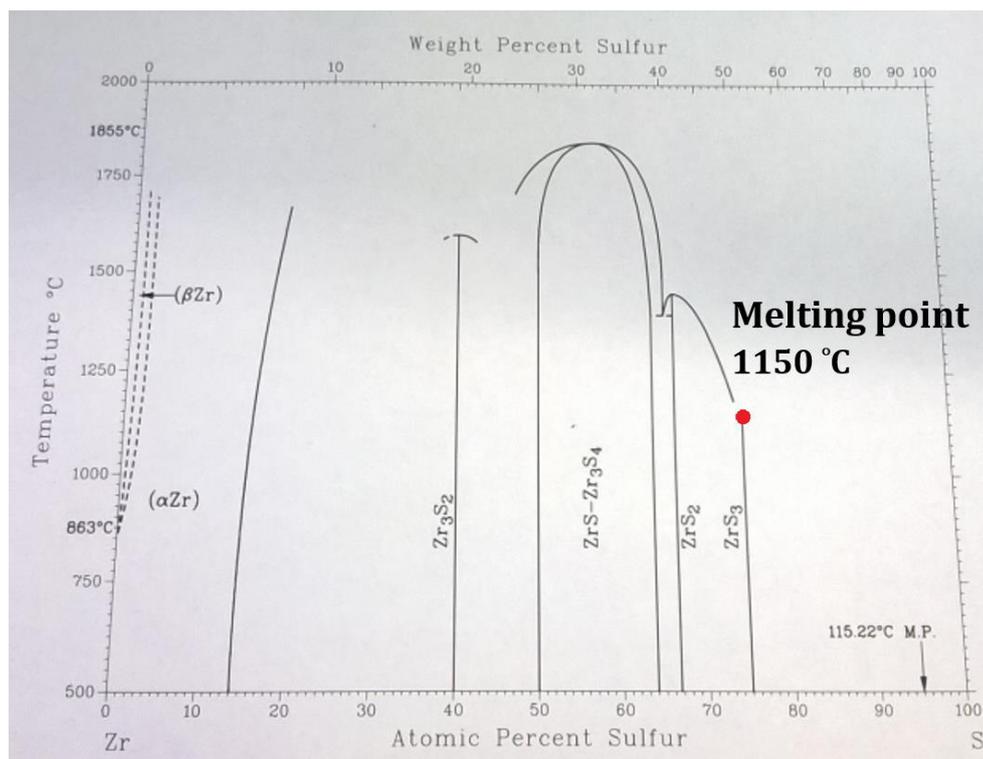


Figure 5.5. Cell volume and thermal expansion coefficient of  $ZrS_3$  vs temperature from 25 °C up to 500 °C [6]

The morphology and the shape of crystallites of  $ZrS_3$  was investigated by SEM and are presented in Figure 5.6. Crystallites of  $ZrS_3$  have a uniform morphology, which is consistent with a single phase sample and the crystallites are needles. EDX analysis confirms the average elemental composition of  $ZrS_3$  with zirconium  $25 \pm 3$  at% and sulfur  $75 \pm 3$  at% [6]. This elemental analysis is in agreement with the phase diagram of Zr - S system as shown in Figure 5.7. The melting point of  $ZrS_3$  is  $1150 \text{ }^\circ\text{C}$  [7].



**Figure 5.6.** SEM image of  $ZrS_3$  [6]

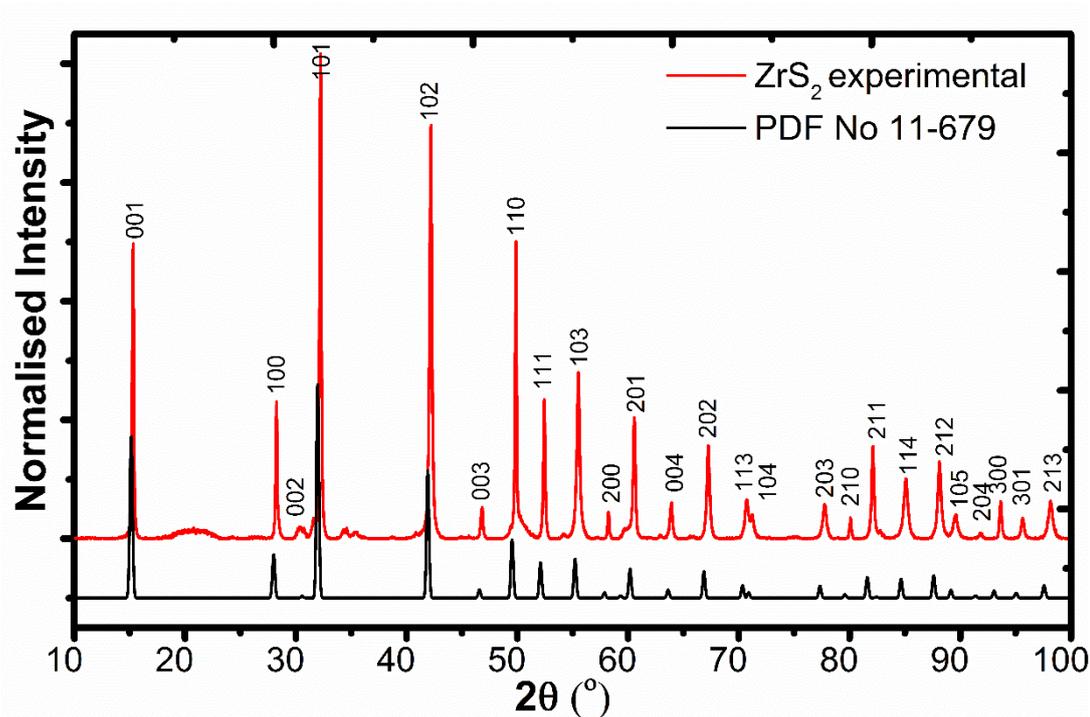


**Figure 5.7.** Phase diagram of Zr - S system

(permission by J. Rasneur and F. Marion) [7]

To investigate the thermal stability of ZrS<sub>3</sub> even further, a quantity of ZrS<sub>3</sub> was heated to 700 °C at 6 °C min<sup>-1</sup> and was held at this temperature for 1 hour under flowing argon. Then the sample was cooled to room temperature at 6 °C min<sup>-1</sup>. The resulting diffraction pattern is presented in Figure 5.8 and the PXRD data shows that ZrS<sub>3</sub> had decomposed to ZrS<sub>2</sub>.

ZrS<sub>2</sub> crystallises in space group  $P\bar{3}m1$  with refined unit cell parameters  $a = b = 3.6631(4)$  Å,  $c = 5.8331(5)$  Å and this is in agreement with Fotouhi [8]. The mass of ZrS<sub>3</sub> before heating was 159 mg and it lost a mass of 43 mg after heating to 700 °C. This mass loss of 27 % is consistent with the thermal decomposition of ZrS<sub>3</sub> to ZrS<sub>2</sub> and gaseous sulfur at high temperatures [6].



**Figure 5.8.** PXRD data (Cu radiation) of thermal decomposition of  $ZrS_3$  to  $ZrS_2$  (red line) [6] compared to the simulated diffraction pattern using the published crystallographic model [8] (black line)

## 5.2 Electrochemical Investigation of Zirconium Sulfides

### 5.2.1 $ZrS_3$

$ZrS_3$  was characterised electrochemically by galvanostatic discharge and galvanostatic intermittent titration technique.

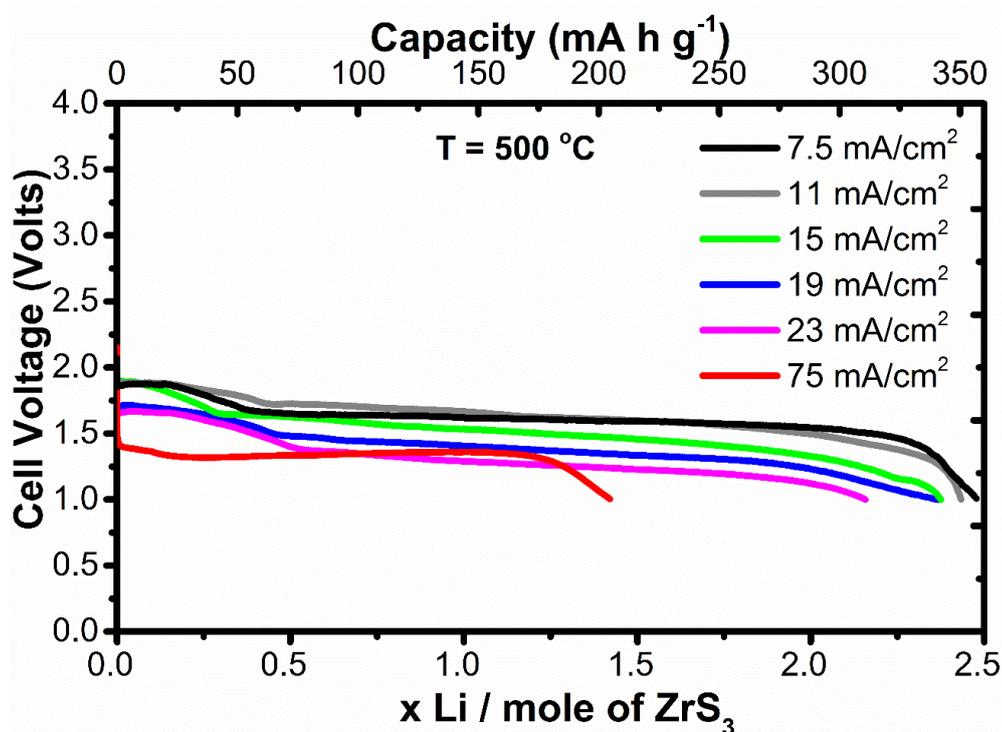
The galvanostatic discharging of  $ZrS_3$  at 500 °C is presented in Figure 5.9.  $ZrS_3$  was discharged at different current densities from 7.5 to 75 mA/cm<sup>2</sup> to investigate the performance and the resulting discharge profiles. The voltage cut-off for this measurement was 1 Volt.

At both current densities of 7.5 and 11 mA/cm<sup>2</sup> there was a single flat voltage plateau at around 1.70 V and a capacity of 357 mA h g<sup>-1</sup> was achieved ( $x = 2.5$  Li) [6].

At current densities of 15, 19 and 23 mA/cm<sup>2</sup>, the single flat voltage plateau is lower than 1.70 V as the cell resistance might be higher, however the capacity is still high (over 300 mA h g<sup>-1</sup>) and  $x = 2.25$  Li.

At a current density of 75 mA/cm<sup>2</sup> the single plateau is around 1.25 V and a capacity of around 200 mA h g<sup>-1</sup> was achieved, ( $x = 1.5$  Li).

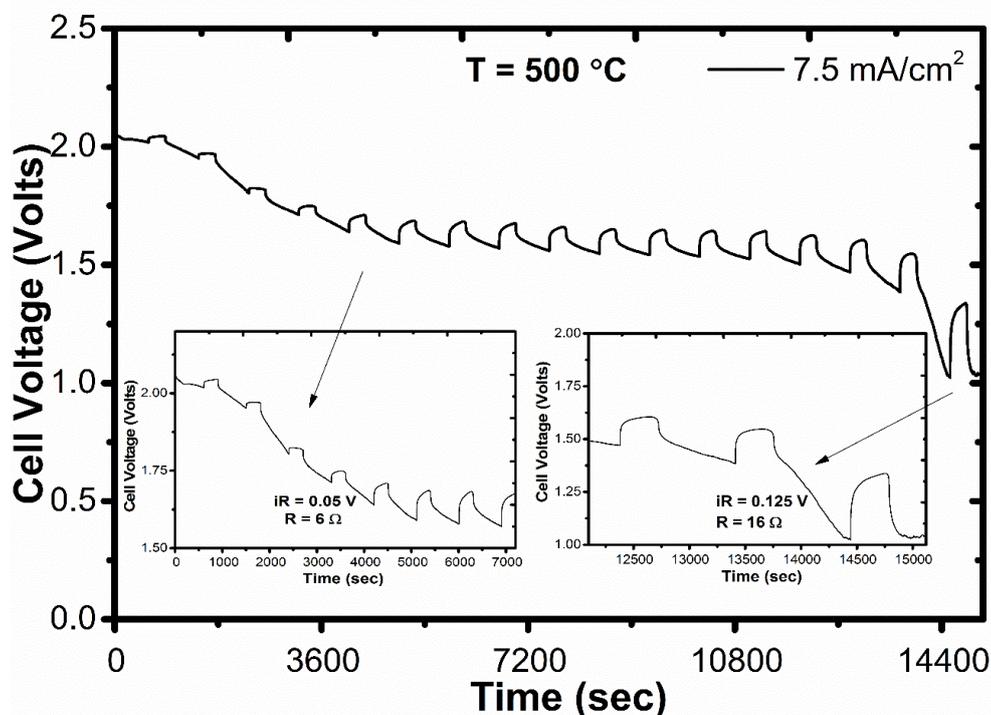
The amount of active anode (0.15 g) corresponds to 73 mA h for the discharge plateau from Li<sub>13</sub>Si<sub>4</sub> to Li<sub>7</sub>Si<sub>3</sub> which is 0.157 V vs Li. The measured capacity of the cathode is 54 mA h which keeps the discharge as being performed against the 0.157 V Li plateau.



**Figure 5.9.** Galvanostatic discharge of ZrS<sub>3</sub> at current densities of 7.5 to 75 mA/cm<sup>2</sup> at 500 °C [6]

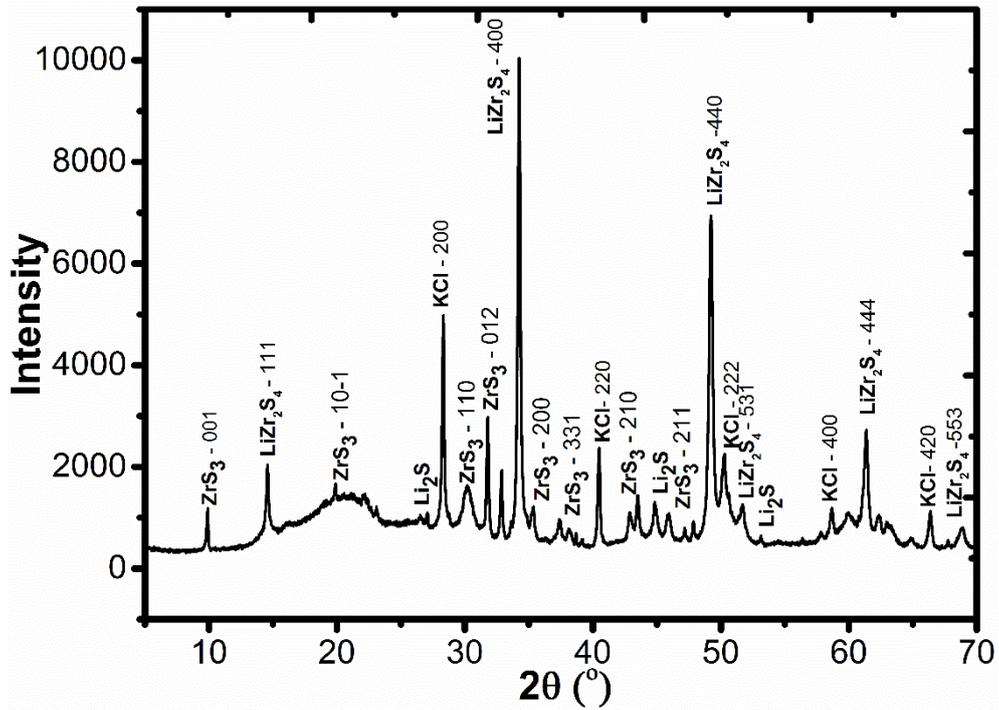
GITT results of  $\text{ZrS}_3$  at a current density of  $7.5 \text{ mA/cm}^2$  at  $500 \text{ }^\circ\text{C}$  are presented in Figure 5.10. The voltage drops between the current pulses and the relaxation time until a voltage of  $1 \text{ V}$  is reached. The IR drop is  $50 \text{ mV}$  at the beginning of discharge and  $125 \text{ mV}$  at the end of the measurement, which indicates that the cell resistance is increasing during the reduction of the cathode, from a resistance of around  $6 \text{ } \Omega$  at the beginning of the measurement to around  $16 \text{ } \Omega$  after the cell discharge [6].

The chemical diffusion coefficient  $D = 4.12 \cdot 10^{-5} \text{ cm}^2 \text{ s}^{-1}$  for  $\text{ZrS}_3$  can be calculated from equation [3.1] where  $n_m = 0.00106 \text{ (mol)}$ ,  $V_m = 49.84 \text{ (cm}^3 \text{ / mol)}$ ,  $\Delta E_s = 0.070 \text{ (V)}$  and  $\Delta E_t = 0.020 \text{ (V)}$ .



**Figure 5.10.** Galvanostatic intermittent titration technique of  $\text{ZrS}_3$  at current density of  $7.5 \text{ mA/cm}^2$  at  $500 \text{ }^\circ\text{C}$  [6]

For further understanding to electrochemical investigation of  $\text{ZrS}_3$ , PXRD data and EDX analysis was carried out as shown in Figures 5.11 and 5.12.



**Figure 5.11.** PXRD data of the cathode electrode after discharge. There are some peaks from the starting material  $ZrS_3$ , some peaks of the electrolyte KCl and some sharp peaks of the new cubic phase  $LiZr_2S_4$  [6]

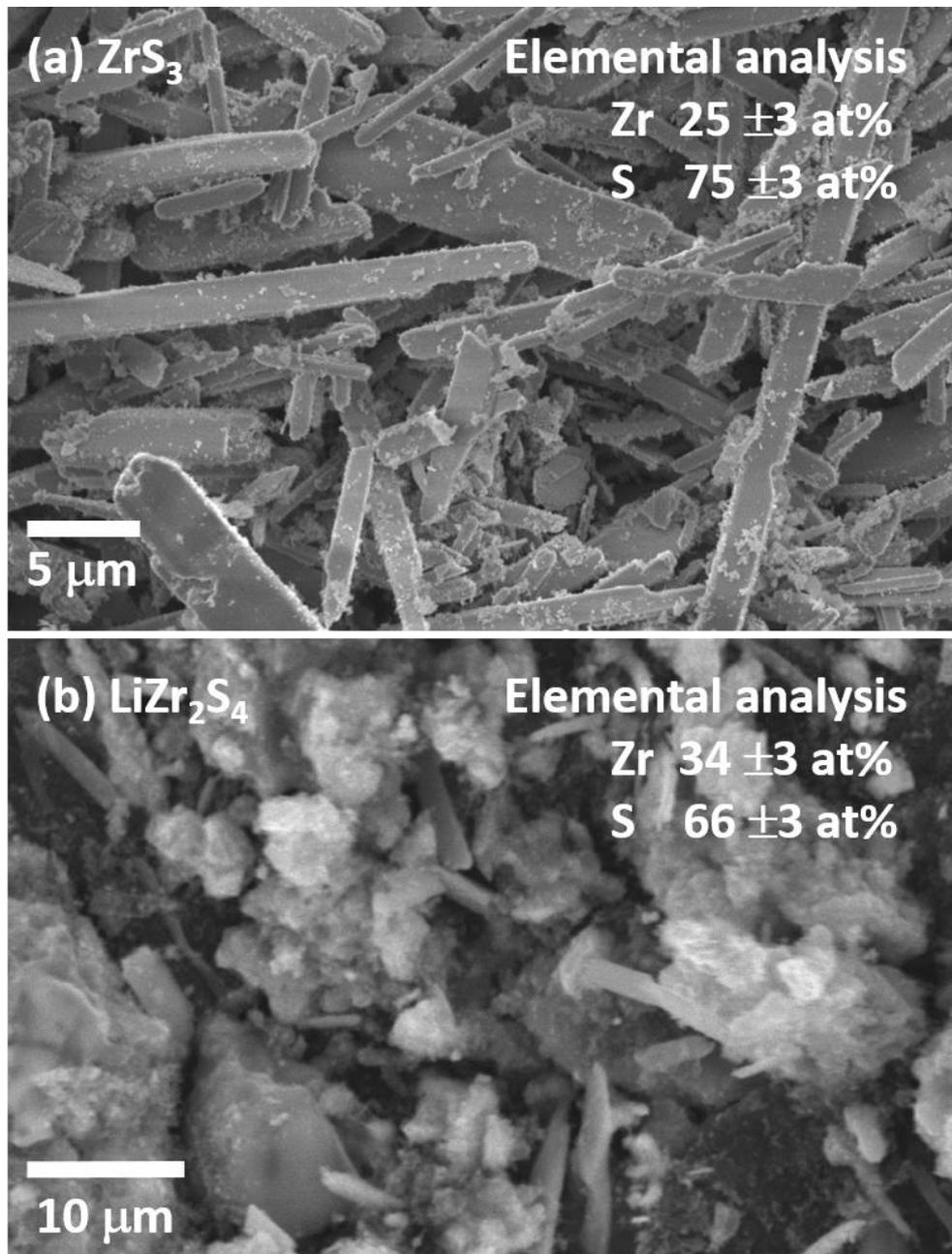


Figure 5.12. SEM image of cathode electrode before (a) and after (b) discharge [6]

ZrS<sub>3</sub> has an orange/red color as shown in Figure 3.1, so 25 wt% Super P Carbon was added to the cathode electrode to increase the electronic conductivity of the sample. According to the electrochemical process in Figure 5.9 the result is



This result is in agreement with PXRD data and SEM/EDX analysis of the cathode after testing.

PXRD data were collected on the cathode after discharge and the diffraction pattern shows peaks from a number of different phases due to the difficulty in separating the cathode from the electrolyte/separator after battery testing as shown in Figure 5.11.

On the diffraction pattern there are a number of peaks which could not be assigned to any known crystalline phase in the PDF database. These peaks could be indexed to a cubic unit cell, with cell parameters  $a = 10.452(8) \text{ \AA}$  and space group  $Fd\bar{3}m$  and suggests a spinel structure, which means a new phase with a cubic structure forms during discharge.

The SEM image of the cathode after electrochemical testing shows that the crystallites are not needles, indicating a morphology very different to that observed before electrochemical testing. EDX analysis can confirm a new phase with a composition of zirconium  $34 \pm 3 \text{ at\%}$  and sulfur  $66 \pm 3 \text{ at\%}$  as shown in Figure 5.12 [6].

### 5.3 Summary

In the past a low temperature  $\text{Li}_{0.5}\text{ZrS}_2$  phase was formed by Li insertion to  $\text{ZrS}_2$  with a different polymorph structure [9].

Compared to  $\text{MS}_2$  cathodes such as  $\text{FeS}_2$ ,  $\text{NiS}_2$  or  $\text{CoS}_2$ , the  $\text{ZrS}_3$  has a good voltage profile, a good thermal stability, a high capacity of  $357 \text{ mA h g}^{-1}$  and most importantly a single flat voltage plateau at 1.70 V vs  $\text{Li}_{13}\text{Si}_4$  at 500 °C. These properties of  $\text{ZrS}_3$  are suitable for thermal battery applications.

Moreover, the Table 5.2 shows the comparison of thermal stability, capacity, lithiated products and voltages of  $\text{ZrS}_3$  to the transition metal disulfides.

**Table 5.2.** Thermal stability, capacity, lithiated products or not, and voltages of  $\text{ZrS}_3$  compared to  $\text{FeS}_2$ ,  $\text{CoS}_2$  or  $\text{NiS}_2$

Sulfides	Capacity ( $\text{mA h g}^{-1}$ )	Thermal decomposition	Products and Voltages against $\text{Li}_{13}\text{Si}_4$ at 500 °C
$\text{FeS}_2$	558 [10]	$\text{FeS}_2 \Rightarrow \text{FeS} + \frac{1}{2} \text{S}_2$ at 580 °C [11 - 12]	$\text{Li}_3\text{Fe}_2\text{S}_4$ at 1.77 V $\text{Li}_2\text{FeS}_2$ at 1.64 V Fe at 1.13 V [15]
$\text{CoS}_2$	598 [10]	$3 \text{CoS}_2 \Rightarrow \text{Co}_3\text{S}_4 + \text{S}_2$ at 650 °C [13]	$\text{Co}_3\text{S}_4$ at 1.75 V $\text{Co}_9\text{S}_8$ at 1.40 V Co at 1.25 V [15]
$\text{NiS}_2$	545 [10]	$\text{NiS}_2 \Rightarrow \text{NiS} + \frac{1}{2} \text{S}_2$ at 600 °C [14]	NiS at 1.76 V $\text{Ni}_7\text{S}_6$ at 1.60 V $\text{Ni}_3\text{S}_2$ at 1.40 V Ni at 1.25 V [15]
$\text{ZrS}_3$	357[6]	$\text{ZrS}_3 \Rightarrow \text{ZrS}_2 + \frac{1}{2} \text{S}_2$ at 700 °C [6]	$\text{LiZr}_2\text{S}_4$ at 1.70 V [6]

The work in Chapter 5 has been published titled as: *Zirconium Trisulfide as a Promising Cathode Material for Li Primary Thermal Batteries* at Journal of The Electrochemical Society [6].

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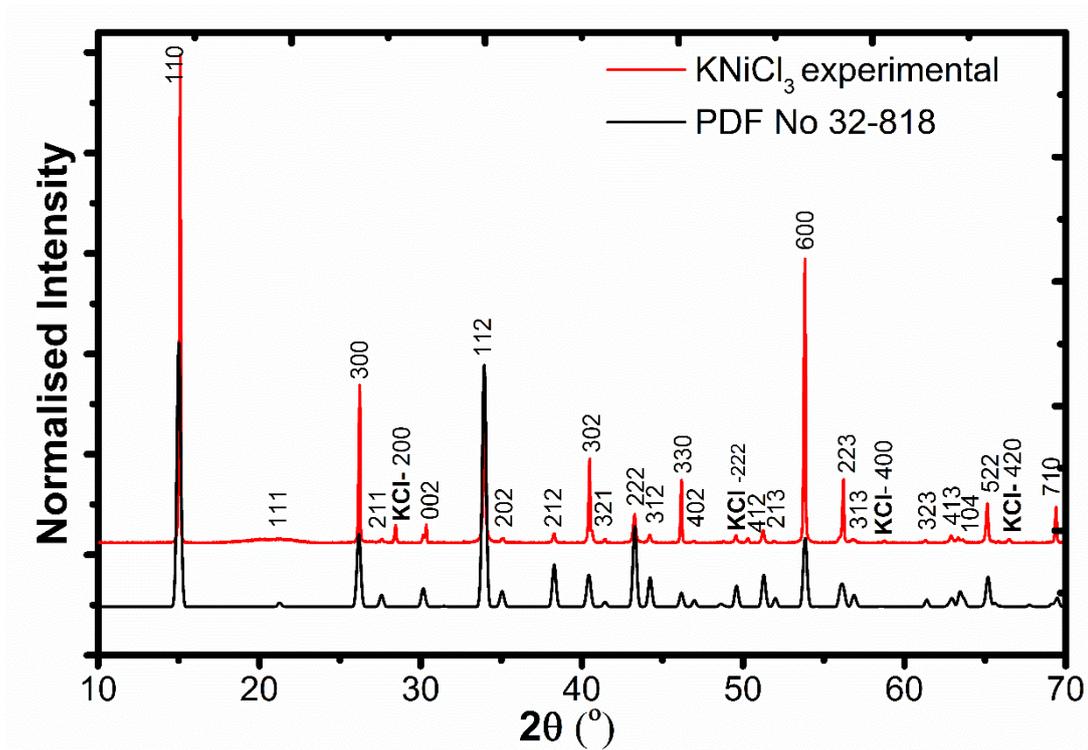
## Chapter 6: Transition Metal Chloride Cathodes

### 6.1 Material Characterisation of Transition Metal Chlorides

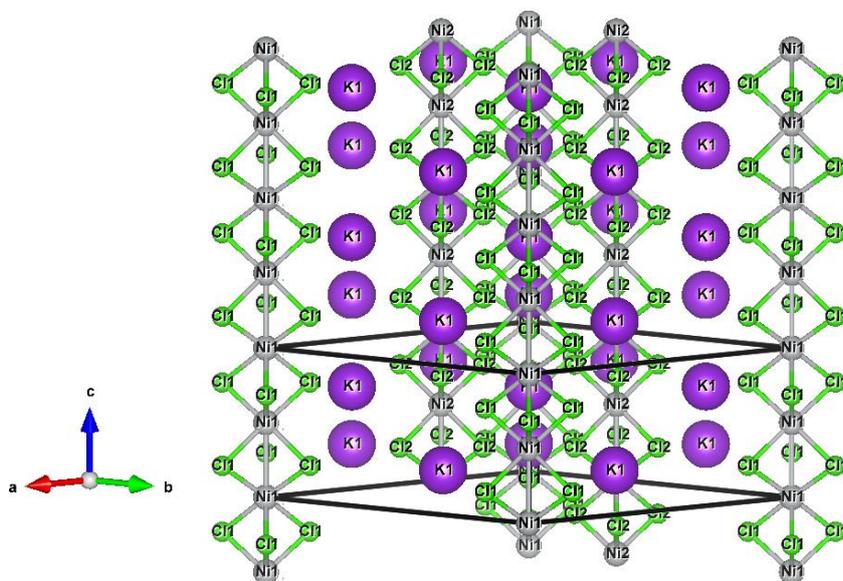
#### 6.1.1 KNiCl<sub>3</sub>

KNiCl<sub>3</sub> was analysed by powder X-ray diffraction and the resulting diffraction pattern is presented in Figure 6.1. KNiCl<sub>3</sub> was identified as the main phase but there is also a KCl impurity ( $a = 6.280(25) \text{ \AA}$ ) from the starting material, which did not react during the synthesis. KNiCl<sub>3</sub> crystallises in hexagonal perovskite  $P6_3mc$  with cell dimensions ( $a = b = 11.800(11) \text{ \AA}$  and  $c = 5.926(4) \text{ \AA}$ ) as shown in Figure 6.2. NiCl<sub>6</sub> face-sharing octahedra form linear chains along the  $c$ -axis and they are also arranged triangularly in the  $ab$ -plane. The face-sharing octahedra compared to corner-sharing octahedra provide 3D structure and better conductivity. This is due to the fact that in the case of face-sharing octahedra conductivity is improved by closer metal-metal distances. The phase diagram, as shown in Figure 6.3, shows that the melting point of KNiCl<sub>3</sub> is 645 °C [1 - 2].

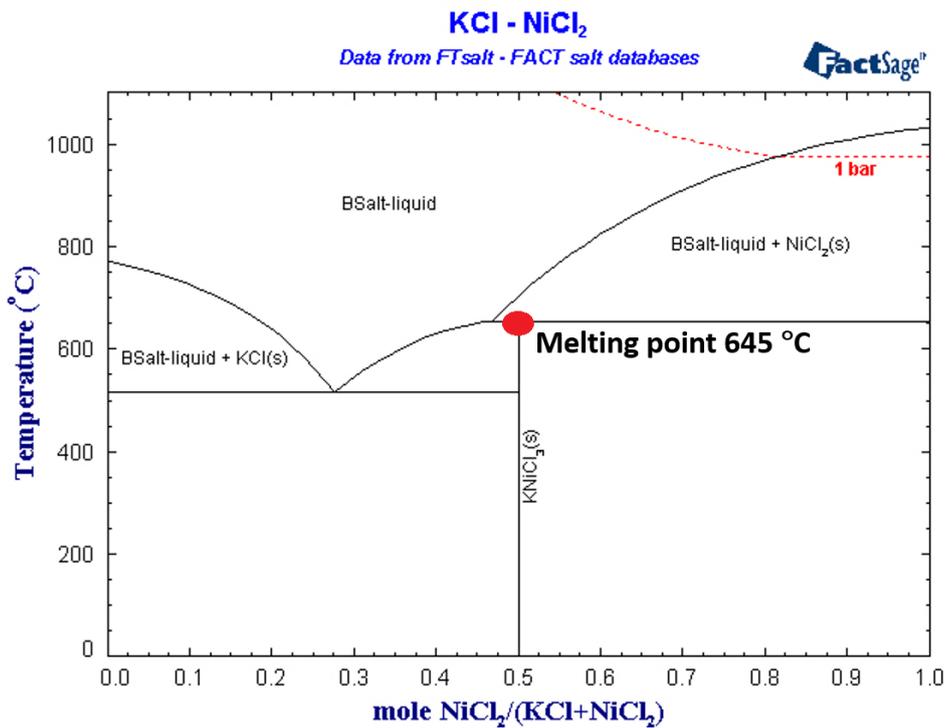
KNiCl<sub>3</sub> exhibits two structural phase transitions during cooling to room temperature, according to the literature [3 - 5]. The first phase transition takes place at 490 °C and the second one takes place at 287 °C. The first phase is hexagonal and the second phase is orthorhombic. However, in our experiments with respect this phase transition could not be obtained.



**Figure 6.1.** PXRD data of  $\text{KNiCl}_3$  at room temperature. Experimental pattern is shown by the red line and the simulated diffraction pattern using published crystallographic model [6] is shown by the black line. Impurity is KCl



**Figure 6.2.** Crystal structure of  $\text{KNiCl}_3$ . Purple atoms are potassium, green atoms are chlorine, grey atoms are nickel



**Figure 6.3.** Phase diagram of NiCl<sub>2</sub> – KCl system [1-2]

The morphology of KNiCl<sub>3</sub>, before and after discharge, was studied by SEM as shown in Figures 6.4a and 6.4b. The size of the crystallites is bigger than 50 μm before testing and smaller than 50 μm after the discharge. EDX confirms K 19 ±1 at%, Ni 19 ±1 at% and Cl 62 ±1 at% as expected for KNiCl<sub>3</sub> before it being tested as a cathode in a Li thermal battery as shown in Figure 6.4a. The elemental analysis of KNiCl<sub>3</sub> cathode electrode after testing is K 14 ±2 at%, Ni 5 ±2 at% and Cl 81 ±2 at% (Figure 6.4b) and this means that the metals have been reduced, producing species such as Ni metal, KCl and LiCl. These products will be investigated at a later stage by powder X-ray diffraction.

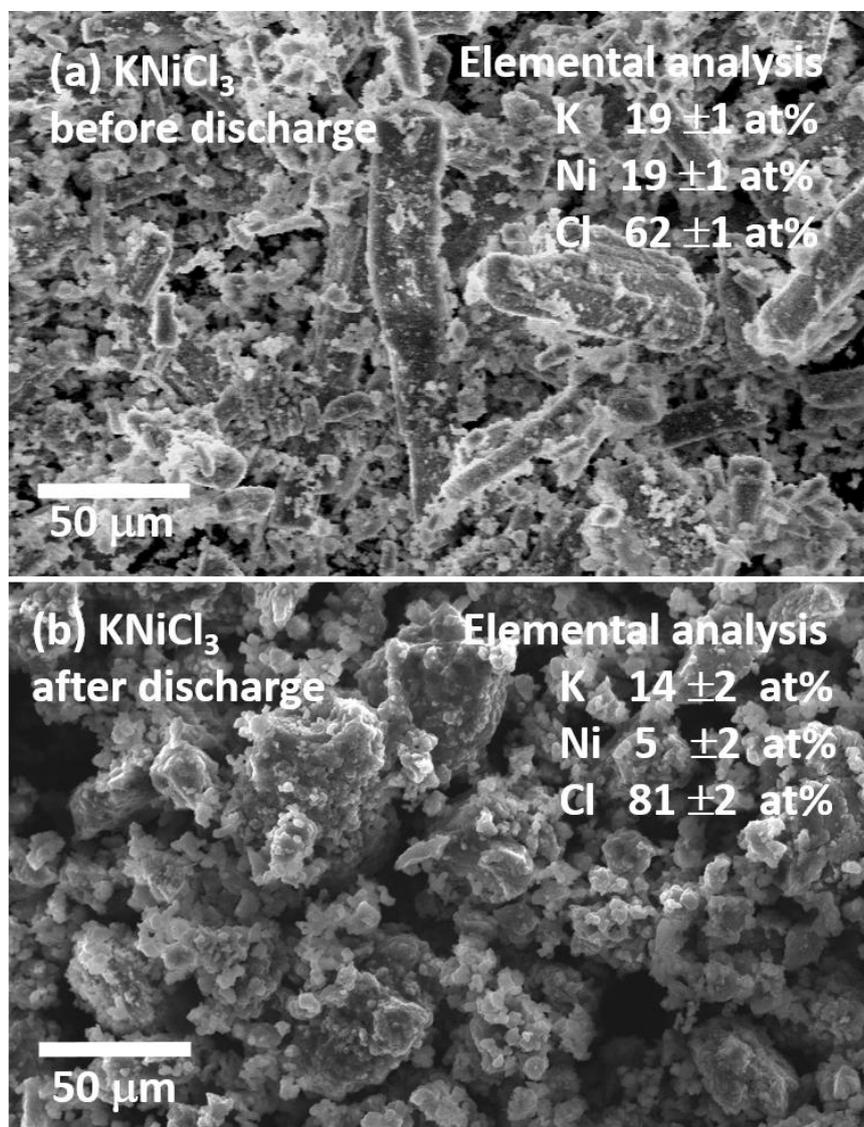
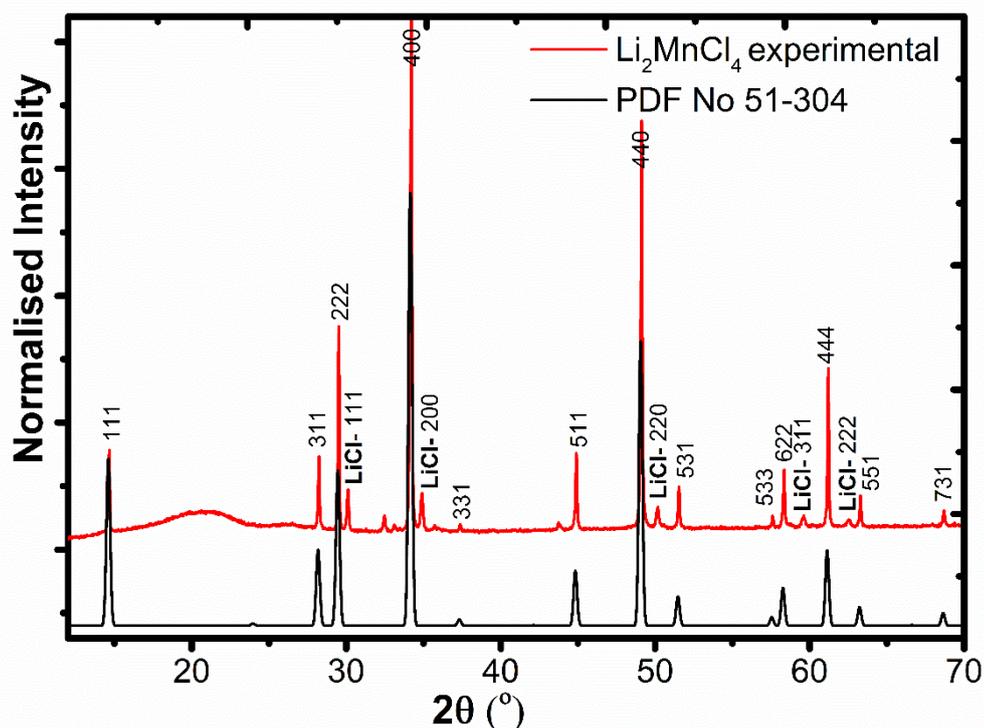


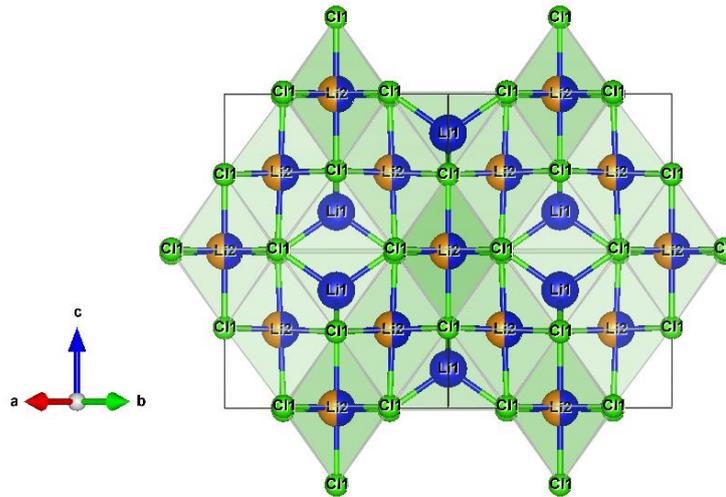
Figure 6.4. SEM images of  $\text{KNiCl}_3$  before (a) and after (b) discharge

6.1.2  $\text{Li}_2\text{MnCl}_4$ 

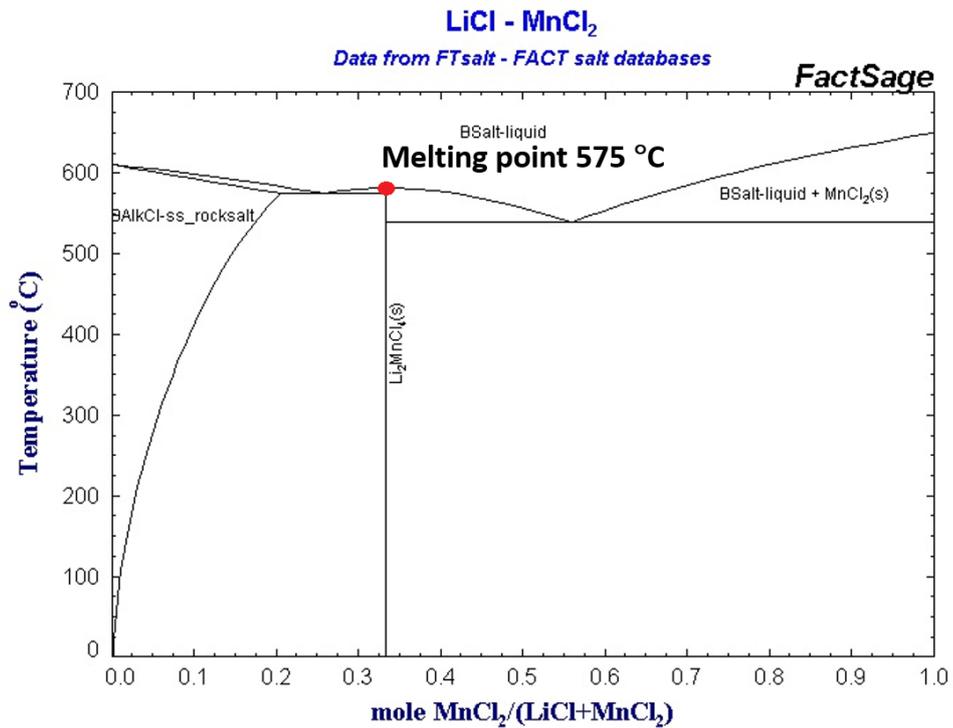
$\text{Li}_2\text{MnCl}_4$  was analysed by powder X-ray diffraction and the diffraction pattern is shown in Figure 6.5.  $\text{Li}_2\text{MnCl}_4$  was identified as the main phase but there is also a LiCl impurity ( $a = 5.140(10) \text{ \AA}$ ) from the starting material, which did not react during the synthesis.  $\text{Li}_2\text{MnCl}_4$  crystallises in cubic  $Fd\bar{3}m$  with unit cell parameters ( $a = 10.495(7) \text{ \AA}$ ), as shown in Figure 6.6.  $\text{Li}_2\text{MnCl}_4$  adopts an inverse spinel structure with half of the lithium ions tetrahedrally coordinated by chlorine ions and the remaining Li atoms, together with the Mn ions, are distributed statistically over the occupied octahedral sites [7 - 8]. The phase diagram, as shown in Figure 6.7, shows the melting point of  $\text{Li}_2\text{MnCl}_4$  at  $575 \text{ }^\circ\text{C}$  [9].



**Figure 6.5.** PXRD data of  $\text{Li}_2\text{MnCl}_4$  at room temperature. Experimental pattern is shown by the red line and the simulated diffraction pattern using published crystallographic model [10] is shown by the black line. Impurity is LiCl

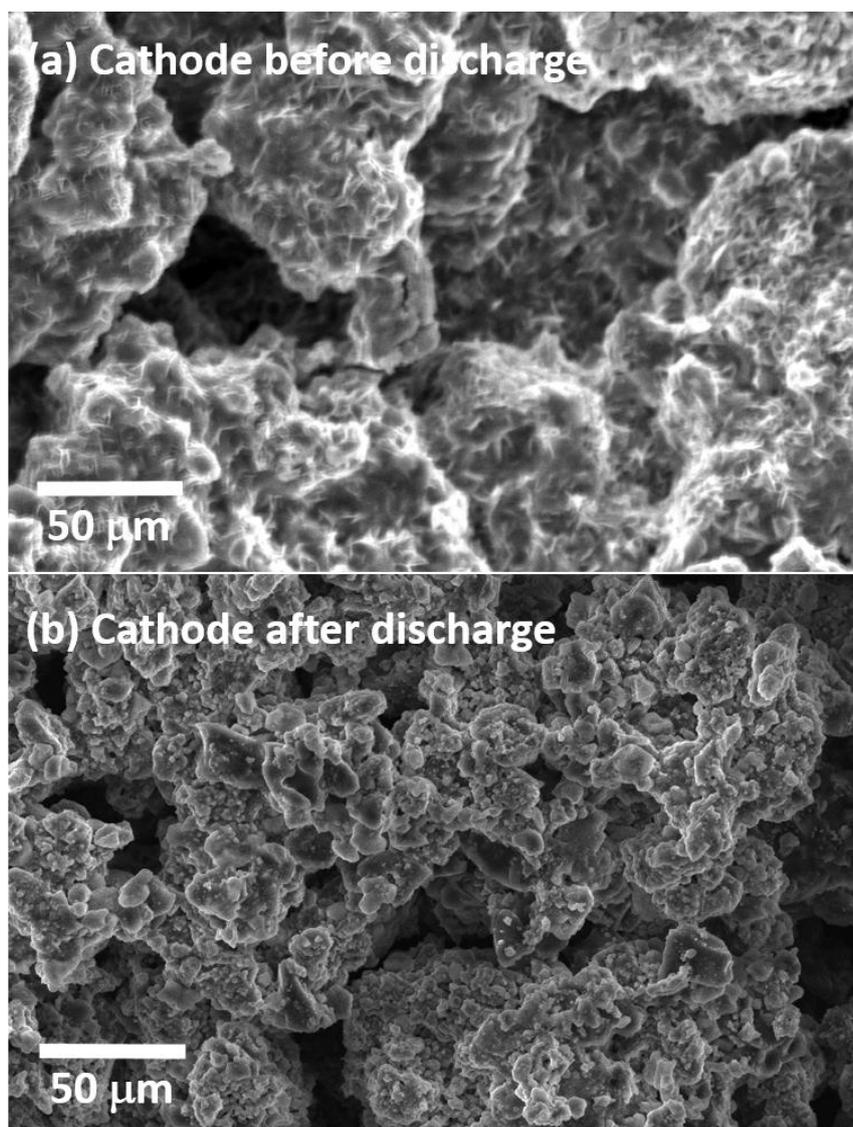


**Figure 6.6.** Crystal structure of  $\text{Li}_2\text{MnCl}_4$ . Green atoms are chlorine, blue atoms are lithium, orange atoms are manganese



**Figure 6.7.** Phase diagram of  $\text{MnCl}_2 - \text{LiCl}$  system [9]

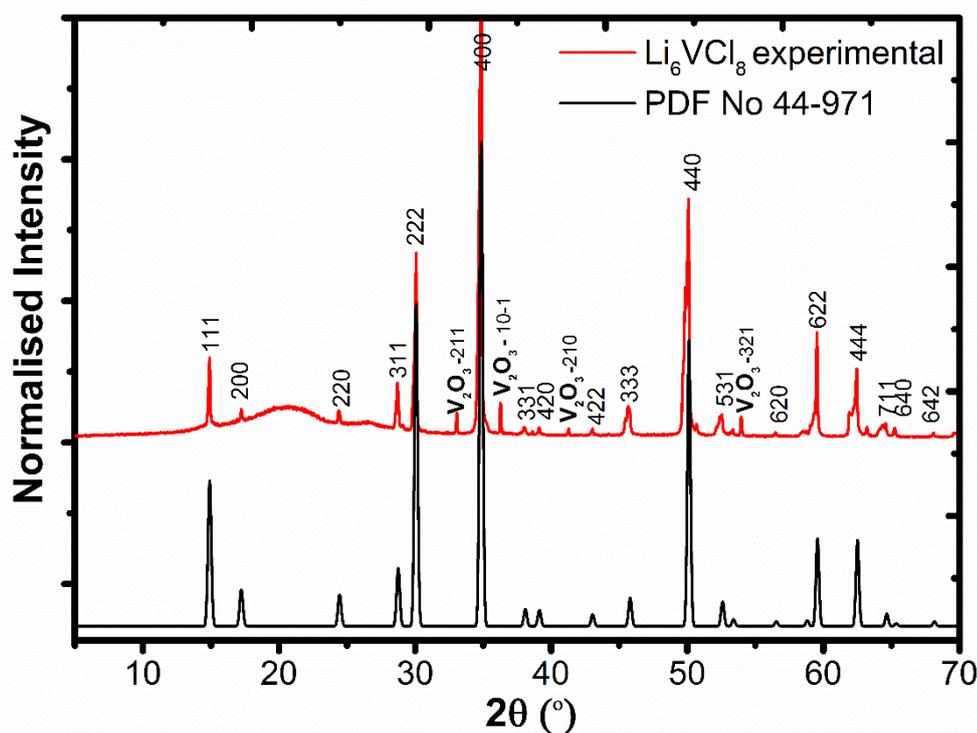
The morphology of  $\text{Li}_2\text{MnCl}_4$  was investigated by SEM before and after discharge and images are shown in Figures 6.8a and 6.8b. The SEM images show that the morphology has been changed after the discharge. However, there is no difference that could be observed in the size of the crystallites.



**Figure 6.8.** SEM images of  $\text{Li}_2\text{MnCl}_4$  before (a) and after (b) discharge

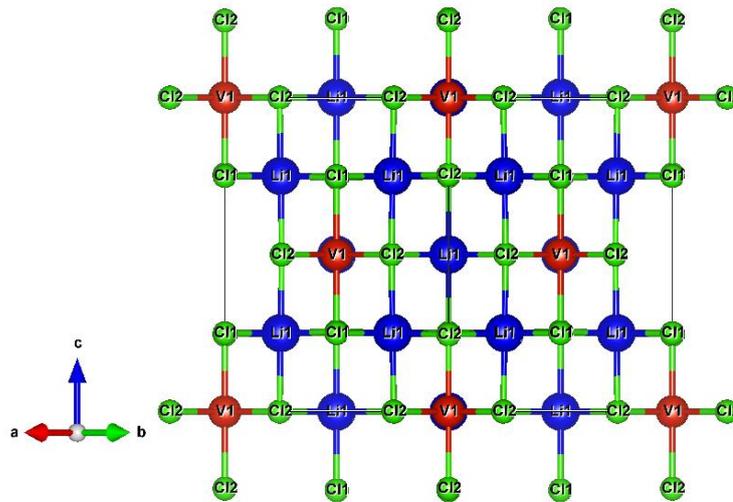
6.1.3  $\text{Li}_6\text{VCl}_8$ 

The diffraction pattern is shown in Figure 6.9. In the synthesis of  $\text{Li}_6\text{VCl}_8$  the main phase corresponded to  $\text{Li}_6\text{VCl}_8$  but there is also a  $\text{V}_2\text{O}_3$  impurity ( $a = 4.948(7) \text{ \AA}$ ,  $c = 13.989(20) \text{ \AA}$ ). As the synthesis of  $\text{Li}_6\text{VCl}_8$  was in a sealed quartz tube this work suggests that the  $\text{V}_2\text{O}_3$  arises as an impurity in the synthesis of the  $\text{VCl}_2$  reagent during the decomposition  $\text{VCl}_3$  to  $\text{VCl}_2$ .  $\text{Li}_6\text{VCl}_8$  crystallises in cubic  $Fm\bar{3}m$  with cell parameter ( $a = 10.294(5) \text{ \AA}$ ) as shown in Figure 6.10. The phase diagram, as shown in Figure 6.11, shows the melting point of  $\text{Li}_6\text{VCl}_8$  at  $763 \text{ }^\circ\text{C}$  [11].

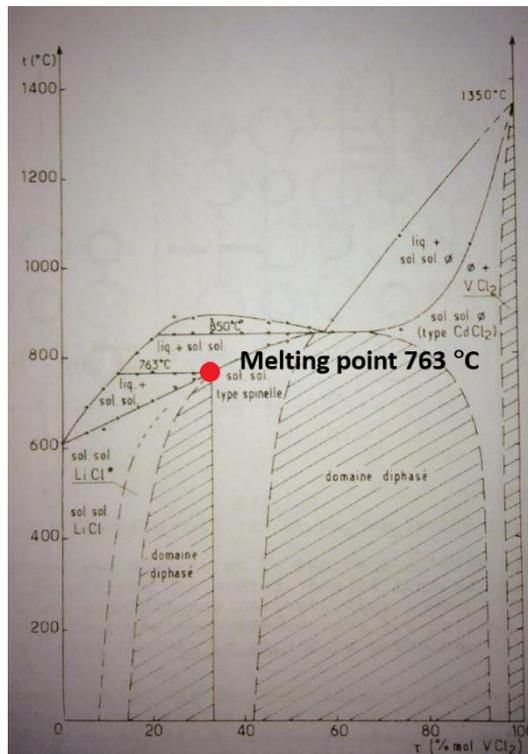


**Figure 6.9.** PXRD data of  $\text{Li}_6\text{VCl}_8$  at room temperature. Experimental pattern is shown by the red line and the simulated diffraction pattern using published crystallographic model [11] is shown by the black line. Impurity is  $\text{V}_2\text{O}_3$

## Chapter 6: Transition Metal Chloride Cathodes



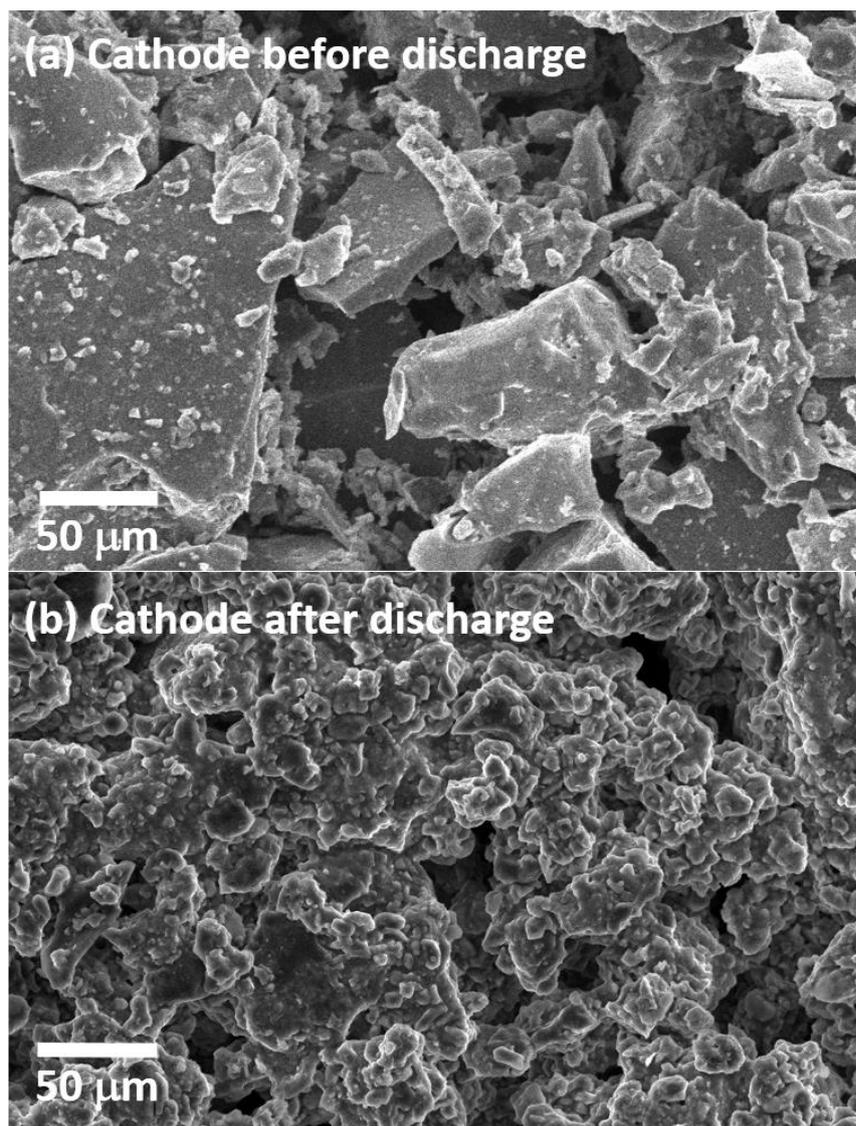
**Figure 6.10.** Crystal structure of  $\text{Li}_6\text{VCl}_8$ . Green atoms are chlorine, blue atoms are lithium and red atoms are vanadium



**Figure 6.11.** Phase diagram of  $\text{VCl}_2 - \text{LiCl}$  system

(permission by Hanebali L, Machej T, Cros C and Hagenmuller P) [11]

The morphology of  $\text{Li}_6\text{VCl}_8$  was studied by SEM before and after discharge and results are presented in Figures 6.12a and 6.12b. SEM images show that the morphology has been changed after the discharge and the size of the crystallites differs. The size of the crystallites is bigger than  $50\ \mu\text{m}$  before the discharge. However, the size of the crystallites is smaller than  $50\ \mu\text{m}$  after the discharge.

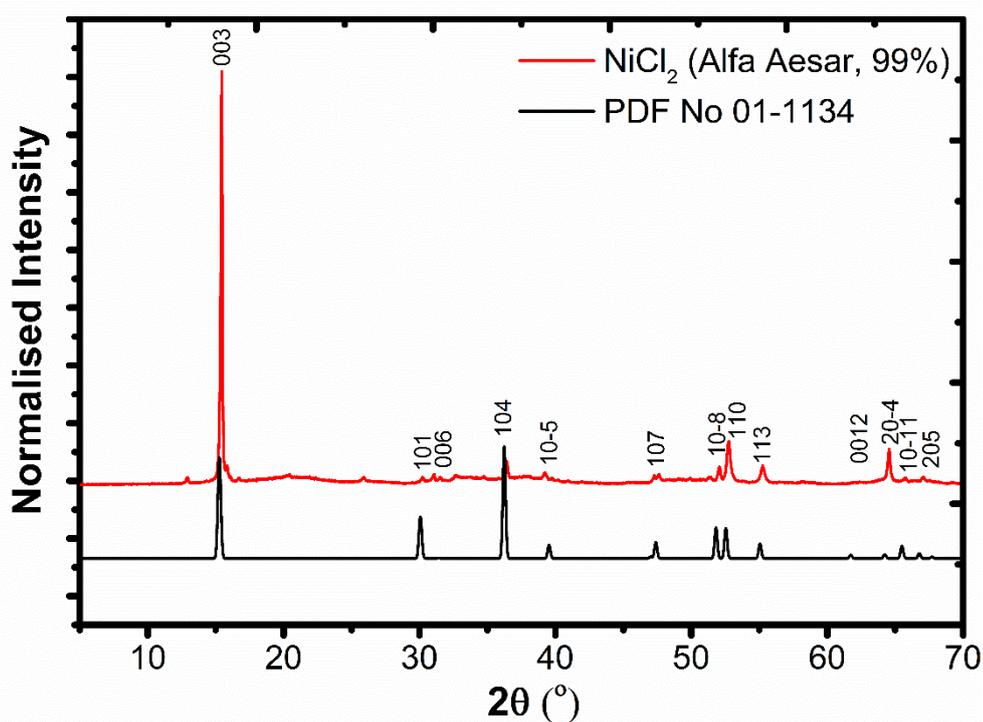


**Figure 6.12.** SEM images of  $\text{Li}_6\text{VCl}_8$  before (a) and after (b) discharge

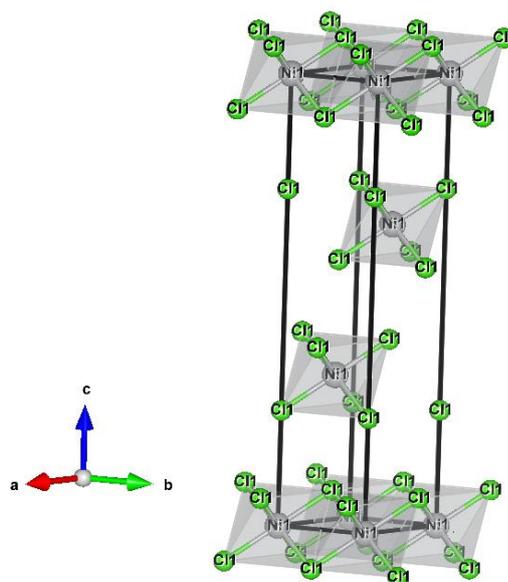
All the samples were studied electrochemically with the impurities (LiCl and KCl) as the electrolyte LiCl-KCl eutectic which is used, consists of KCl and LiCl.

#### 6.1.4 NiCl<sub>2</sub>

NiCl<sub>2</sub> (Alfa Aesar, 99%) was analysed by powder X-ray diffraction and the resulting diffraction pattern is presented in Figure 6.13. NiCl<sub>2</sub> was identified as the main phase and crystallises in trigonal  $R\bar{3}m$  with cell dimensions ( $a = b = 3.468(21)$  Å and  $c = 17.30(7)$  Å). NiCl<sub>2</sub> adopts a layer structure, in which each Ni<sup>2+</sup> is coordinated to six Cl<sup>-</sup> and each chloride is bonded to three Ni as shown in Figure 6.14 [12]. The NiCl<sub>6</sub> octahedra are shared with other octahedra in such a way as to form layers along  $c$ -axis. The melting point of NiCl<sub>2</sub> is 1030 °C [13].



**Figure 6.13.** PXRD data of NiCl<sub>2</sub> at room temperature. Experimental pattern is shown by the red line and the simulated diffraction pattern using published crystallographic model [14] is shown by the black line



**Figure 6.14.** Crystal structure of NiCl<sub>2</sub>. Green atoms are chlorine and grey atoms are nickel

SEM images, as shown in Figures 6.15a and 6.15b, show the morphology and the size of crystallites before and after testing. EDX confirms Ni  $30 \pm 2$  at% and Cl  $70 \pm 2$  at% as expected for NiCl<sub>2</sub> before it being tested as a cathode in a Li thermal battery, as shown in Figure 6.15a. The elemental analysis of NiCl<sub>2</sub> cathode electrode after testing is Ni  $62 \pm 1$  at% and Cl  $38 \pm 1$  at% (Figure 6.15b) and this means different products of the electrochemical mechanism are formed, such as Ni metal and LiCl. These products will be investigated at a later stage by powder X-ray diffraction.

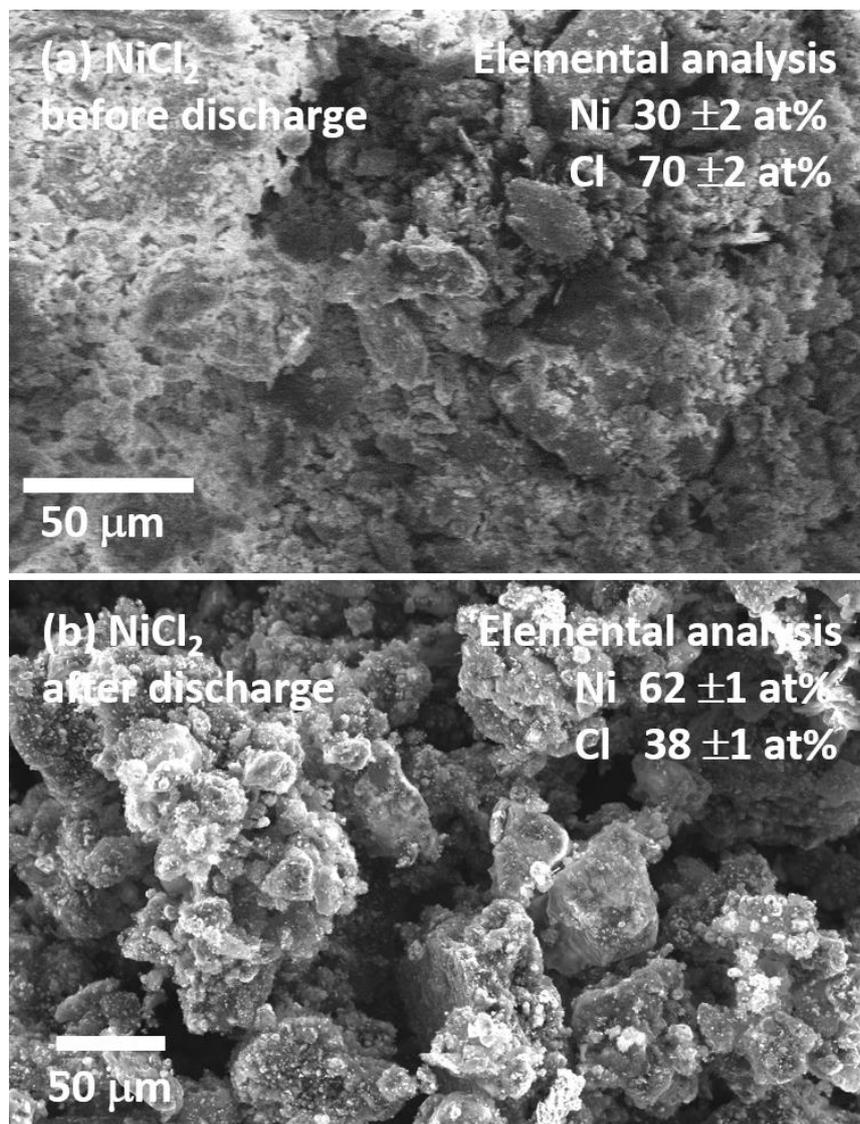
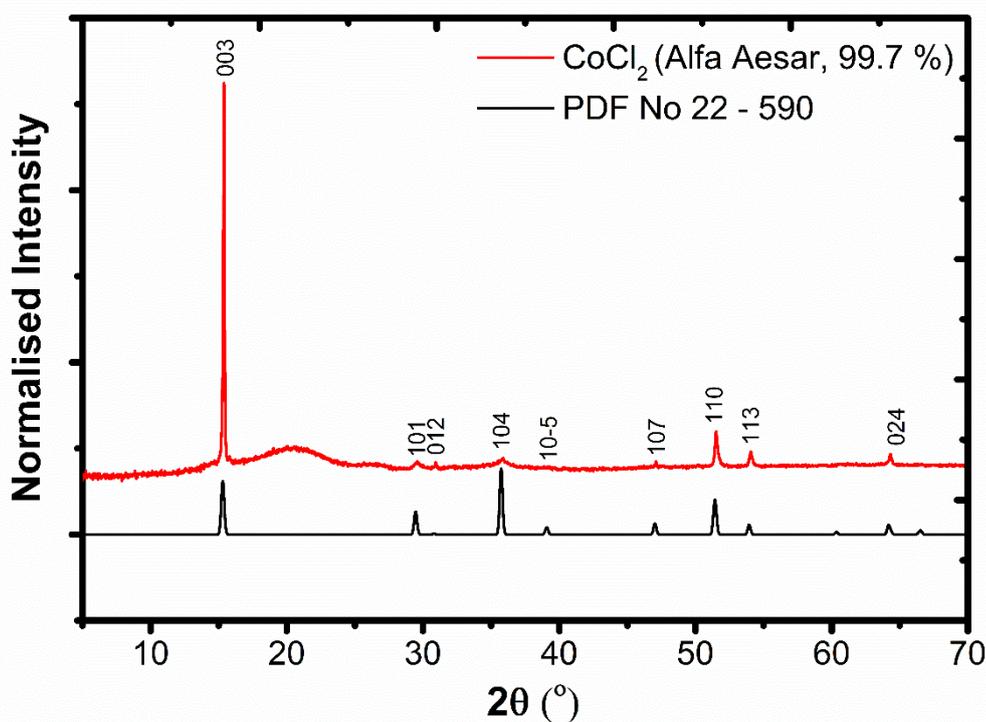


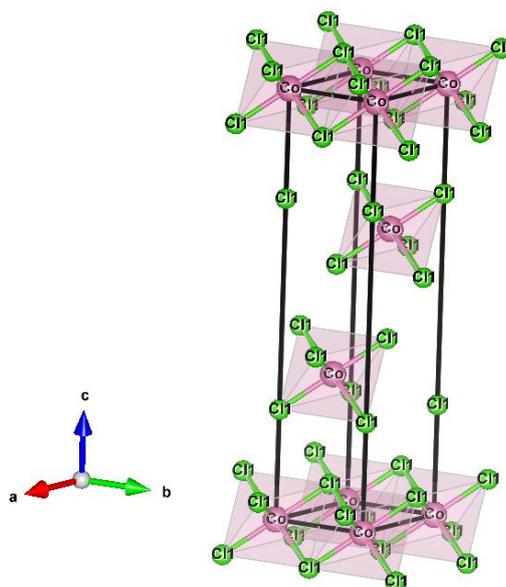
Figure 6.15. SEM images of  $\text{NiCl}_2$  before (a) and after (b) discharge

6.1.5 CoCl<sub>2</sub>

CoCl<sub>2</sub> (Alfa Aesar, 99.7 %) was analysed by powder X-ray diffraction and the resulting diffraction pattern is presented in Figure 6.16. CoCl<sub>2</sub> was identified as the main phase and crystallises in hexagonal  $R\bar{3}m$  with cell dimensions ( $a = b = 3.55(7)$  Å and  $c = 17.36(9)$  Å). CoCl<sub>2</sub> adopts the same structure as NiCl<sub>2</sub>, as shown in Figure 6.17. The melting point of CoCl<sub>2</sub> is 740 °C [15].

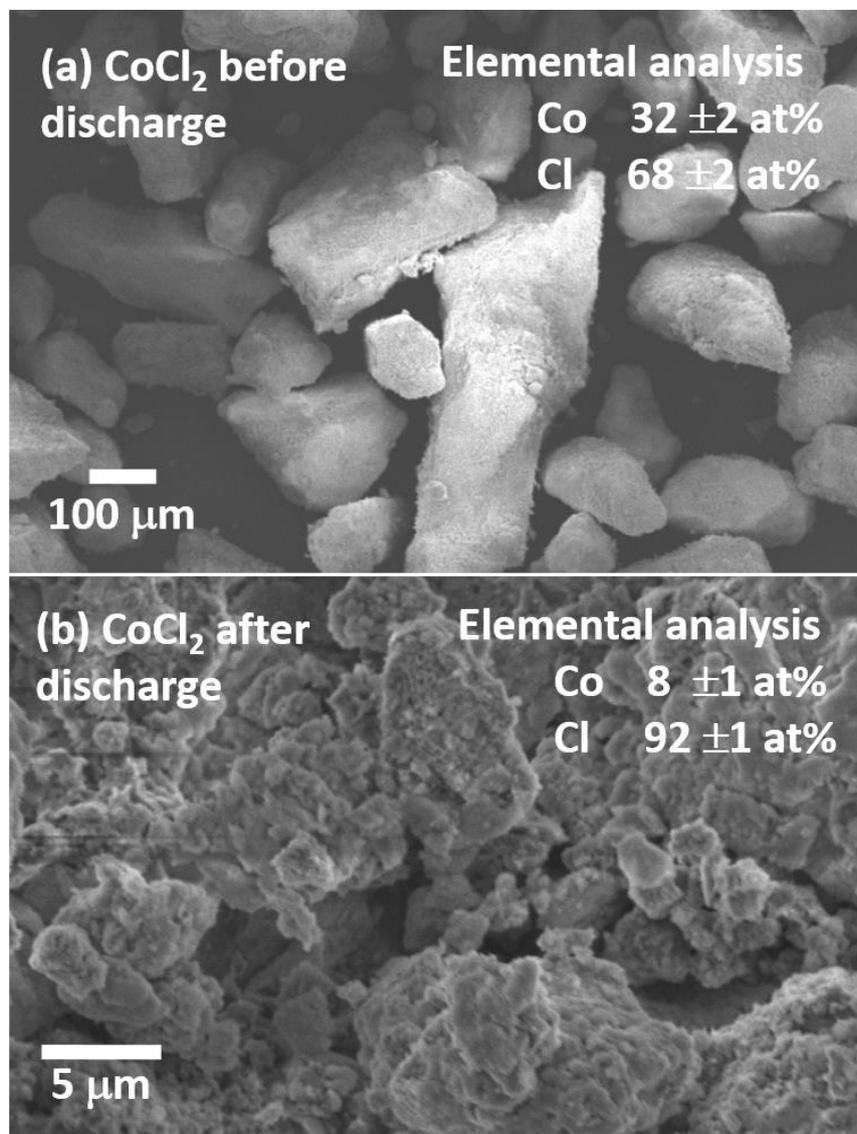


**Figure 6.16.** PXRD data of CoCl<sub>2</sub> at room temperature. Experimental pattern is shown by the red line and the simulated diffraction pattern using published crystallographic model [16] is shown by the black line



**Figure 6.17.** Crystal structure of CoCl<sub>2</sub>. Green atoms are chlorine and pink atoms are cobalt

The morphology and the size of crystallites of CoCl<sub>2</sub> was studied by SEM as shown in Figures 6.18a and 6.18b. The morphology and the size of the crystallites have been changed after the discharge. EDX confirms Co  $32 \pm 2$  at% and Cl  $68 \pm 2$  at% as expected for CoCl<sub>2</sub> before it being tested as a cathode in a Li thermal battery, as shown in Figure 6.18a. The elemental analysis of CoCl<sub>2</sub> cathode electrode after testing is Co  $8 \pm 1$  at% and Cl  $92 \pm 1$  at% (Figure 6.18b) and this means different products of the electrochemical mechanism are formed, such as Co metal and LiCl. These products will be investigated at a later stage by powder X-ray diffraction.



**Figure 6.18.** SEM images of CoCl<sub>2</sub> before (a) and after (b) discharge

## 6.2 Electrochemical Investigation of Transition Metal Chlorides

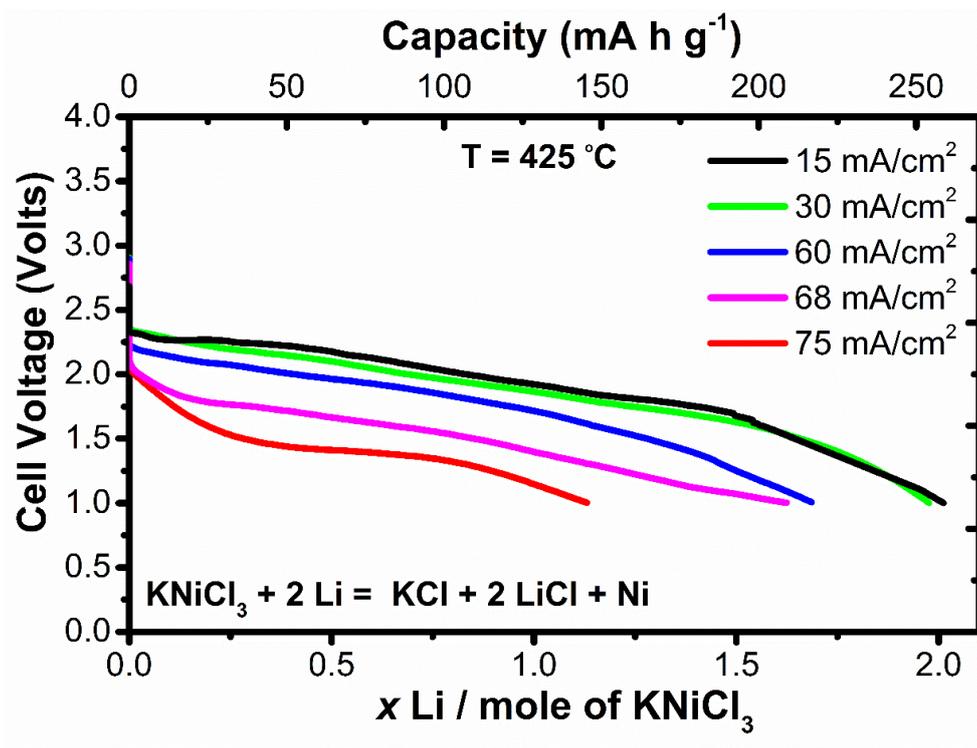
All transition metal chlorides were studied electrochemically by galvanostatic discharge and galvanostatic intermittent titration technique.

### 6.2.1 KNiCl<sub>3</sub>

Galvanostatic discharge curves for measurements carried out at 425 °C for KNiCl<sub>3</sub> are presented in Figure 6.19. Galvanostatic discharge was performed at different current densities from 15 mA/cm<sup>2</sup> to 75 mA/cm<sup>2</sup> and the voltage cut-off was 1 V. At current densities of 15, 30 and 60 mA/cm<sup>2</sup> there is a high cell voltage (2.30 V) but a flat voltage plateau could not be obtained. At current densities of 68 and 75 mA/cm<sup>2</sup> the cell voltage is lower which is probably due to a higher cell resistance as confirmed at a later stage by GITT. A capacity of 262 mA h g<sup>-1</sup> was measured for KNiCl<sub>3</sub> and this corresponds to a value of  $x = 2$  for the number of lithium atoms transferred during the discharge process. The electrochemical mechanism corresponds to:



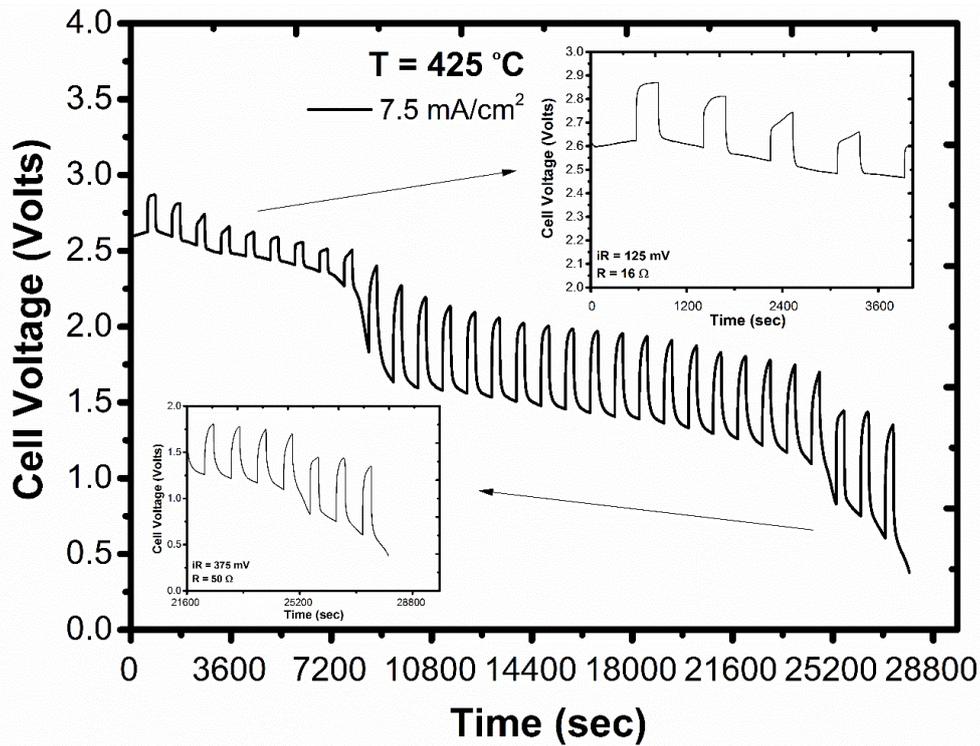
This electrochemical reaction [6.1] is expected as it is analogous to the system Na/NaAlCl<sub>4</sub>/NiCl<sub>2</sub> [17]. Capacities of 259, 220, 210 and 150 mA h g<sup>-1</sup> were measured at a current densities of 30, 60, 68 and 75 mA/cm<sup>2</sup>, respectively. The amount of active anode (0.15 g) corresponds to 73 mA h for the discharge plateau from Li<sub>13</sub>Si<sub>4</sub> to Li<sub>7</sub>Si<sub>3</sub> which is 0.157 V vs Li. The measured capacity of the cathode is 39.3 mA h which keeps the discharge as being performed against the 0.157 V Li plateau.



**Figure 6.19.** Galvanostatic discharge of  $\text{KNiCl}_3$  at current densities of 15, 30, 60, 68 and 75  $\text{mA}/\text{cm}^2$  at 425 °C

Galvanostatic intermittent titration technique curve for a measurement at 425 °C of  $\text{KNiCl}_3$  is shown in Figure 6.20. The galvanostatic intermittent titration technique measurements (GITT) show the IR drop is 125 mV at the beginning of discharge and 375 mV at the end of the measurement, which indicates that the cell resistance is increasing during the reduction of the cathode, from a resistance of 16  $\Omega$  at the beginning of the measurement to 50  $\Omega$  after the cell discharge, which suggests that it is more difficult for the lithium ions to transfer from the anode to the cathode electrode. The voltage profile is still high at 2.5 V at a current density of 7.5  $\text{mA}/\text{cm}^2$ .

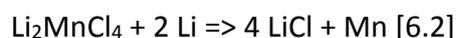
The chemical diffusion coefficient  $D = 3.82 \cdot 10^{-6} \text{ cm}^2 \text{ s}^{-1}$  for  $\text{KNiCl}_3$  can be calculated from equation [3.1] where  $n_m = 0.000979$  (mol),  $V_m = 71.88$  ( $\text{cm}^3 / \text{mol}$ ),  $\Delta E_s = 0.060$  (V) and  $\Delta E_t = 0.075$  (V).

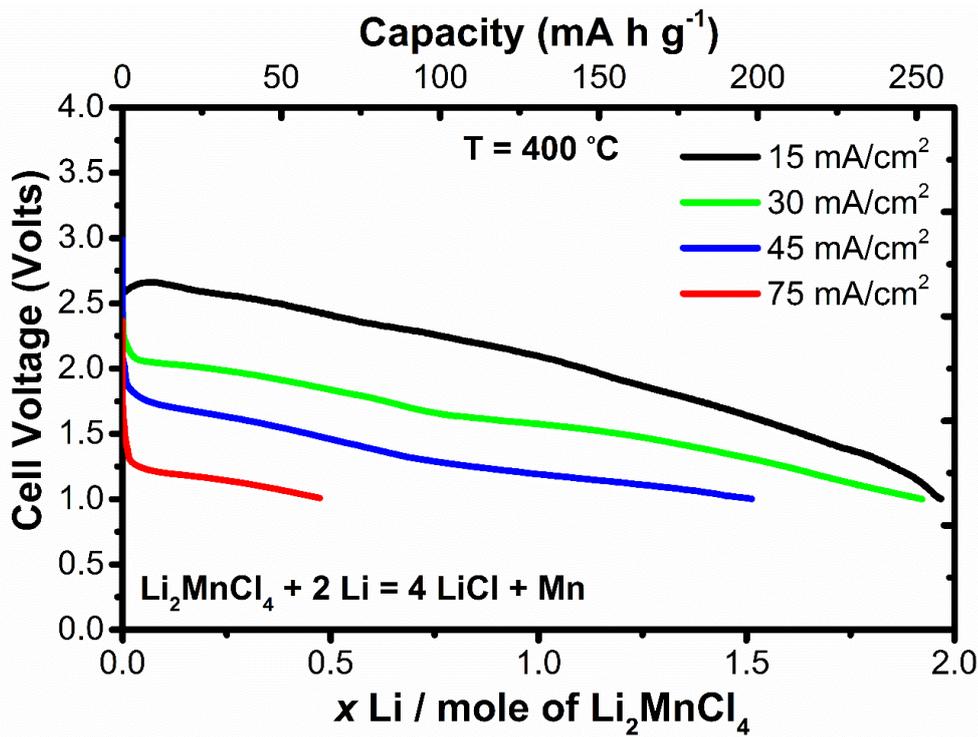


**Figure 6.20.** Galvanostatic intermittent titration technique of  $\text{KNiCl}_3$  at current density of  $7.5 \text{ mA/cm}^2$  at  $425 \text{ }^\circ\text{C}$

### 6.2.2 $\text{Li}_2\text{MnCl}_4$

Galvanostatic discharge curves for measurements carried out at  $400 \text{ }^\circ\text{C}$  for  $\text{Li}_2\text{MnCl}_4$  are presented in Figure 6.21. Galvanostatic discharge was performed at different current densities from  $15 \text{ mA/cm}^2$  to  $75 \text{ mA/cm}^2$  and the voltage cut-off was  $1 \text{ V}$ . At a current density of  $15 \text{ mA/cm}^2$  there is a high cell voltage ( $2.50 \text{ V}$ ) similar to  $\text{KNiCl}_3$  but again a flat voltage plateau could not be obtained. At current densities of  $30$ ,  $45$  and  $75 \text{ mA/cm}^2$  the cell voltage is lower which is probably due to a higher cell resistance as confirmed at a later stage by GITT.  $\text{Li}_2\text{MnCl}_4$  exhibits a maximum capacity of  $254 \text{ mA h g}^{-1}$  and the electrochemical mechanism corresponds to:

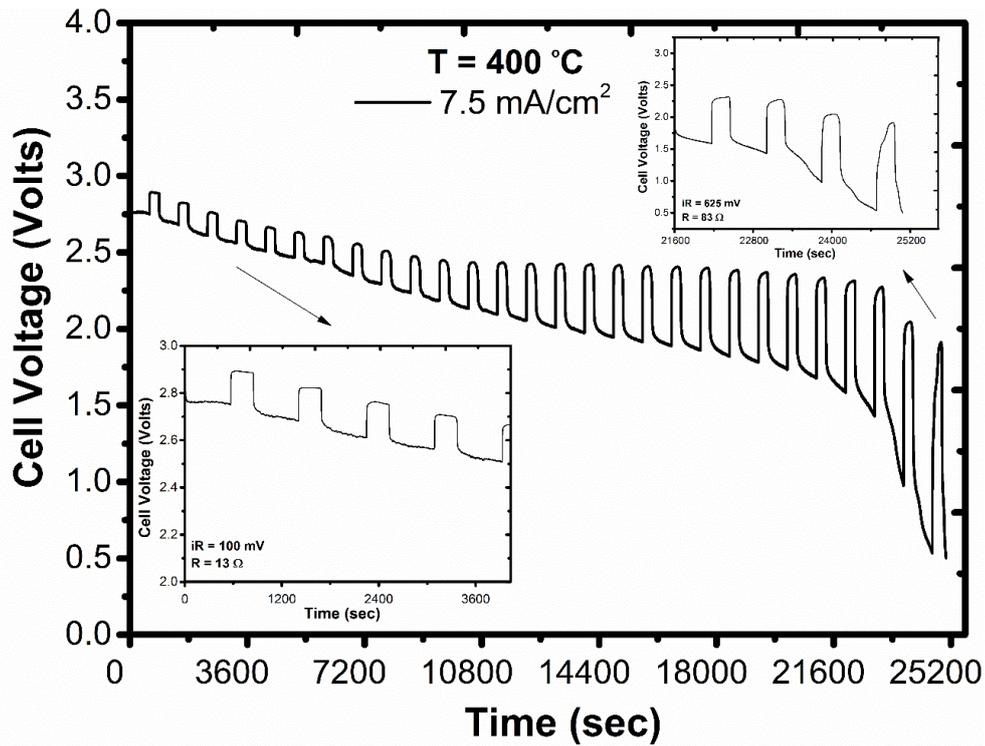




**Figure 6.21.** Galvanostatic discharge of Li<sub>2</sub>MnCl<sub>4</sub> at current densities of 15, 30, 45 and 75 mA/cm<sup>2</sup> at 400 °C

Capacities of 250, 200 and 65 mA h g<sup>-1</sup> were measured at a current densities of 30, 45 and 75 mA/cm<sup>2</sup>, respectively. The amount of active anode (0.15 g) corresponds to 73 mA h for the discharge plateau from Li<sub>13</sub>Si<sub>4</sub> to Li<sub>7</sub>Si<sub>3</sub> which is 0.157 V vs Li. The measured capacity of the cathode is 38.1 mA h which keeps the discharge as being performed against the 0.157 V Li plateau.

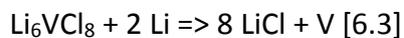
Galvanostatic intermittent titration technique curve for measurements carried out at 400 °C for Li<sub>2</sub>MnCl<sub>4</sub> is presented in Figure 6.22. The IR drop is 100 mV at the beginning of discharge and 625 mV at the end of the measurement, which indicates that the cell resistance is increasing from a resistance of 13 Ω at the beginning of the measurement to 83 Ω after the cell discharge. However, the voltage profile is still high at 2.75 V at a current density of 7.5 mA/cm<sup>2</sup>. The chemical diffusion coefficient  $D = 1.18 \cdot 10^{-5} \text{ cm}^2 \text{ s}^{-1}$  for Li<sub>2</sub>MnCl<sub>4</sub> can be calculated from equation [3.1] where  $n_m = 0.000949 \text{ (mol)}$ ,  $V_m = 87.03 \text{ (cm}^3 / \text{mol)}$ ,  $\Delta E_s = 0.060 \text{ (V)}$  and  $\Delta E_t = 0.050 \text{ (V)}$ .

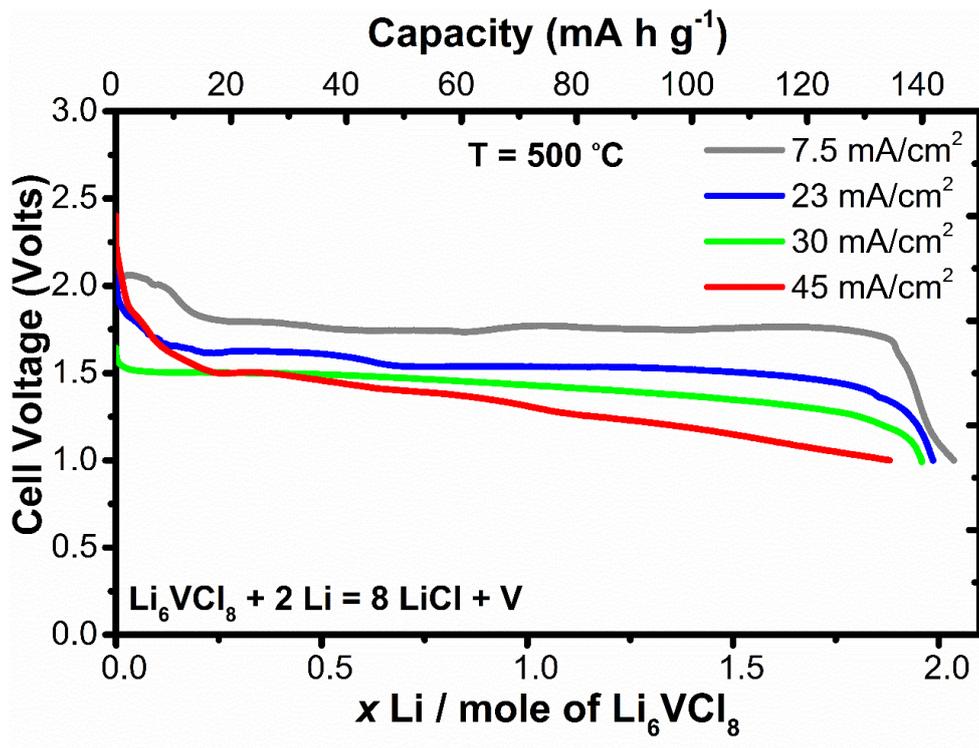


**Figure 6.22.** Galvanostatic intermittent titration technique of  $\text{Li}_2\text{MnCl}_4$  at current density of  $7.5 \text{ mA/cm}^2$  at  $400 \text{ }^\circ\text{C}$

### 6.2.3 $\text{Li}_6\text{VCl}_8$

Galvanostatic discharge curves for measurements carried out at  $500 \text{ }^\circ\text{C}$  for  $\text{Li}_6\text{VCl}_8$  are presented in Figure 6.23. Galvanostatic discharge was performed at different current densities from  $7.5 \text{ mA/cm}^2$  to  $45 \text{ mA/cm}^2$  and the voltage cut-off was 1 V. At a current density of  $7.5 \text{ mA/cm}^2$  there is a flat voltage plateau at 1.80 V and a capacity of  $145 \text{ mA h g}^{-1}$  was achieved. At current densities of 23 and  $30 \text{ mA/cm}^2$ ,  $\text{Li}_6\text{VCl}_8$  shows a lower but again flat voltage plateau at 1.50 V. However, at a current density of  $45 \text{ mA/cm}^2$  a flat voltage plateau could not be obtained. The electrochemical mechanism corresponds to:



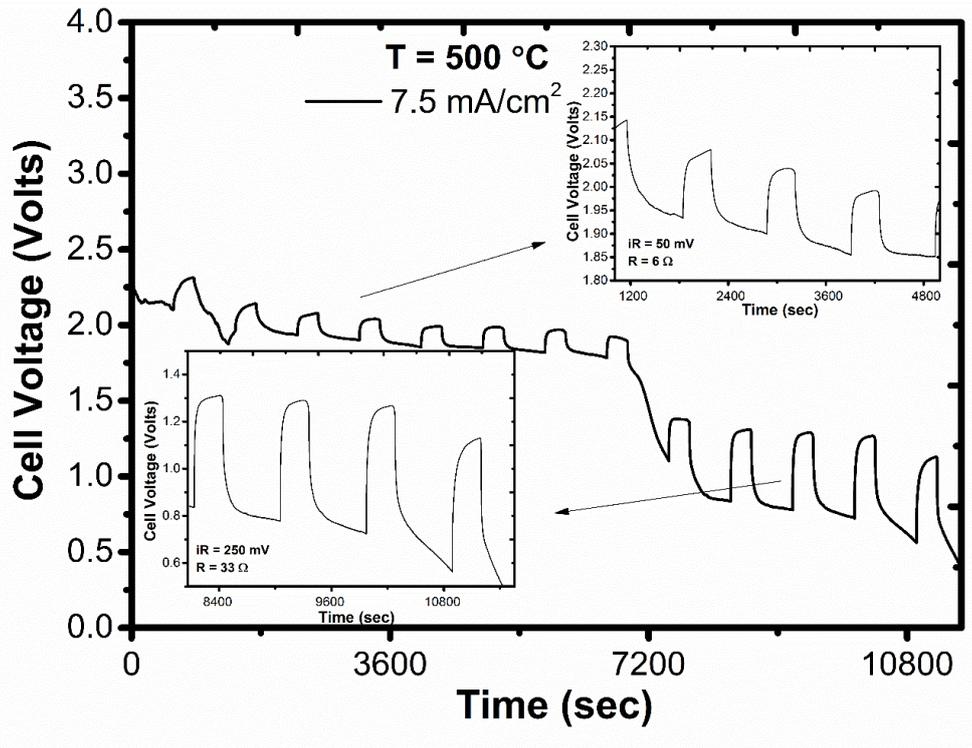


**Figure 6.23.** Galvanostatic discharge of  $\text{Li}_6\text{VCl}_8$  at current densities of 7.5, 23, 30 and 45  $\text{mA}/\text{cm}^2$  at 500 °C

Capacities of 140, 138 and 135  $\text{mA h g}^{-1}$  were measured at a current densities of 23, 30 and 45  $\text{mA}/\text{cm}^2$ , respectively. The amount of active anode (0.15 g) corresponds to 73  $\text{mA h}$  for the discharge plateau from  $\text{Li}_{13}\text{Si}_4$  to  $\text{Li}_7\text{Si}_3$  which is 0.157 V vs Li. The measured capacity of the cathode is 21.75  $\text{mA h}$  which keeps the discharge as being performed against the 0.157 V Li plateau.

Galvanostatic intermittent titration technique curve for a measurement carried out at 500 °C for  $\text{Li}_6\text{VCl}_8$  is presented in Figure 6.24. The cell resistance increases during the reduction of the cathode from 6  $\Omega$  at the beginning to 33  $\Omega$  at the end of discharge.

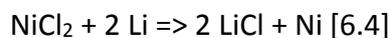
The chemical diffusion coefficient  $D = 5.74 \cdot 10^{-7} \text{ cm}^2 \text{ s}^{-1}$  for  $\text{Li}_6\text{VCl}_8$  can be calculated from equation [3.1] where  $n_m = 0.000531$  (mol),  $V_m = 164.28$  ( $\text{cm}^3 / \text{mol}$ ),  $\Delta E_s = 0.025$  (V) and  $\Delta E_t = 0.100$  (V).

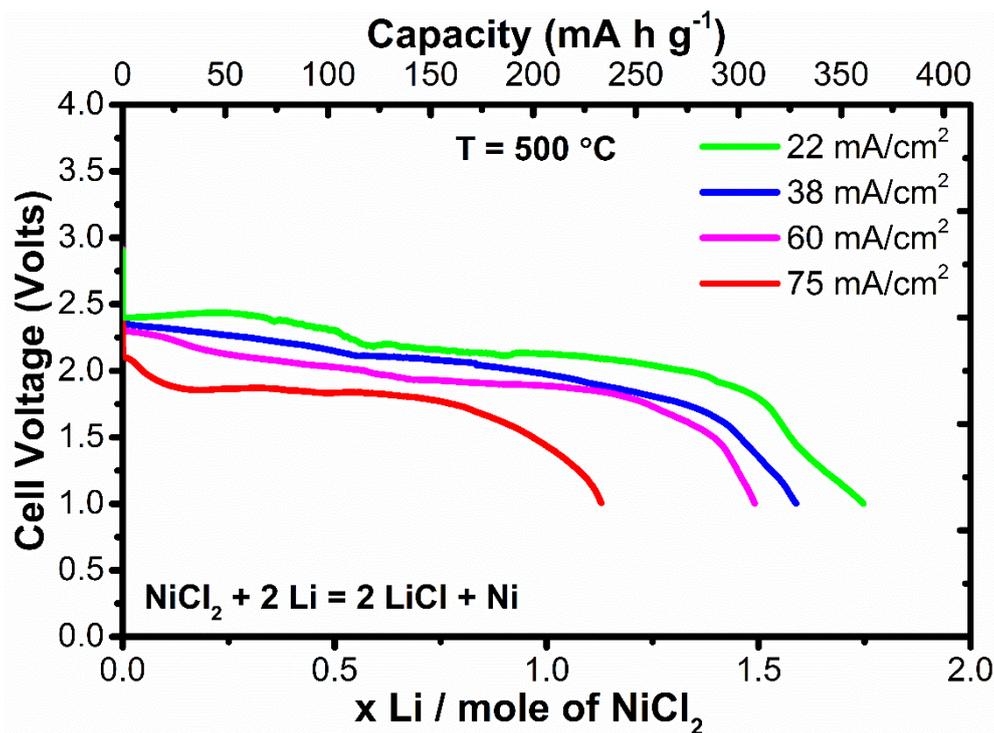


**Figure 6.24.** Galvanostatic intermittent titration technique of  $\text{Li}_6\text{VCl}_8$  at current density of  $7.5 \text{ mA/cm}^2$  at  $500 \text{ }^\circ\text{C}$

#### 6.2.4 $\text{NiCl}_2$

Galvanostatic discharge curves for measurements carried out at  $500 \text{ }^\circ\text{C}$  for  $\text{NiCl}_2$  are presented in Figure 6.25. Galvanostatic discharge was performed at different current densities from  $22 \text{ mA/cm}^2$  to  $75 \text{ mA/cm}^2$  and the voltage cut-off was  $1 \text{ V}$ . At current densities of  $22$ ,  $38$  and  $60 \text{ mA/cm}^2$  there is a high cell voltage over than  $2 \text{ V}$  and a voltage plateau could be obtained. At current densities of  $75 \text{ mA/cm}^2$  the cell voltage is lower which is probably due to a higher cell resistance as confirmed at a later stage by GITT.  $\text{NiCl}_2$  exhibits a capacity of  $360 \text{ mA h g}^{-1}$  and the electrochemical mechanism corresponds to:



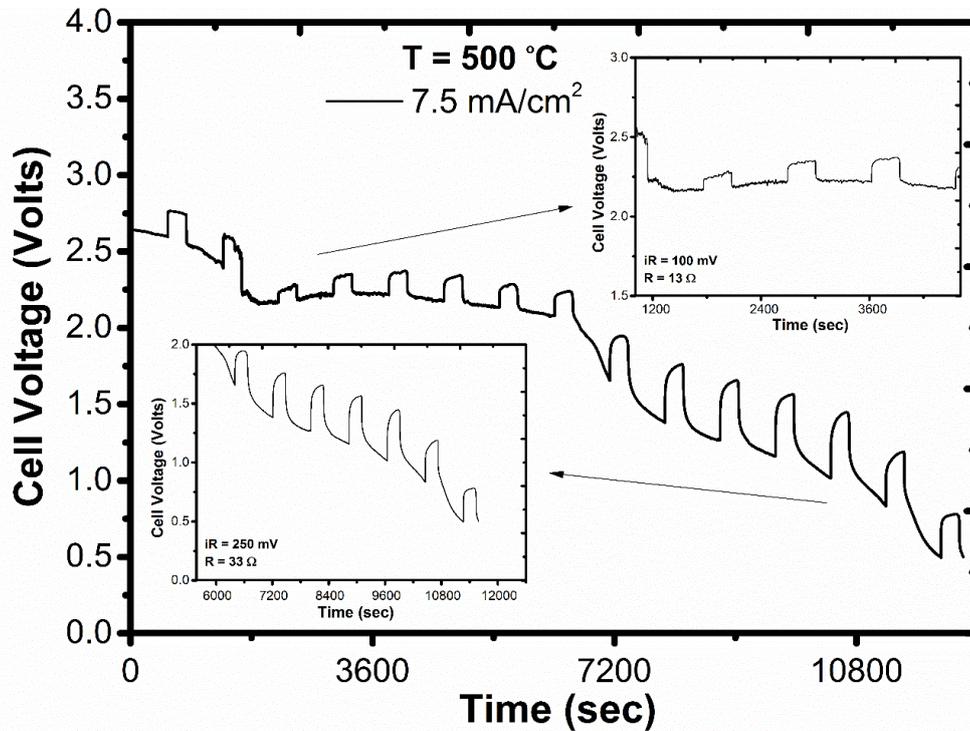


**Figure 6.25.** Galvanostatic discharge of NiCl<sub>2</sub> at current densities of 22, 38, 60 and 75 mA/cm<sup>2</sup> at 500 °C

Capacities of 325, 310 and 230 mA h g<sup>-1</sup> were measured at a current densities of 38, 60 and 75 mA/cm<sup>2</sup>, respectively. The amount of active anode (0.15 g) corresponds to 73 mA h for the discharge plateau from Li<sub>13</sub>Si<sub>4</sub> to Li<sub>7</sub>Si<sub>3</sub> which is 0.157 V vs Li. The measured capacity of the cathode is 54 mA h which keeps the discharge as being performed against the 0.157 V Li plateau.

Galvanostatic intermittent titration technique curve for a measurement at 500 °C of NiCl<sub>2</sub> is shown in Figure 6.26. The galvanostatic intermittent titration technique measurements (GITT) show the IR drop is 100 mV at the beginning of discharge and 250 mV at the end of the measurement, which indicates that the cell resistance is increasing during the reduction of the cathode, from a resistance of 13 Ω at the beginning of the measurement to 33 Ω after the cell discharge, which suggests that it is more difficult for the lithium ions to transfer from the anode to the cathode electrode.

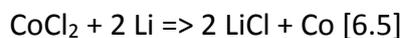
The chemical diffusion coefficient  $D = 8.23 \cdot 10^{-6} \text{ cm}^2 \text{ s}^{-1}$  for  $\text{NiCl}_2$  can be calculated from equation [3.1] where  $n_m = 0.0015 \text{ (mol)}$ ,  $V_m = 36.71 \text{ (cm}^3 \text{ / mol)}$ ,  $\Delta E_s = 0.075 \text{ (V)}$  and  $\Delta E_t = 0.050 \text{ (V)}$ .

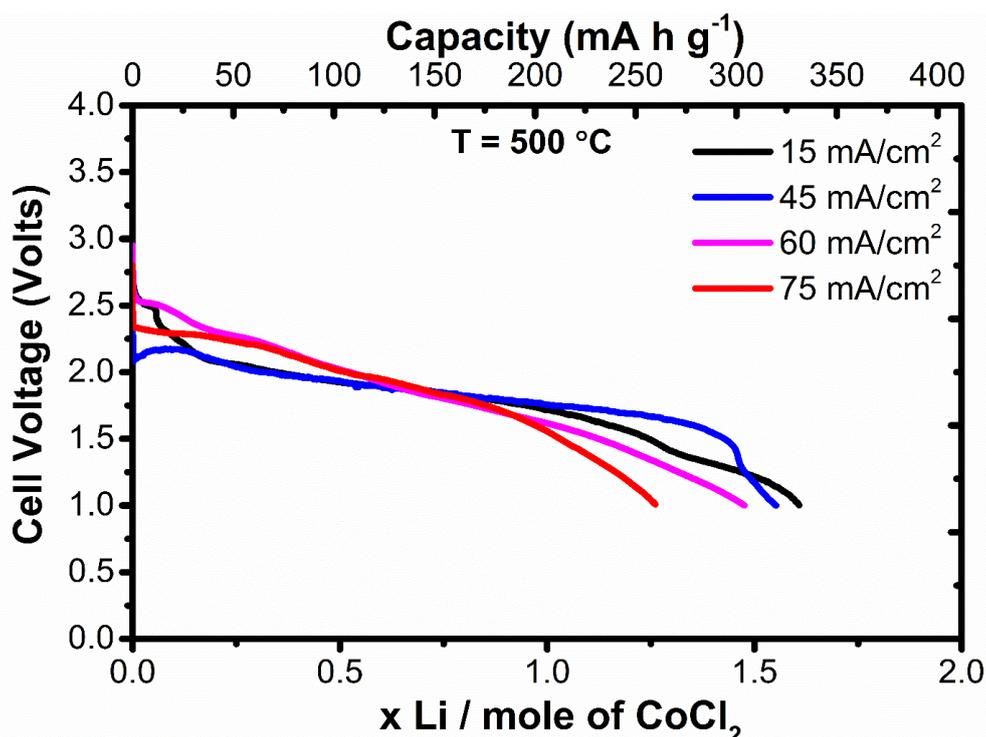


**Figure 6.26.** Galvanostatic intermittent titration technique of  $\text{NiCl}_2$  at current density of  $7.5 \text{ mA/cm}^2$  at  $500 \text{ }^\circ\text{C}$

### 6.2.5 $\text{CoCl}_2$

Galvanostatic discharge curves for measurements carried out at  $500 \text{ }^\circ\text{C}$  for  $\text{CoCl}_2$  are presented in Figure 6.27. Galvanostatic discharge was performed at different current densities from  $15 \text{ mA/cm}^2$  to  $75 \text{ mA/cm}^2$  and the voltage cut-off was  $1 \text{ V}$ . At current densities of  $15$  and  $45 \text{ mA/cm}^2$  there is a high cell voltage around  $2 \text{ V}$  but a flat voltage plateau could not be obtained. At current densities of  $60$  and  $75 \text{ mA/cm}^2$  the cell voltage is still high but again there is no flat voltage plateau.  $\text{CoCl}_2$  exhibits a capacity of  $330 \text{ mA h g}^{-1}$  and the electrochemical mechanism corresponds to:



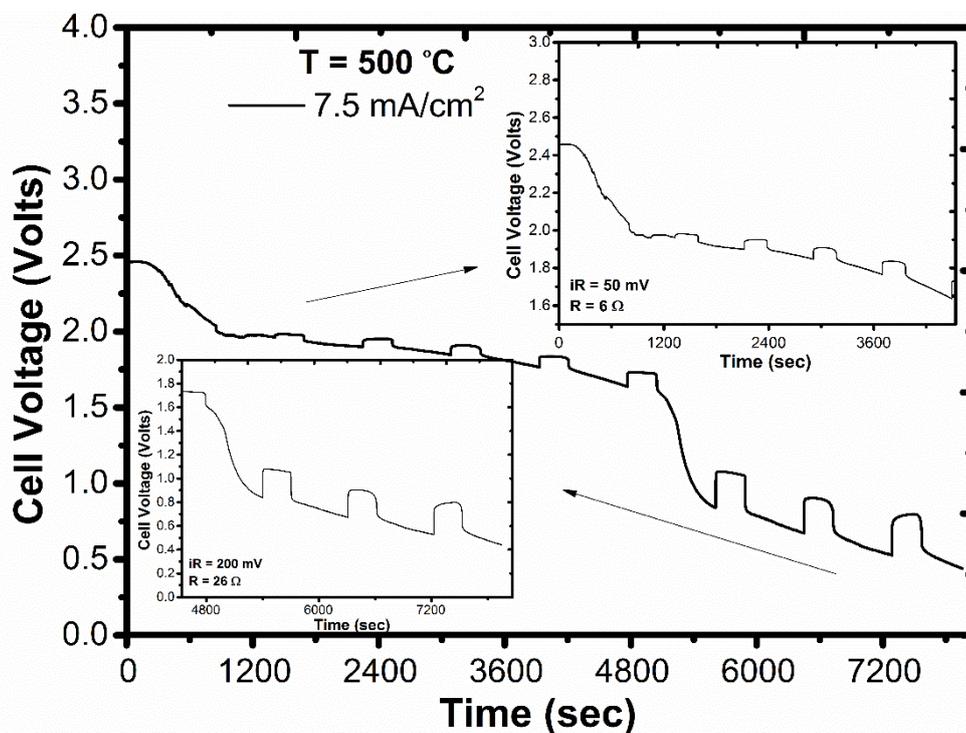


**Figure 6.27.** Galvanostatic discharge of  $\text{CoCl}_2$  at current densities of 15, 45, 60 and 75  $\text{mA}/\text{cm}^2$  at  $500\text{ }^\circ\text{C}$

Capacities of 325, 310 and 260  $\text{mA h g}^{-1}$  were measured at a current densities of 45, 60 and 75  $\text{mA}/\text{cm}^2$ , respectively. The amount of active anode (0.15 g) corresponds to 73  $\text{mA h}$  for the discharge plateau from  $\text{Li}_{13}\text{Si}_4$  to  $\text{Li}_7\text{Si}_3$  which is 0.157 V vs Li. The measured capacity of the cathode is 50  $\text{mA h}$  which keeps the discharge as being performed against the 0.157 V Li plateau.

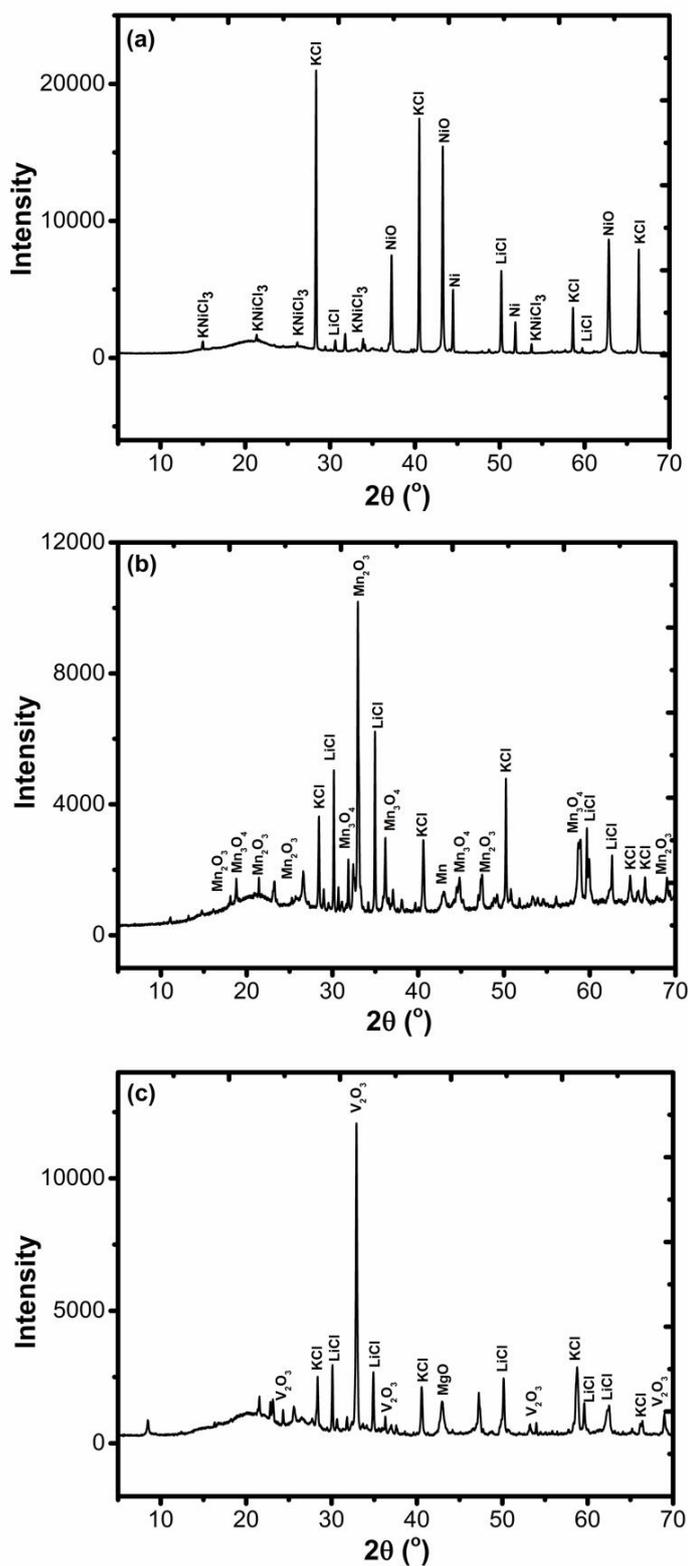
Galvanostatic intermittent titration technique curve for a measurement at  $500\text{ }^\circ\text{C}$  of  $\text{CoCl}_2$  is shown in Figure 6.28. The galvanostatic intermittent titration technique measurements (GITT) show the IR drop is 50 mV at the beginning of discharge and 200 mV at the end of the measurement, which indicates that the cell resistance is increasing during the reduction of the cathode, from a resistance of 6  $\Omega$  at the beginning of the measurement to 26  $\Omega$  after the cell discharge, which suggests that it is more difficult for the lithium ions to transfer from the anode to the cathode electrode.  $\text{CoCl}_2$  compared to  $\text{NiCl}_2$  is more conductive.

The chemical diffusion coefficient  $D = 1.58 \cdot 10^{-5} \text{ cm}^2 \text{ s}^{-1}$  for  $\text{CoCl}_2$  can be calculated from equation [3.1] where  $n_m = 0.0015 \text{ (mol)}$ ,  $V_m = 38.18 \text{ (cm}^3 \text{ / mol)}$ ,  $\Delta E_s = 0.050 \text{ (V)}$  and  $\Delta E_t = 0.025 \text{ (V)}$ .



**Figure 6.28.** Galvanostatic intermittent titration technique of  $\text{CoCl}_2$  at current density of  $7.5 \text{ mA/cm}^2$  at  $500 \text{ }^\circ\text{C}$

PXRD data were collected after discharge for all of the cathodes as shown in Figures 6.29 and 6.30.



**Figure 6.29.** PXRD data of the cathode after galvanostatic discharge of (a) KNiCl<sub>3</sub>, (b) Li<sub>2</sub>MnCl<sub>4</sub>, and (c) Li<sub>6</sub>VCl<sub>8</sub>

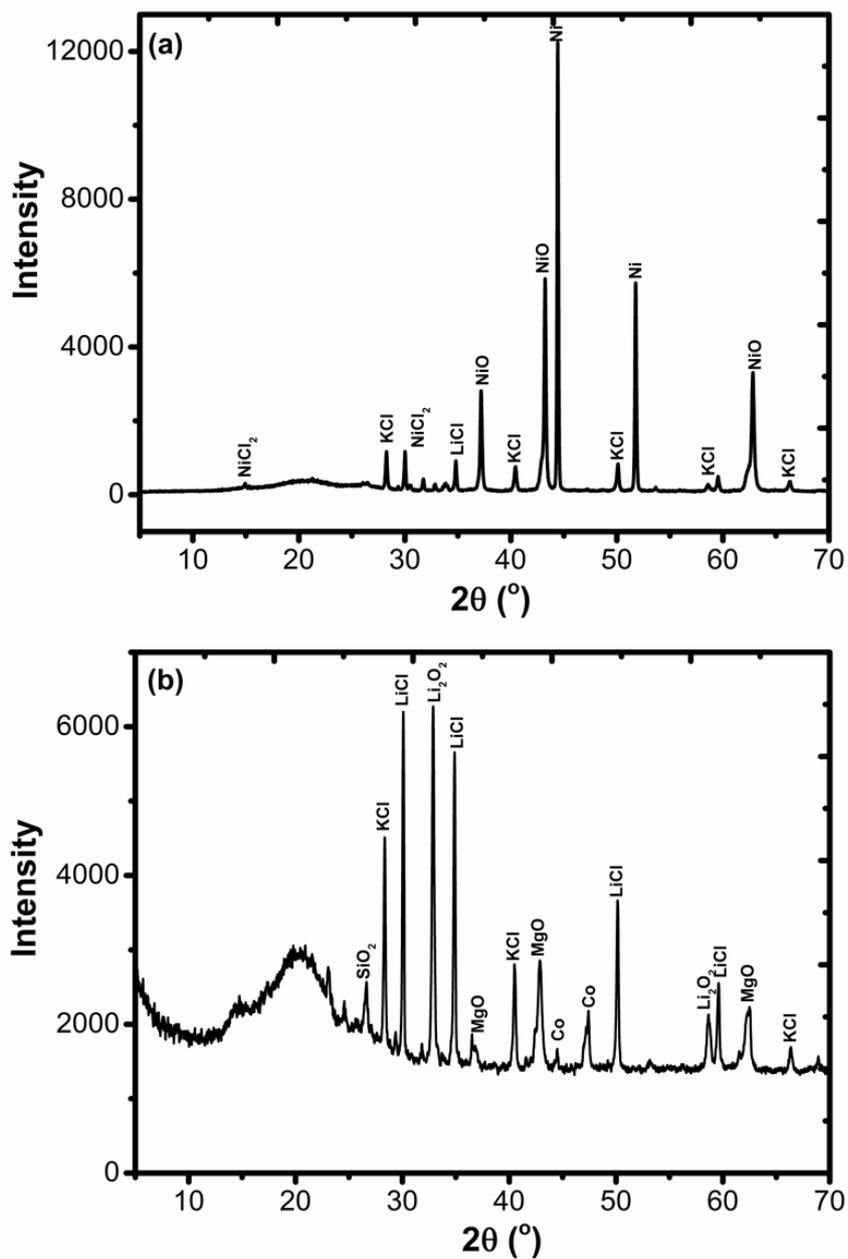


Figure 6.30. XRD data of the cathode after galvanostatic discharge of (a)  $\text{NiCl}_2$  and (b)  $\text{CoCl}_2$

## Chapter 6: Transition Metal Chloride Cathodes

PXRD confirms that the product of the electrochemical reaction of  $\text{KNiCl}_3$  is  $\text{KCl}$  ( $a = 6.292(3) \text{ \AA}$ ),  $\text{Ni}$  metal ( $a = 3.524(7) \text{ \AA}$ ) and  $\text{LiCl}$  as shown in Figure 6.29a. There are some peaks of the starting material  $\text{KNiCl}_3$  ( $a = 11.805(4) \text{ \AA}$  and  $c = 5.935(12) \text{ \AA}$ ) and some peaks of  $\text{NiO}$  ( $a = 4.177(4) \text{ \AA}$ ).

The product of the electrochemical reaction of  $\text{Li}_2\text{MnCl}_4$  is  $\text{LiCl}$  ( $a = 5.142(17) \text{ \AA}$ ) and  $\text{Mn}$  metal ( $a = 8.948(2) \text{ \AA}$ ) as shown in Figure 6.29b. There are some peaks of the electrolyte  $\text{KCl}$  and peaks of  $\text{Mn}_2\text{O}_3$  ( $a = 9.44(5) \text{ \AA}$ ,  $b = 9.55(4) \text{ \AA}$  and  $c = 9.28(3) \text{ \AA}$ ) and  $\text{Mn}_3\text{O}_4$  ( $a = 5.747(3) \text{ \AA}$  and  $c = 9.444(6) \text{ \AA}$ ).

The product of the electrochemical reaction of  $\text{Li}_6\text{VCl}_8$  is  $\text{LiCl}$  ( $a = 5.139(12) \text{ \AA}$ ) and  $\text{V}_2\text{O}_3$  ( $a = 4.944(15)$  and  $c = 14.020(4) \text{ \AA}$ ) as shown in Figure 6.29c. Also there are peaks of  $\text{KCl}$  ( $a = 6.289(3) \text{ \AA}$ ) and  $\text{MgO}$  ( $a = 4.209(12) \text{ \AA}$ ) and some other peaks that were difficult to identified and indexed to the known PDF database.

The product of the electrochemical reaction of  $\text{NiCl}_2$  is  $\text{LiCl}$  ( $a = 5.129(5) \text{ \AA}$ ) and  $\text{Ni}$  metal ( $a = 3.524(7) \text{ \AA}$ ) as shown in Figure 6.30a. There are some peaks of the starting material  $\text{NiCl}_2$  ( $a = 3.468(21) \text{ \AA}$  and  $c = 17.302(7) \text{ \AA}$ ), some peaks of  $\text{NiO}$  ( $a = 4.180(12) \text{ \AA}$ ) and some peaks of  $\text{KCl}$  ( $a = 6.299(18) \text{ \AA}$ ).

PXRD confirms that the product of the electrochemical reaction of  $\text{CoCl}_2$  is  $\text{LiCl}$  ( $a = 5.142(19) \text{ \AA}$ ) and  $\text{Co}$  metal ( $a = 2.50(18) \text{ \AA}$ ,  $c = 4.10(26) \text{ \AA}$ ) as shown in Figure 6.30b. There are some peaks of  $\text{KCl}$  ( $a = 6.300(6) \text{ \AA}$ ),  $\text{MgO}$  ( $a = 4.215(10) \text{ \AA}$ ),  $\text{Li}_2\text{O}_2$  ( $a = 3.140(6) \text{ \AA}$ ,  $c = 7.658(15) \text{ \AA}$ ) and  $\text{SiO}_2$  ( $a = 4.90(6) \text{ \AA}$ ,  $c = 5.40(15) \text{ \AA}$ ).

There is a small amount of oxide impurity in each of the diffraction patterns after discharge to a small amount of oxidation of the sample prior to and during the collection of PXRD data.

### 6.3 Summary

This chapter focuses on  $\text{NiCl}_2$ ,  $\text{KNiCl}_3$ ,  $\text{Li}_6\text{VCl}_8$ ,  $\text{Li}_2\text{MnCl}_4$  and  $\text{CoCl}_2$  as cathode materials for use in Li thermal batteries. These materials have not been reported as cathodes until now against  $\text{Li}_{13}\text{Si}_4$ .

$\text{CoCl}_2$ ,  $\text{KNiCl}_3$  and  $\text{Li}_2\text{MnCl}_4$  do not exhibit a flat voltage plateau as there is an insertion reaction rather than a conversion reaction. Thermal batteries prefer a flat voltage plateau as they have a better voltage control during the discharge reaction.

Therefore, at low current densities, the behaviour of both  $\text{Li}_6\text{VCl}_8$  and  $\text{NiCl}_2$  is different to that of  $\text{Li}_2\text{MnCl}_4$ ,  $\text{KNiCl}_3$  and  $\text{CoCl}_2$ , as  $\text{Li}_6\text{VCl}_8$  and  $\text{NiCl}_2$  are the only materials which exhibit a flat voltage plateau in the discharge profiles.

$\text{NiCl}_2$  exhibits the highest capacity of  $360 \text{ mA h g}^{-1}$  compared to other transition metal chlorides, such as  $\text{CoCl}_2$ ,  $\text{KNiCl}_3$ ,  $\text{Li}_2\text{MnCl}_4$  and  $\text{Li}_6\text{VCl}_8$ . However,  $\text{CoCl}_2$  exhibits the lowest cell resistance compared to the others.

Transition metal chlorides exhibit higher voltages against  $\text{Li}_{13}\text{Si}_4$  compared to transition metal disulfides, such as  $\text{FeS}_2$ ,  $\text{NiS}_2$  or  $\text{CoS}_2$ . However, these sulfides exhibit higher capacities compared to transition metal chlorides.

All the electrochemical mechanisms and the products after discharge were confirmed by PXRD data.

## 6.4 References

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## **Chapter 7: Transition Metal Fluoride Cathodes**

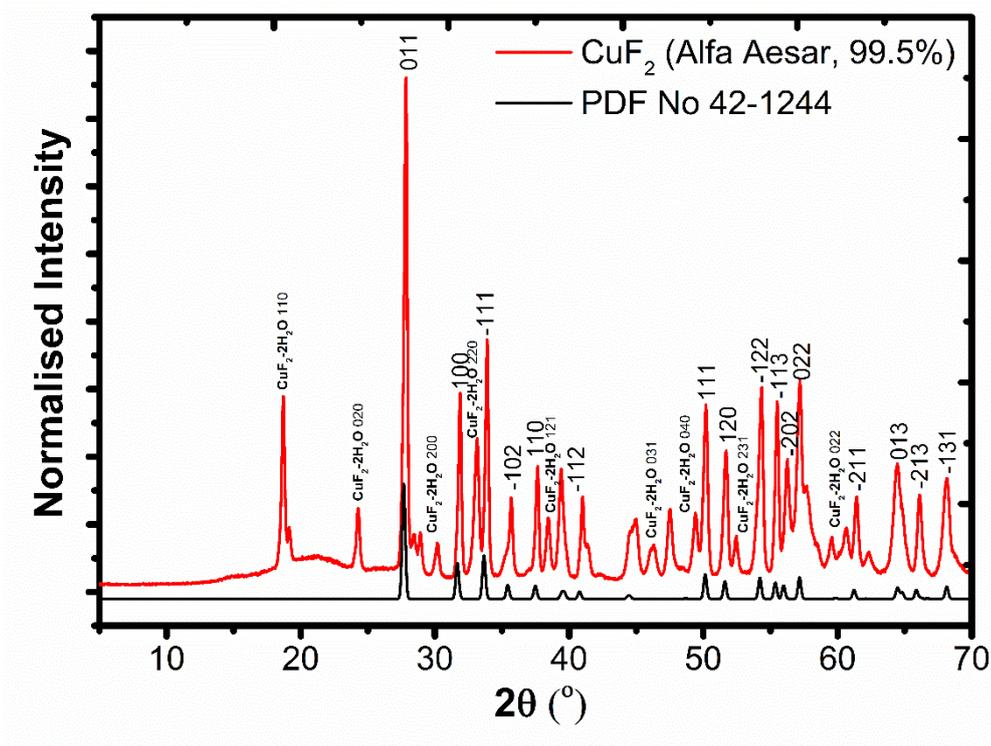
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## Chapter 7: Transition Metal Fluoride Cathodes

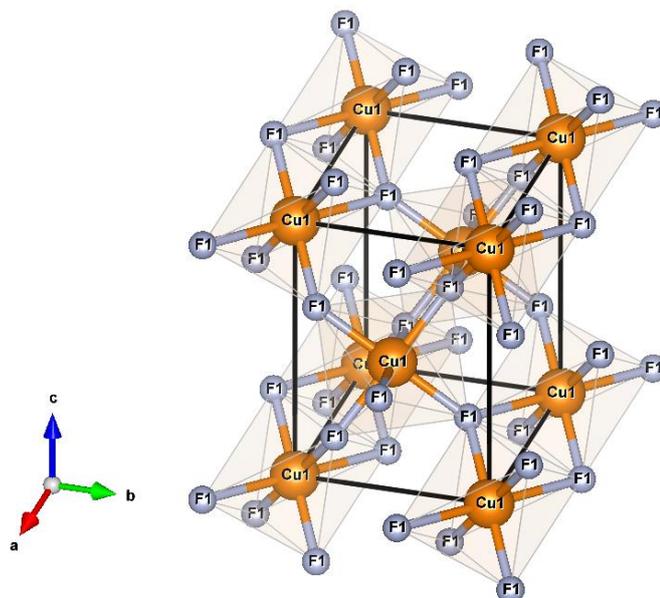
### 7.1 Material Characterisation of Transition Metal Fluorides

#### 7.1.1 CuF<sub>2</sub>

CuF<sub>2</sub> (Alfa Aesar, 99.5%) was analysed by powder X-ray diffraction and the resulting diffraction pattern is presented in Figure 7.1. CuF<sub>2</sub> was identified as the main phase, but there is also a CuF<sub>2</sub>·2H<sub>2</sub>O impurity with cell parameters ( $a = 6.415(16)$  Å,  $b = 7.407(17)$  Å and  $c = 3.319(7)$  Å). CuF<sub>2</sub> crystallises in monoclinic  $P2_1/c$  with cell dimensions ( $a = 3.302(7)$  Å,  $b = 4.563(4)$  Å and  $c = 5.354(5)$  Å) as shown in Figure 7.2. The monoclinic structure of CuF<sub>2</sub> is formed by octahedra of fluorine surrounding Cu cations and each fluorine anion is coordinated by three Cu cations [1]. The melting point of CuF<sub>2</sub> is 836 °C [2].



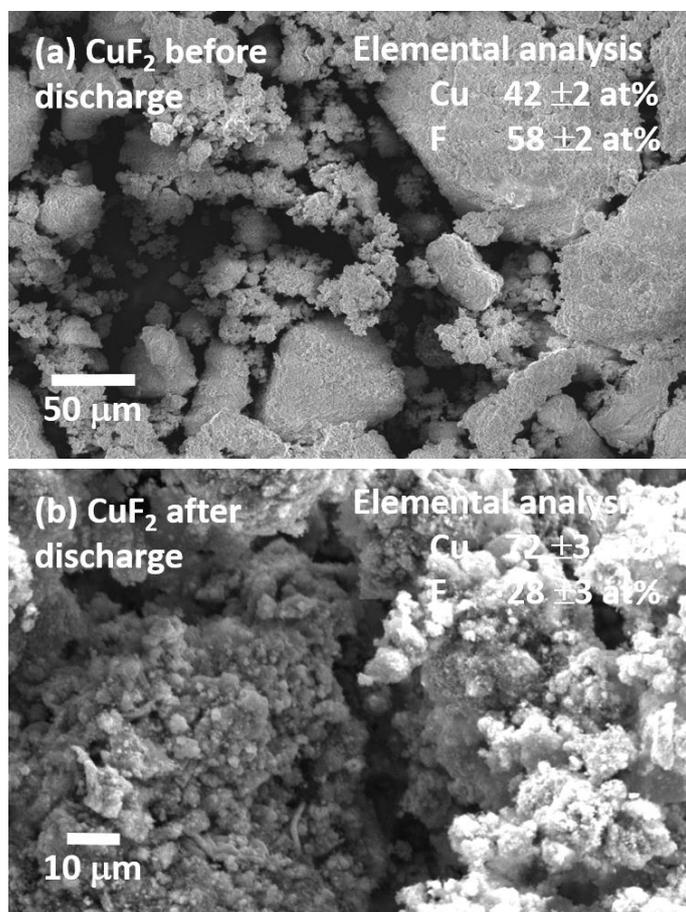
**Figure 7.1.** PXRD data of CuF<sub>2</sub> at room temperature. Experimental pattern is shown by the red line and the simulated diffraction pattern using published crystallographic model [3] is shown by the black line. Impurity is CuF<sub>2</sub>·2H<sub>2</sub>O



**Figure 7.2.** Crystal structure of CuF<sub>2</sub>. Orange atoms are copper and grey atoms are fluorine

## Chapter 7: Transition Metal Fluoride Cathodes

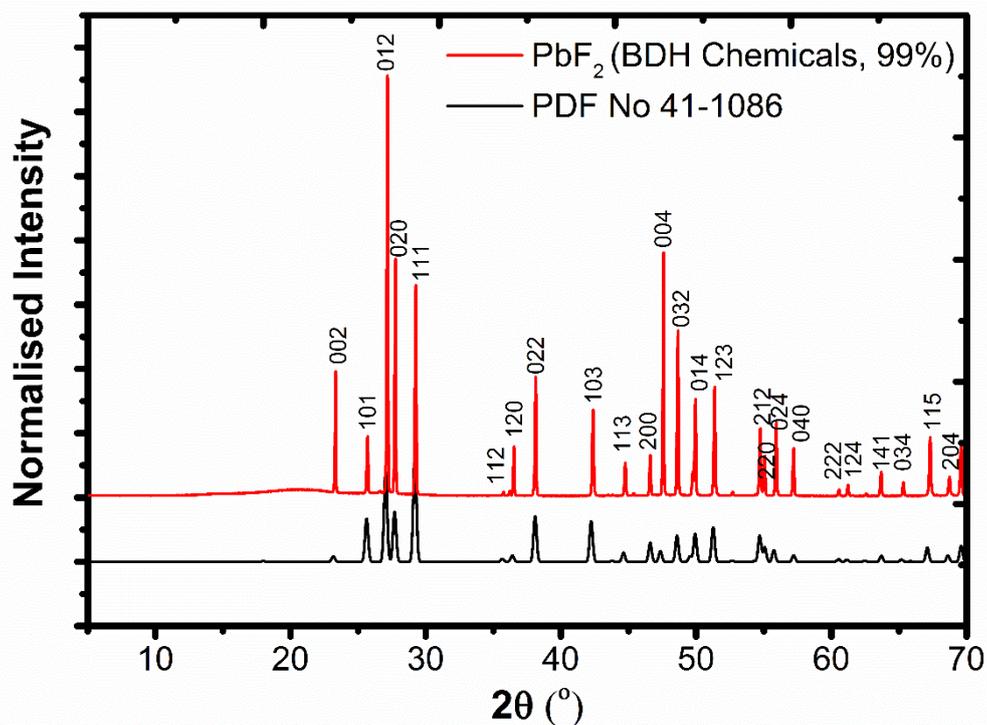
The SEM images of  $\text{CuF}_2$ , as shown in Figures 7.3a and 7.3b, show the size of the crystallites before and after the discharge. Crystallites are bigger than  $50\ \mu\text{m}$ , before testing and become smaller than  $10\ \mu\text{m}$ , after testing. EDX confirms Cu  $42 \pm 2$  at% and F  $58 \pm 2$  at% as expected for  $\text{CuF}_2$  before it being tested as a cathode in a Li thermal battery as shown in Figure 7.3a. The elemental analysis of  $\text{CuF}_2$  cathode electrode after the discharge is Cu  $72 \pm 3$  at% and F  $28 \pm 3$  at% (Figure 7.3b) and this means that different products of the electrochemical mechanism are formed, such as Cu metal and LiF. These products will be confirmed at a later stage by powder X-ray diffraction.



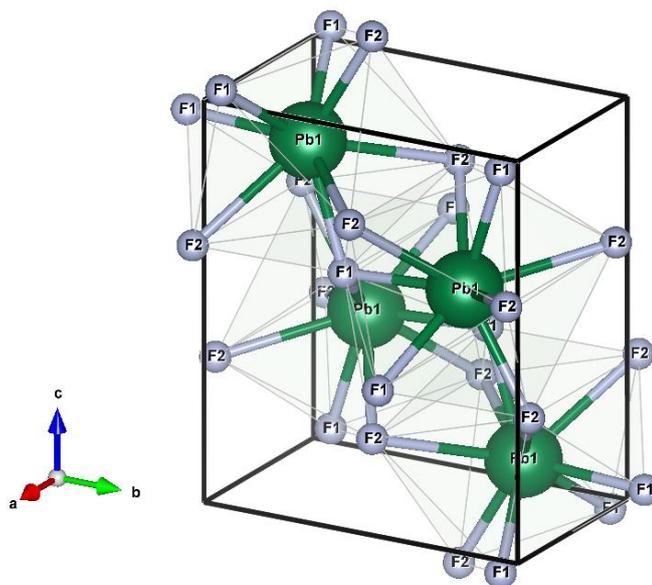
**Figure 7.3.** SEM images of  $\text{CuF}_2$  before (a) and after (b) discharge

7.1.2 PbF<sub>2</sub>

PbF<sub>2</sub> (BDH Chemicals, 99%) was analysed by powder X-ray diffraction and the diffraction pattern is shown in Figure 7.4. PbF<sub>2</sub> was identified as the main phase and crystallises in orthorhombic *Pmnb* with unit cell parameters ( $a = 3.9027(4)$  Å,  $b = 6.4468(5)$  Å and  $c = 7.6552(7)$  Å). This orthorhombic phase transforms to a cubic phase *Fm* $\bar{3}m$  with unit cell parameters ( $a = 5.9395(6)$  Å) at 337 °C [4]. This phase transformation of PbF<sub>2</sub> was obtained in our experiments after the electrochemical test. The orthorhombic structure of PbF<sub>2</sub> has twelve ions, four lead ions and eight fluorine ions as shown in Figure 7.5 [5]. The melting point of PbF<sub>2</sub> is 855 °C [6].



**Figure 7.4.** PXRD data of PbF<sub>2</sub> at room temperature. Experimental pattern is shown by the red line and the simulated diffraction pattern using published crystallographic model [7] is shown by the black line



**Figure 7.5.** Crystal structure of PbF<sub>2</sub>. Green atoms are lead and grey atoms are fluorine

The morphology of PbF<sub>2</sub> was investigated by SEM before and after discharge and images are shown in Figures 7.6a and 7.6b. The SEM images show that the morphology has been changed after the discharge and the size of the crystallites differs. EDX confirms Pb 33 ±1 at% and F 67 ±1 at% as expected for PbF<sub>2</sub> before being tested as a cathode in a Li thermal battery as shown in Figure 7.6a. The elemental analysis of PbF<sub>2</sub> cathode electrode after testing is Pb 15 ±1 at% and F 85 ±1 at% (Figure 7.6b) and this means that different products of the electrochemical mechanism are formed, such as Pb metal and LiF. Once again, these products will be confirmed at a later stage by powder X-ray diffraction.

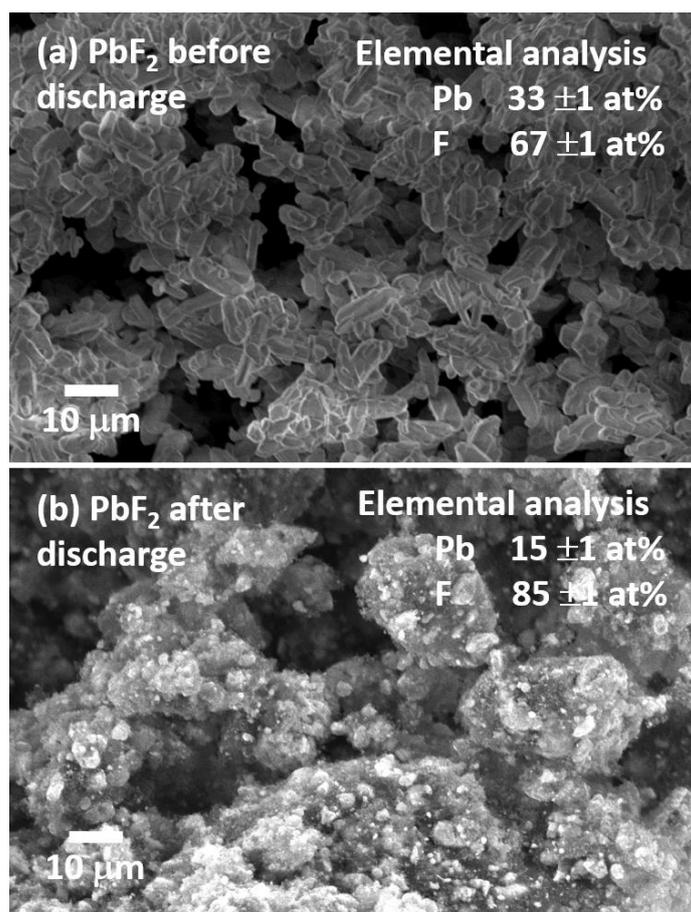


Figure 7.6. SEM images of  $\text{PbF}_2$  before (a) and after (b) discharge

## 7.2 Electrochemical Investigation of Transition Metal Fluorides

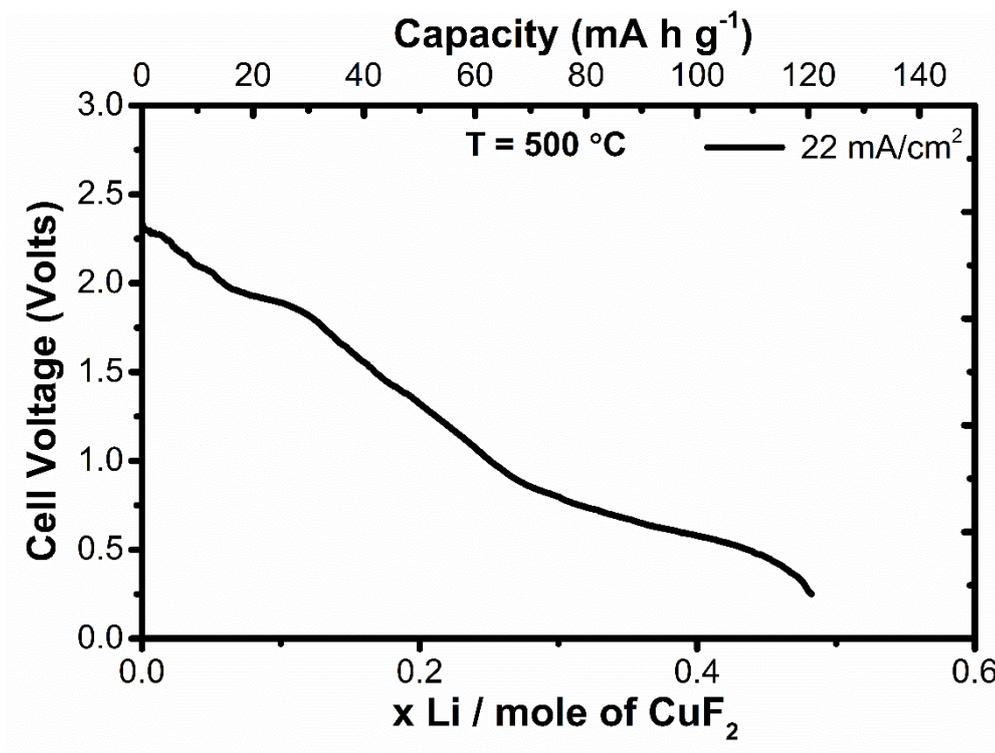
Both transition metal fluorides were studied electrochemically by galvanostatic discharge and  $\text{PbF}_2$  was also studied by galvanostatic intermittent titration technique.

### 7.2.1 $\text{CuF}_2$

Galvanostatic discharge curve for measurements carried out at 500 °C for  $\text{CuF}_2$  is presented in Figure 7.7. Galvanostatic discharge was performed at a current density of 22 mA/cm<sup>2</sup> and the voltage cut-off was 0.25 V as shown in Figure 7.7. There is a high cell voltage (2.25 V) but a flat voltage plateau could not be obtained. A capacity of 120 mA h g<sup>-1</sup> was measured for  $\text{CuF}_2$  and this corresponds to a value of  $x = 0.5$  for the number of lithium atoms transferred during the discharge process. The electrochemical mechanism was expected to be as:



The observed value of  $x = 0.5$  does not match to the theoretical value of  $x = 2$ , because the grain size of the powder  $\text{CuF}_2$  is in the range of microns.  $\text{CuF}_2$  was used as a cathode material at room temperature Li ion batteries and exhibited a voltage profile of 3 V. However, the powder of  $\text{CuF}_2$  was ball milled in different conditions [8]. Therefore, a macro-composite of  $\text{CuF}_2$  exhibited a capacity of 100 m Ah g<sup>-1</sup> [9] and this is similar to 120 m Ah g<sup>-1</sup>, which was measured in our experiments.



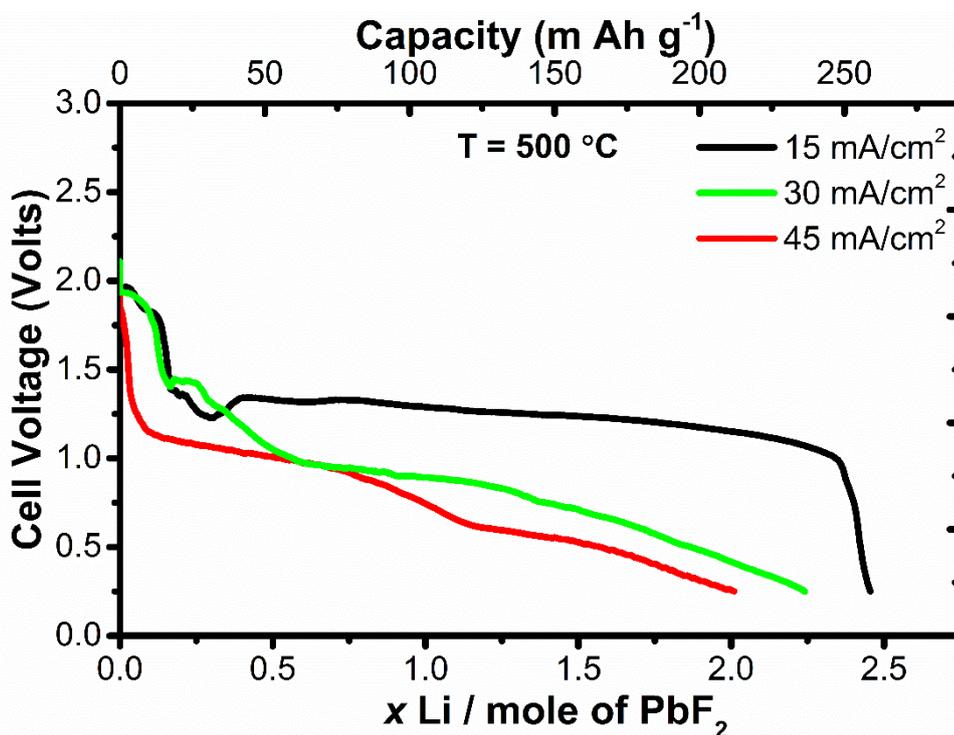
**Figure 7.7.** Galvanostatic discharge of CuF<sub>2</sub> at a current density of 22 mA/cm<sup>2</sup> at 500 °C

### 7.2.2 PbF<sub>2</sub>

Galvanostatic discharge curves for measurements carried out at 500 °C for PbF<sub>2</sub> are presented in Figure 7.8. Galvanostatic discharge was performed at current densities of 15, 30 and 45 mA/cm<sup>2</sup>. The voltage cut-off was 0.25 V as shown in Figure 7.8, and the voltage of PbF<sub>2</sub> drops quickly after 1 V is reached, at a current density of 15 mA/cm<sup>2</sup>. Moreover, there is a single flat voltage plateau at 1.25 V at a current density of 15 mA/cm<sup>2</sup>. A capacity of 260 mA h g<sup>-1</sup> was achieved and this corresponds to a value of  $x = 2.5$ . At higher current densities of 30 and 45 mA/cm<sup>2</sup> a flat voltage plateau could not be obtained due to the decomposition of PbF<sub>2</sub>. Capacities of 245 mA h g<sup>-1</sup> and 219 mA h g<sup>-1</sup> were measured at current densities of 30 and 45 mA/cm<sup>2</sup>, respectively. The electrochemical mechanism corresponds to:



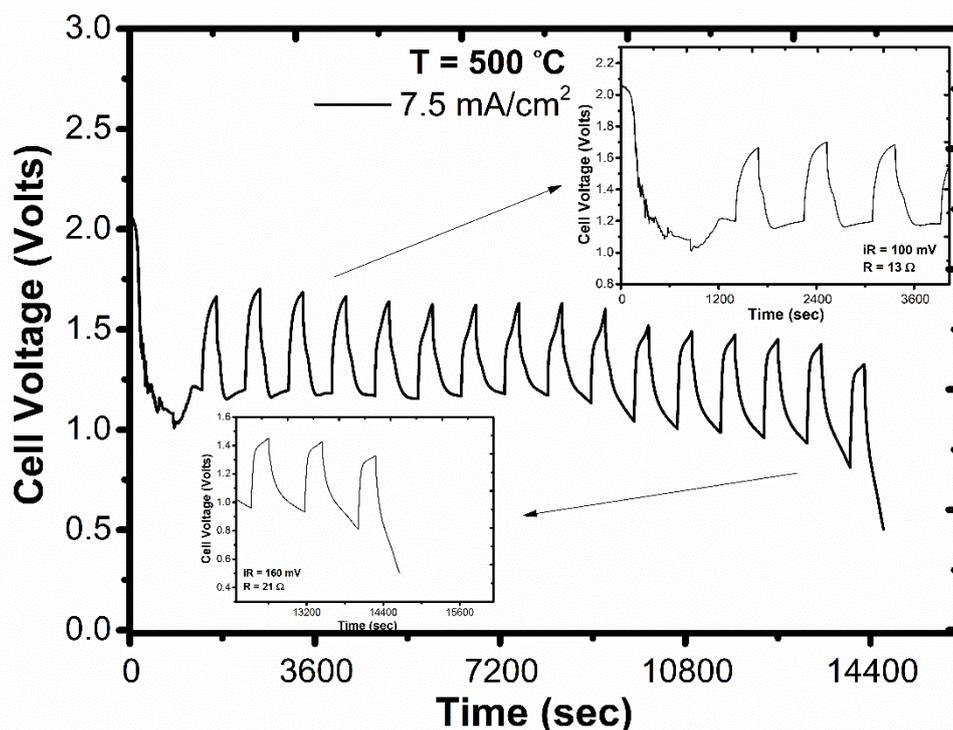
$\text{PbF}_2$  was used as an electrolyte in thin film solid state galvanic cells [10].  $\text{PbF}_2$  was also tested as a cathode material at room temperature in Li ion batteries. The electrochemical reaction of  $\text{PbF}_2$  was completed in two steps between 2.4 and 1.5 V against Li metal. The product of the discharge mechanism was  $2\text{LiF}$  per formula unit and this corresponded to  $360 \text{ mA h g}^{-1}$  [11]. We suggest that  $\text{PbF}_2$  exhibits different electrochemical behaviour at high temperature batteries as the observed value of  $x = 2.5$  does not match to the theoretical value of  $x = 2$ . However, the single plateau of 1.25 V appears from value of  $x = 0.5$  to value of  $x = 2.5$  and this range corresponds to value of  $x = 2.0$  as expected.



**Figure 7.8.** Galvanostatic discharge of  $\text{PbF}_2$  at current densities of 15, 30 and 45  $\text{mA/cm}^2$  at  $500 \text{ }^\circ\text{C}$

The galvanostatic intermittent titration technique measurement (GITT) of  $\text{PbF}_2$  at 500 °C is shown in Figure 7.9. The IR drop is 100 mV at the beginning of discharge and 160 mV at the end of the measurement, which indicates that the cell resistance is increasing during the reduction of the cathode, from a resistance of 13  $\Omega$  at the beginning of the measurement to 21  $\Omega$  after the cell discharge. A single voltage plateau at 1.25 V at a current density of 7.5 mA/cm<sup>2</sup> is also obtained.

The chemical diffusion coefficient  $D = 1.05 \cdot 10^{-8} \text{ cm}^2 \text{ s}^{-1}$  for  $\text{PbF}_2$  can be calculated from equation [3.1] where  $n_m = 0.000815 \text{ (mol)}$ ,  $V_m = 29.01 \text{ (cm}^3 \text{ / mol)}$ ,  $\Delta E_s = 0.050 \text{ (V)}$  and  $\Delta E_t = 0.400 \text{ (V)}$ .



**Figure 7.9.** Galvanostatic intermittent titration technique of  $\text{PbF}_2$  at a current density of 7.5 mA/cm<sup>2</sup> at 500 °C

PXRD data were collected after discharge for both of the cathodes as shown in Figure 7.10.

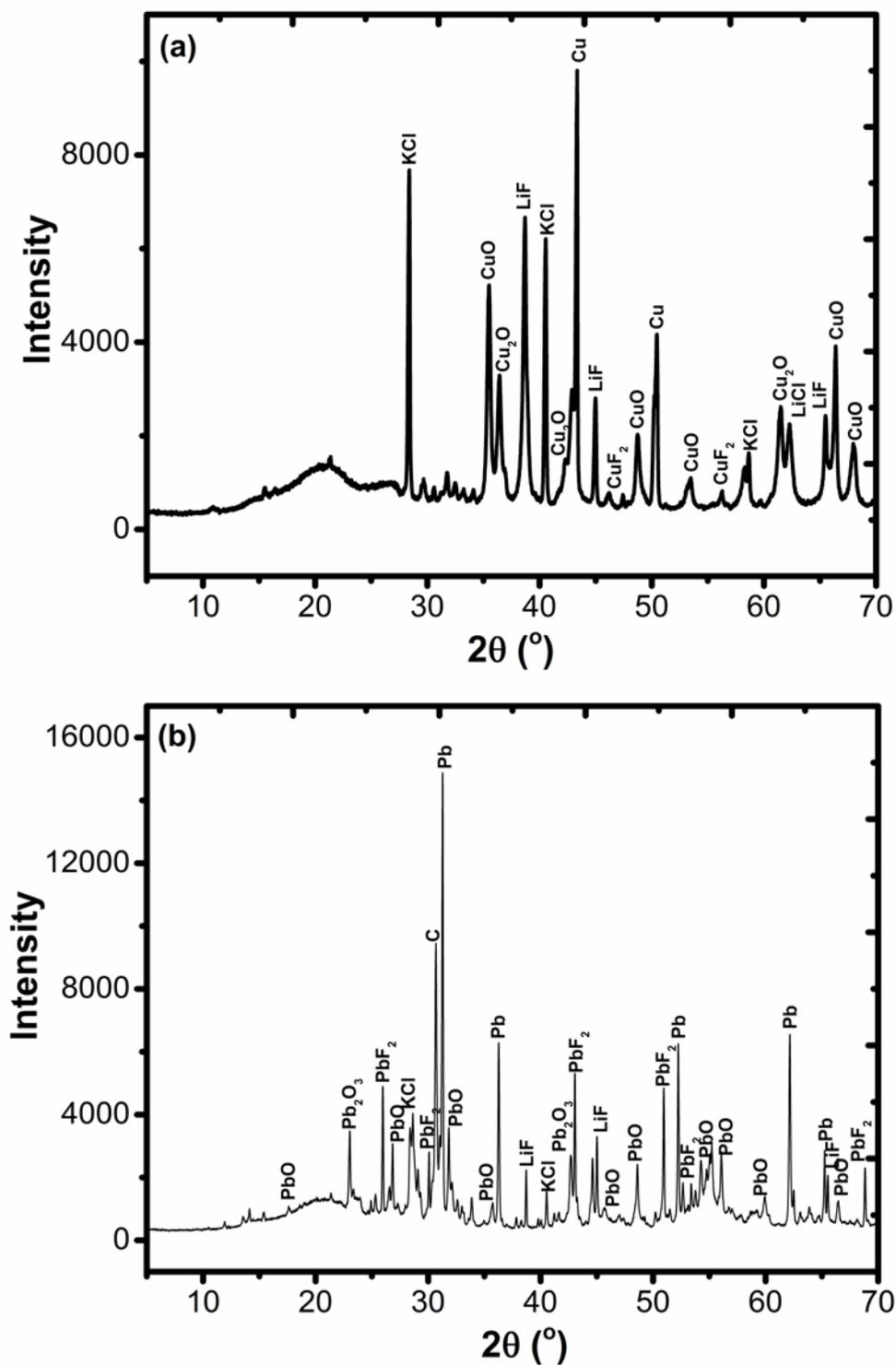


Figure 7.10. PXRD data of the cathode after galvanostatic discharge of (a)  $\text{CuF}_2$  and (b)  $\text{PbF}_2$

PXRD data confirm that the product of the electrochemical reaction of  $\text{CuF}_2$  is Cu metal ( $a = 3.60(6) \text{ \AA}$ ) and LiF ( $a = 3.99(23) \text{ \AA}$ ) as shown in Figure 7.10a. There are some peaks of copper oxides, such as CuO and  $\text{Cu}_2\text{O}$  and some peaks of KCl. The present amount of KCl causes low capacity of the cathode  $\text{PbF}_2$  compared to the expected as we suggest that  $\text{PbF}_2$  dissolves into KCl.

The product of the electrochemical reaction of  $\text{PbF}_2$  is Pb metal ( $a = 4.951(19) \text{ \AA}$ ) and LiF ( $a = 4.025(6) \text{ \AA}$ ) as shown in Figure 7.10b. There are some peaks of the electrolyte KCl and some peaks of lead oxides, such as PbO and  $\text{Pb}_2\text{O}_3$ .

There is a small amount of oxide impurity in each of the diffraction patterns after discharge to a small amount of oxidation of the sample prior to and during the collection of PXRD data.

### 7.3 Summary

This chapter focuses on  $\text{CuF}_2$  and  $\text{PbF}_2$  as cathode materials for use in Li thermal batteries. These materials have not been reported as cathodes against  $\text{Li}_{13}\text{Si}_4$  until now.

$\text{CuF}_2$  does not exhibit a single flat voltage plateau compared to that of  $\text{PbF}_2$  which exhibits a single flat voltage plateau at 1.25 V. This single plateau of  $\text{PbF}_2$  exists only at low current densities of 7.5 and 15  $\text{mA/cm}^2$ .

These electrochemical properties (low capacity and low voltage) of  $\text{CuF}_2$  and  $\text{PbF}_2$  are not suitable for lithium thermal battery applications. This is due to the fact that thermal batteries require as cathodes materials with high voltage and high capacity.

## 7.4 References

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## **Chapter 8: General Conclusions**

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## Chapter 8: General Conclusions

### 8.1 General Conclusions

In this work, ten novel materials ( $\text{CoNi}_2\text{S}_4$ ,  $\text{NiCo}_2\text{S}_4$ ,  $\text{ZrS}_3$ ,  $\text{NiCl}_2$ ,  $\text{CoCl}_2$ ,  $\text{KNiCl}_3$ ,  $\text{Li}_2\text{MnCl}_4$ ,  $\text{Li}_6\text{VCl}_8$ ,  $\text{CuF}_2$  and  $\text{PbF}_2$ ) were studied and tested as cathodes for use in Li thermal batteries.

$\text{CoNi}_2\text{S}_4$  was synthesized by an improved and shorter solid state reaction with a pure phase being synthesized at 550 °C in just two firing steps. The structure was probed by powder X-ray diffraction, while the  $\text{Co}^{2+}/\text{Ni}^{3+}$  cation order and thermal stability of  $\text{CoNi}_2\text{S}_4$  were studied using powder neutron diffraction. SEM showed the morphology and the shape of crystallites of  $\text{CoNi}_2\text{S}_4$  around 5  $\mu\text{m}$  and EDX confirmed the elemental composition as the expected.

The high temperature electrochemical performance of  $\text{CoNi}_2\text{S}_4$  was characterised by galvanostatic discharge and galvanostatic intermittent titration technique (GITT). At a temperature of 500 °C, the value of the working voltage plateau was recorded at different current densities from 15 to 60  $\text{mA}/\text{cm}^2$  and a capacity of 350  $\text{mA h g}^{-1}$  was achieved. A voltage value of 1.75 V [ $x = 4/3$  Li] and of 1.50 V [ $x = 8/3$  Li] vs  $\text{Li}_{13}\text{Si}_4$  for  $\text{CoNi}_2\text{S}_4$  was found at 500 °C. GITT showed an increase in the cell resistance from 13  $\Omega$  to 23  $\Omega$  during the reduction of the cathode electrode.

This material could be a promising candidate for Li thermal battery applications as it exhibits a similar behaviour to the most commonly used sulfides  $\text{FeS}_2$ ,  $\text{NiS}_2$  or  $\text{CoS}_2$ .

$\text{NiCo}_2\text{S}_4$  was synthesised by a solid state reaction with a small amount of impurity  $\text{Co}_9\text{S}_8$  at 550 °C in just two firing steps. The structure was studied by powder X-ray diffraction. SEM showed the morphology and the shape of crystallites of  $\text{NiCo}_2\text{S}_4$  ranges 1 to 10  $\mu\text{m}$  and EDX confirmed the elemental composition as the expected.

The high temperature electrochemical performance of  $\text{NiCo}_2\text{S}_4$  was characterised by galvanostatic discharge and galvanostatic intermittent titration technique (GITT). At a temperature of 500 °C, the value of the working voltage plateau was recorded at

different current densities from 7.5 to 60 mA/cm<sup>2</sup> and a capacity of 290 mA h g<sup>-1</sup> was achieved. A voltage value of 1.70 V [ $x = 2/3$  Li] and of 1.50 V [ $x = 8/3$  Li] vs Li<sub>13</sub>Si<sub>4</sub> for NiCo<sub>2</sub>S<sub>4</sub> was obtained at 500 °C. GITT showed an increase in the cell resistance from 13 Ω to 20 Ω during the reduction of the cathode electrode. This material has a lower voltage and a less capacity compared to CoNi<sub>2</sub>S<sub>4</sub>. The products of the discharge mechanism of both CoNi<sub>2</sub>S<sub>4</sub> and NiCo<sub>2</sub>S<sub>4</sub> were NiS, Co<sub>3</sub>S<sub>4</sub> and Co<sub>9</sub>S<sub>8</sub>.

Zirconium trisulfide (ZrS<sub>3</sub>) was synthesised as a pure phase by a shorter solid state reaction in sealed quartz tube at 730 °C. The structure of the sample was studied by powder X-ray diffraction, the morphology was studied by SEM and the crystals of ZrS<sub>3</sub> are shaped needles.

The high temperature discharge behaviour of ZrS<sub>3</sub> at 500 °C was investigated by galvanostatic discharge and galvanostatic intermittent titration technique (GITT). The value of the working voltage plateau was measured for different current densities of 7.5, 11, 15, 19, 23 and 75 mA/cm<sup>2</sup>. The GITT method showed that the cell resistance increased during the discharge from 6 Ω to 16 Ω.

A new cubic phase LiZr<sub>2</sub>S<sub>4</sub> was found after discharge with cell parameter  $a = 10.452(8)$  Å and EDX confirmed the elemental composition.

The value of the single voltage plateau at 1.70 V with a capacity of 357 mA h g<sup>-1</sup> can define ZrS<sub>3</sub> as a promising candidate material for Li thermal batteries.

KNiCl<sub>3</sub> was synthesised by a solid state reaction in sealed quartz tube at 675 °C for 1 week. It was found a small amount of impurity KCl as the starting material. The structure was probed by powder X-ray diffraction and the morphology was studied by SEM. EDX confirmed the elemental composition as was expected.

KNiCl<sub>3</sub> exhibits a high cell voltage 2.30 V at 425 °C vs Li<sub>13</sub>Si<sub>4</sub> but not a flat voltage profile and a capacity of 262 mA h g<sup>-1</sup> was achieved. The products of the discharge mechanism were Ni metal, KCl and LiCl. The cell resistance was increased from 15 Ω at the beginning of the measurement to 26 Ω after the cell discharge.

Li<sub>2</sub>MnCl<sub>4</sub> was synthesised at 600 °C for 1 week but not as a pure phase. LiCl impurity was found as a starting material. Li<sub>2</sub>MnCl<sub>4</sub> was tested at 400 °C and a capacity of 254 mA h g<sup>-1</sup> was achieved. The cell resistance was measured at 13 Ω at the beginning of the

discharge to 66  $\Omega$  at the end of the discharge. Mn metal and LiCl were formed after the cell discharge.

$\text{Li}_6\text{VCl}_8$  was synthesised at 800  $^\circ\text{C}$  for 1 week with a small amount of impurity  $\text{V}_2\text{O}_3$ . A flat voltage plateau of 1.80 V at a current density of 7.5  $\text{mA}/\text{cm}^2$  with capacity of 145  $\text{mA h g}^{-1}$  was obtained. The cell resistance increased from 6  $\Omega$  to 33  $\Omega$  at the end of the measurement.

$\text{NiCl}_2$  was tested as a commercial compound at 500  $^\circ\text{C}$  and a high voltage profile of 2.25 V at a current density of 22  $\text{mA}/\text{cm}^2$  with capacity of 360  $\text{mA h g}^{-1}$  was obtained. Ni metal and LiCl were formed at the end of discharge. Cell resistance of 13  $\Omega$  at the beginning and 33  $\Omega$  at the end of discharge was obtained.

$\text{CoCl}_2$  was tested as a commercial compound at 500  $^\circ\text{C}$  and a lower voltage profile compared to  $\text{NiCl}_2$  was obtained. Co metal and LiCl were formed at the end of discharge as expected. The cell resistance of 6  $\Omega$  at the beginning of the discharge to 26  $\Omega$  at the end, characterises Co as more conductive than Ni.

$\text{CuF}_2$  was tested as a commercial compound at 500  $^\circ\text{C}$  but decomposed quickly to Cu metal and LiF at a current density of 22  $\text{mA}/\text{cm}^2$  and a capacity of 120  $\text{mA h g}^{-1}$  was obtained.

$\text{PbF}_2$  was tested as a commercial compound at 500  $^\circ\text{C}$  and a single voltage plateau at 1.25 V at a current density of 15  $\text{mA}/\text{cm}^2$  with capacity of 260  $\text{mA h g}^{-1}$  was obtained. Pb metal and LiF were formed as expected. The cell resistance was 13  $\Omega$  at the beginning of the measurement and 21  $\Omega$  at the end of discharge. However,  $\text{PbF}_2$  seems to be more stable than  $\text{CuF}_2$ .

Clearly a full understanding of all the chemical compositions and crystalline phases that are presented in post electrochemical testing is extremely important as it can lead to the discovery of new crystalline phases, whilst also providing an insight into the electrochemical processes occurring during discharge.

Finally, Table 8.1 shows the comparison between the novel cathodes and the well-known transition metal disulfides.

**Table 8.1.** Thermal stability, overall capacity, voltages vs  $\text{Li}_{13}\text{Si}_4$ , and discharge products of Novel Cathodes compared to that of transition metal disulfides  $\text{FeS}_2$ ,  $\text{CoS}_2$  and  $\text{NiS}_2$

Materials	Thermal stability ( $^{\circ}\text{C}$ )	Capacity ( $\text{mA h g}^{-1}$ )	Voltages (V) vs $\text{Li}_{13}\text{Si}_4$	Discharge Products
$\text{FeS}_2$	550 [1, 2]	558 [3]	1.77, 1.64, 1.13 [4]	Fe and $\text{Li}_2\text{S}$ [4]
$\text{CoS}_2$	650 [5]	598 [3]	1.75, 1.40, 1.25 [4]	Co and $\text{Li}_2\text{S}$ [4]
$\text{NiS}_2$	600 [6]	545 [3]	1.76, 1.60, 1.40, 1.25 [4]	Ni and $\text{Li}_2\text{S}$ [4]
$\text{ZrS}_3$	700 [7]	357 [7]	1.70 [7]	$\text{LiZr}_2\text{S}_4$ [7]
$\text{CoNi}_2\text{S}_4$	550 [8]	350 [8]	1.75, 1.50 [8]	$\text{Co}_3\text{S}_4$ , NiS and $\text{Co}_9\text{S}_8$ [8]
$\text{NiCo}_2\text{S}_4$	550	290	1.70, 1.50	$\text{Co}_3\text{S}_4$ , NiS and $\text{Co}_9\text{S}_8$
$\text{KNiCl}_3$	675	262	2.30	Ni, KCl and LiCl
$\text{NiCl}_2$	500	360	2.25	Ni and LiCl
$\text{CoCl}_2$	500	330	2.00	Co and LiCl
$\text{Li}_2\text{MnCl}_4$	600	254	2.50	Mn and LiCl
$\text{Li}_6\text{VCl}_8$	800	145	1.80	V and LiCl
$\text{PbF}_2$	500	260	1.25	Pb and LiF
$\text{CuF}_2$	500	120	2.25	Cu and LiF

## 8.2 References

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